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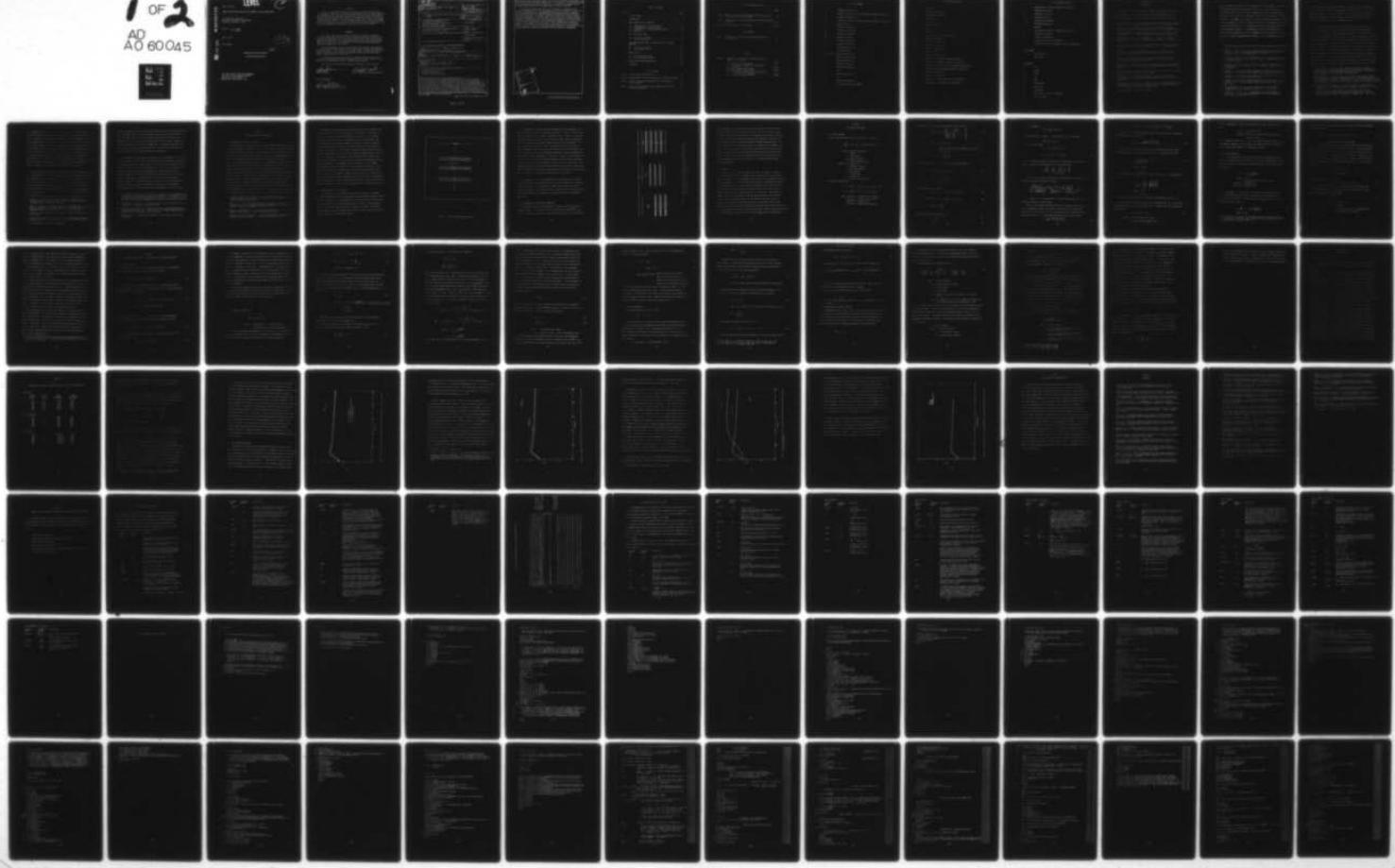
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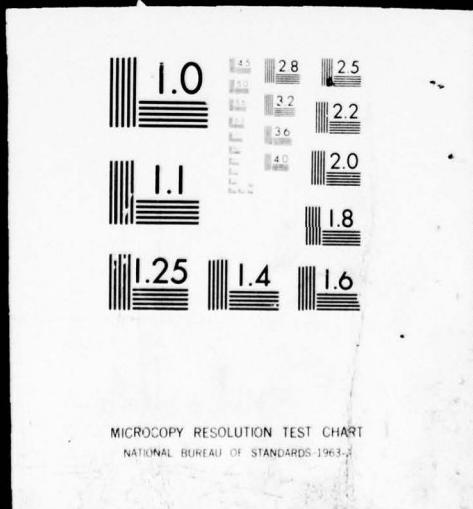
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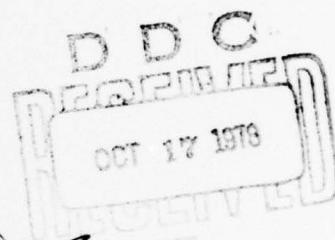
COMBUSTION RESPONSE MODELING FOR COMPOSITE SOLID PROPELLANTS

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June 1, 1978

Final Report



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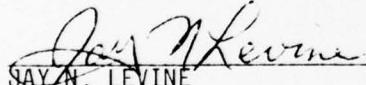
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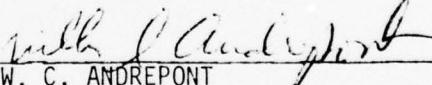
This report was prepared by the Jet Propulsion Laboratory, Pasadena, California 91103, under Air Force Rocket Propulsion Laboratory MIPR No. F04611-76-X-0050 as administered by the National Aeronautics and Space Administration under Contract NAS7-100. This investigation is entitled, "Combustion Response Modeling for Composite Solid Propellants," and was technically monitored by Captain Jack Donn and Mr. Jay Levine.

The Program Manager for this program was Mr. Leon Strand. Contributions to the technical effort were made by Drs. James Bowyer, Norman Cohen, Fred Culick and Kumar Ramohalli. The program was conducted within the Advanced Technology Group of the Solid Propulsion and Environmental Systems Section, under the general supervision of Dr. Giulio Varsi.

This report has been reviewed by the Information Office/XOJ and is releasable to the National Technical Information Service (NTIS). At NTIS it will be available to the general public, including foreign nations.

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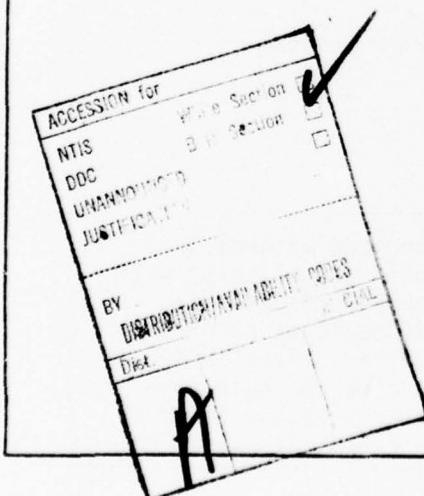
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approximation of the BDP flame model is utilized to represent the gas phase. By the use of several reasonable assumptions, it is found that a significant portion of the problem can be solved in closed form. A method is presented by which the model can be applied to tetramodal particle size distributions.

A computerized steady-state version of the model was completed, which served to validate the various approximations and lay a foundation for the combustion response modeling. The combustion response modeling was completed in a form which does not require an iterative solution, and some preliminary results were acquired. The model satisfactorily describes the steady state combustion properties, but is deficient in describing the transient combustion response. Although an effect of solid phase heterogeneity on transient combustion response is predicted by the current model, the effect is so small as to allow it to be neglected in future work. It is concluded that some other mechanism associated with the propellant heterogeneity must be incorporated into the theory to account for observed behavior. Potential deficiencies of the current model are identified, and areas for future work are recommended.



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### LIST OF SYMBOLS

a	defined in Equation 15
A	kinetics prefactor; also a solid phase parameter in Equation 51
b	defined in Equation 15
B	defined in Equation 3; also a gas phase parameter in Equation 51
c	heat capacity
C	defined in Equation 4.
$C_F$	defined in Equation 24
$C_M$	defined in Equation 13
$C_1, C_2$	arbitrary constants
d	defined in Equation 16
D	defined in Equation 4
$D_1$	oxidizer particle size
E	activation energy
$f_1(x), f_2(x)$	denotes functions of x
F	defined in Equation 22
g	spatial gradient in $\tau$
H	defined in Equation 3
$H_f$	defined in Equation 43
i	$\sqrt{-1}$
k	thermal conductivity
K	C/D
$K_2$	defined by Equation 49
n	burning rate pressure exponent

LIST OF SYMBOLS (cont'd)

$p$	pressure
$Q$	heat of decomposition
$Q_f$	heat release in the gas
$r$	burning rate
$R$	gas constant
$R$	response function
$t$	time
$T$	temperature
$u$	gas velocity normal to the surface
$v_3$	defined in Equation 50
$v_5$	defined in Equation 32
$v_{6A}$	defined in Equation 50
$v_{6B}$	defined in Equation 50
$w$	weight fraction
$x$	distance into the solid
$x^*$	effective flame height, defined by Equation 24
$y$	dimensionless distance $x$ , defined in Equation 3
$y_s$	time-dependent surface position, defined in Equation 29
$y^*$	dimensionless flame height, defined in Equation 20
$z$	defined in Equation 16
$z$	defined in Equation 5b
$\Delta y$	thickness of a particular layer, see Equation 18
$\epsilon$	an extremely small number, see Equation 38b

LIST OF SYMBOLS (Cont'd)

$\xi$	dimensionless distance $x$ , defined in Equation 19
$n$	defined by Equation 7
$o$	Defined in Equation 32
$\kappa$	thermal diffusivity
$\lambda_1, \lambda_2$	defined in Equation 36
$\xi$	defined by Equation 6
$\rho$	density
$\tau$	normalized temperature $T$ , defined in Equation 3
$\tau_F$	defined in Equation 41
$x$	defined in Equation 32
$\omega$	angular frequency of oscillations
$\Omega$	dimensionless angular frequency, defined in Equation 26

Superscripts

'	perturbed value
-	mean value

Subscripts

a	AP
b	binder
f	flame
g	gas
m	melt
N	Nth AP layer
o	deep solid
s	propellant
Top	upper side of boundary or interface
w	wall or surface

SECTION I  
INTRODUCTION

Experimental data have established that ammonium perchlorate (AP) particle size has a significant effect upon the pressure-coupled response function of composite solid propellants (1-14). Moreover, the effect cannot be attributed

1. Green, L.G., "Effects of Oxidizer Concentration and Particle Size on Resonance Burning of Composite Solid Propellants", Jet Prop. 28, 159-164 (Mar., 1958).
2. Strand, L. D., "Low Pressure L\* Instability and Extinction", 3rd ICRPG Combustion Conference (CPIA Publication 138, Vol. I, Feb., 1967) pp. 195-207.
3. "Experimental Studies on the Oscillatory Combustion of Solid Propellants", Report NWC-TP-4393, U.S. Naval Weapons Center, China Lake, CA (Mar., 1969).
4. Beckstead, M.W., Boggs, T.L. and Madden, O.H., "The effect of Oxidizer Particle Size and Binder Type on Nonacoustic Instability", AIAA Paper 69-175 (1969).
5. Boggs, T.L. and Beckstead, M.W., "Failure of Existing Theories to Correlate Experimental Nonacoustic Combustion Instability Data", J. AIAA 8, 626-631 (Apr. 1970).
6. Crump, J.E., "Combustion Instability in a Series of AP-HTPB Smokeless Propellants", 8th JANNAF Combustion Meeting (CPIA Publication 220, Vol. II, Dec. 1971) pp. 81-90.
7. Crump, J.E., "Combustion Instability Studies on Non-metallized AP-HTPB Propellants", 9th JANNAF Combustion Meeting (CPIA Publication 231, Vol. III, Dec., 1972) pp 123-134.
8. Wendelken, C.P., "Combustion Stability Characteristics of Solid Propellants", AFRPL-TR-73-63, Air Force Rocket Propulsion Laboratory, Edwards, CA (Oct., 1973).
9. "Aluminum Behaviour in Solid Propellant Combustion", AFRPL-TR-74-13, Lockheed Propulsion Company, Redlands, CA (May, 1974).
10. Micheli, P.L., "Stabilization of Smokeless Propellants with Additives", 11th JANNAF Combustion Meeting (CPIA Publication 261, Vol. III, Dec., 1974) pp 123-136.
11. Anderson, F.A. and Kumar, R.N., "Feasibility Study of Propellants and Igniters for Shuttle Solid Rocket Booster Separation Motors", Report 900-710, Jet Propulsion Laboratory, Pasadena, CA (June, 1975).

(See next page for remainder of references.)

simply to changes in burning rate or formulation; the effect appears to involve the composite propellant heterogeneity as well (15). Classical theories of combustion driving (16) have assumed a homogeneous propellant and are therefore inadequate to fully explain the combustion instability characteristics of composite propellants. The community has come to rely upon experimental measurement of the combustion response in T-Burners, and work in recent years has been devoted largely to improving the method (17-19). Although experimental measurement serves several important purposes, interest in the theoretical work has revived because the acquisition and interpretation of full complements of data continues to be expensive and does not furnish a phenomenological mechanism for the guidance of propellant R & D.

Viewing the combustion zone as the region between the thermal wave penetration

- 
12. Cohen, N.S., et al., "Design of a Smokeless Solid Rocket Motor Emphasizing Combustion Stability", 12th JANNAF Combustion Meeting (CPIA Publication 273, Vol. II, Dec. 1975) pp 205-220.
  13. Horton, M.D. and Rice, D. W., "The effects of Compositional Variables Upon Oscillatory Combustion of Solid Rocket Propellants", Combustion and Flame 8, 21-28 (Mar. 1964).
  14. "Control of Solids Distribution in HTPB Propellants", Contract F04611-76-C-0006, Hercules, Inc., Allegheny Ballistics Laboratory, Cumberland, MD. (in progress).
  15. Cohen, N. S., "Report of Workshop on Combustion Instability of Smokeless Propellants", Proceedings of 14th JANNAF Combustion Meeting (to be published).
  16. Culick, F.E.C., "A Review of Calculations for Unsteady Burning of a Solid Propellant", J. AIAA 6, 2241-2254 (Dec. 1968).
  17. "T-Burner Testing of Metallized Solid Propellants", AFRPL-TR-74-28, edited by F.E.C. Culick, Air Force Rocket Propulsion Laboratory, Edwards, Calif. (Oct. 1974).
  18. "T-Burner Motor Verification Program Final Report", AFRPL-TR-74-71, Aerojet Solid Propulsion Company, Sacramento, Calif. (Jan. 1975).
  19. Lorraine, R.L. and Linfor, J.J., "Measurement of Propellant Response at High Frequency", 13th JANNAF Combustion Meeting (CPIA Publication 281, Vol. II, Dec. 1976) pp 95-112.

in the solid and the location of the flames in the gas, there are several ways in which the composite propellant heterogeneity can manifest itself. Two schools of thought have arisen: one which emphasizes the solid phase, treating the gas as a homogeneous source of propellant heating; and one which emphasizes the gas, continuing to treat the solid as a homogeneous medium.

The solid phase proponents may be represented by Lengelle & Williams (20), Kumar (21) and Cohen (12). Lengelle & Williams performed a one-dimensional analysis of a solid having sinusoidal thermal properties. Although the model was too idealized for direct practical application, it made the essential point that the heterogeneity augments the combustion response depending upon the periodicity of the thermal properties (and, therefore, particle size and spacing). Kumar introduced a surface melt layer, purportedly representative of the AP surface, in an otherwise homogeneous solid. The most significant result of this model was a mechanism by which zero-exponent propellants could exhibit a positive combustion response and pressure effects<sup>1</sup>. Since Kumar did not treat in-depth heterogeneity, particle size effects appeared in the solid only through the effect of burn rate on melt layer thickness<sup>2</sup>. Cohen postulated two characteristic parameters for the solid phase,

- 
1. Classical theories produce a response function proportional to pressure exponent, yet it is well known that plateau (zero exponent) and mesa (negative exponent) propellants have exhibited combustion instability. The AP melt may be analogous to the foam zone of such propellants.
  2. An effect of burn rate on melt layer thickness would also appear in double-base propellants, so it cannot be the sole basis for the role of AP particle size in composite propellants. Furthermore, AP size effects persist at constant burning rate when catalysts are used or solids loading or distribution are varied.
- 
20. Williams, F.A., and Lengelle, G., "Simplified Model for Effect of Solid Heterogeneity on Oscillatory Combustion", *Astronautica Acta* 14, 97-118 (1968).
  21. Kumar, R.N., "Some Considerations in the Combustion of AP/Composite Propellants", Report under Contract NAS7-100, Guggenheim Jet Propulsion Center, California Institute of Technology, Pasadena, Calif. (Aug. 1972).

each dependent upon particle size. One was a measure of frequency response, the other of thermal response. He assumed that all response function curves could be determined by the pressure exponent plus these two parameters, and used experimental data for a standard propellant as calibration. The essential result is that decreasing particle size increases the peak response and shifts the peak to higher frequency. He further assumed that all multimodal propellants could be treated by linear superposition of the constituent results, and predicted multi-peaked response functions. Although the method is not founded upon a formal analysis, it is being used to guide propellant tailoring (15,22). Extensive applications have revealed some qualitative and quantitative deficiencies, for example, a tendency to over-emphasize the effect of fine sizes (22).

The gas phase proponents may be represented by Hamann (23), Glick and Condon (24), and Beckstead (25). All utilize some form of the "BDP" model of steady-state combustion (26) to represent the gas phase details, and none consider the solid to be heterogeneous. Hamann performed a perturbation analysis upon the entire BDP model, but did not report any results. Beckstead used the BDP model to calculate values for the parameters which are called for by the homogeneous theory of Denison & Baum (27). This approach of combining unrelated models is

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- 22. Glick, R.L., Private Communications, Thiokol Corp., Huntsville, Ala. (1977).
  - 23. Hamann, R.J., "Three Solid Propellant Combustion Models, A Comparison and Some Application to Non-Steady Cases", Memo. M-215, Delft University of Technology, Delft, Netherlands (Apr. 1974).
  - 24. Condon, J. A., Osborn, J.R. and Glick, R.L., "Statistical Analysis of Poly-disperse, Heterogeneous Propellant Combustion: Nonsteady-state", 13th JANNAF Combustion Meeting (CPIA Pub. 281, Vol. II, Dec. 1976) pp 209-223.
  - 25. Beckstead, M. W., "Combustion Calculations for Composite Solid Propellants", *ibid.*, 299-312.
  - 26. Beckstead, M.W., Derr, R.L. and Price, C.F., "Model of Solid Propellant Combustion Based on Multiple Flames", *J. AIAA* 8, 2200-2207 (Dec. 1970).

(See next page for remainder of references.)

open to question (15), and a review of the technique reveals several deficiencies<sup>3</sup>. Glick and Condon employed a similar approach, but used a modified BDP model (28) for polydisperse particle size distributions and the method of Zeldovich and Novozhilov (29) as an alternative to the theory of Denison & Baum. Comparison of results with experimental data was disappointing. Considerable improvement was noted, however, when the Cohen postulates were incorporated into the method to position the peak response and peak response frequency (24).

The following concensus appears to emerge from this background. First, there is a need to account for the melt layer and the in-depth solid phase heterogeneity of composite propellants. Second, there is a need to provide an analytical basis to test, confirm or modify the Cohen postulates. Third, the representation of the gas phase also should address the heterogeneity of composite propellants by embodying some form of the BDP model rather than the homogeneity of the classical theories. Accordingly, it was the objective of this program to develop an analytical model of the combustion response of composite solid propellants with particular attention to these contributions of the propellant heterogeneity. Primary emphasis was placed on the modeling of heterogeneity in the solid phase.

- 
- 3 For example, calculation of the "A" and "B" parameters of the homogeneous theory by this method reveals much too small a pressure effect to account for measured changes in the response function curve with pressure. As with Kumar, particle size effects appear only through changes in steady-state burning rate properties.
27. Denison, M. R. and Baum, E., "A Simplified Model of Unstable Burning in Solid Propellants", J. ARS 31, 1112-1122 (Aug. 1961).
28. Glick, R.L. and Condon, J.A., "Statistical Analysis of Polydisperse, Heterogeneous Propellant Combustion: Steady-State", 13th JANNAF Combustion Meeting, (CPIA Pub. 281, Vol. II, Dec. 1976) pp 313-345.
29. Novozhilov, B. V., "Nonstationary Combustion of Solid Rocket Fuels", Nauka, Moscow (1973).

SECTION 2  
MODEL PREMISES AND ASSUMPTIONS

2.1 REPRESENTATION OF THE SOLID PHASE

The solid phase is represented by a "sideways sandwich", following the concept of Lengelle & Williams, as shown in Figure 1. This picture, really, does nothing more than state that the analysis is one-dimensional, so its dissimilarity to real propellants is of no greater concern than is the use of a one-dimensional treatment. Such a treatment assumes that the lateral processes are negligible in comparison to the normal processes. The solid is considered to be semi-infinite, having alternating layers of AP and binder. The thickness of the AP layers is nominally equal to the particle size, with exceptions to be noted later. The thickness of the binder layers is equal to the interstitial spacing as determined from the statistical geometry (26, 30). The surface AP layer contains a thin melt layer, which is justified experimentally (31-33), and follows the model of Kumar as a region of decomposition reactions in accordance with an Arrhenius law. The melt layer is "thin" in that the melting point of AP approximates the surface temperature during deflagration (32, 33). The analysis is linearized for small harmonic pressure perturbations, and is concerned with pressure-coupling only.

- 
30. Cohen, N.S., Price, C.F. and Strand L.D., "Analytical Model of the Combustion of Multicomponent Solid Propellants", AIAA Paper 77-927, AIAA/SAE 13th Propulsion Conference (July, 1977).
  31. Boggs, T.L., "The Decomposition, Pyrolysis and Deflagration of Ammonium Perchlorate", et seq., 7th JANNAF Combustion Conference (CPIA Publication 204, Vol. I, 1971) pp 113-138.
  32. Guirao, C. and Williams, F.A., "A Model for Ammonium Perchlorate Deflagration Between 20 and 100 atm", J. AIAA 9, 1345-1356 (July 1971).
  33. Beckstead, M.W. and Hightower, J.D., "Surface Temperature of Deflagrating Ammonium Perchlorate Crystals", J. AIAA 5, 1785-1790 (Oct. 1967).

Although the model contains the convective heating term to represent the regression of the material at the mean rate  $\bar{r}$ , the geometry of the layers is taken to be fixed with the AP layer always at the surface. This assumption is similar to the statistically fixed geometry used in the BDP model. One consequence of this assumption is that the "pulsation" mechanism associated with the sequential burn through of individual crystals and binder layers is excluded. The existence of a "pulsation" mechanism, coherent over microscopic regions of propellant surface, is open to question, although Lengelle & Williams (20) offer an argument in its favor. Thus, the present model examines only the effect of heterogeneity in relation to the thermal wave propagation through the solid propellant. A consequence of this assumption is that in-depth heterogeneity will not be important in those cases where the particle size is larger than the thermal wave (generally, coarse particles and high burn rate). Whether or not this consequence is unduly restrictive remains to be seen, but the fact that catalyzed coarse propellants are more stable than fine propellants would seem to permit it. The statistically fixed geometry requires the surface AP layer (including the melt) to have a thickness  $\sqrt{2/3}$  of the particle size (26).

## 2.2 REPRESENTATION OF THE GAS PHASE

The function of the gas phase in the analytical scheme is to transform the oscillating pressure into an oscillating heat flux boundary condition at the surface of the AP melt. An approximate form of the BDP model has been selected to represent the gas phase, and the gas phase is assumed to be quasi-steady (viz, the gas phase responds instantly to changes in pressure). The approximation assumes a single flame above the propellant surface, where all gas phase reactions occur, as illustrated by Figure 1.

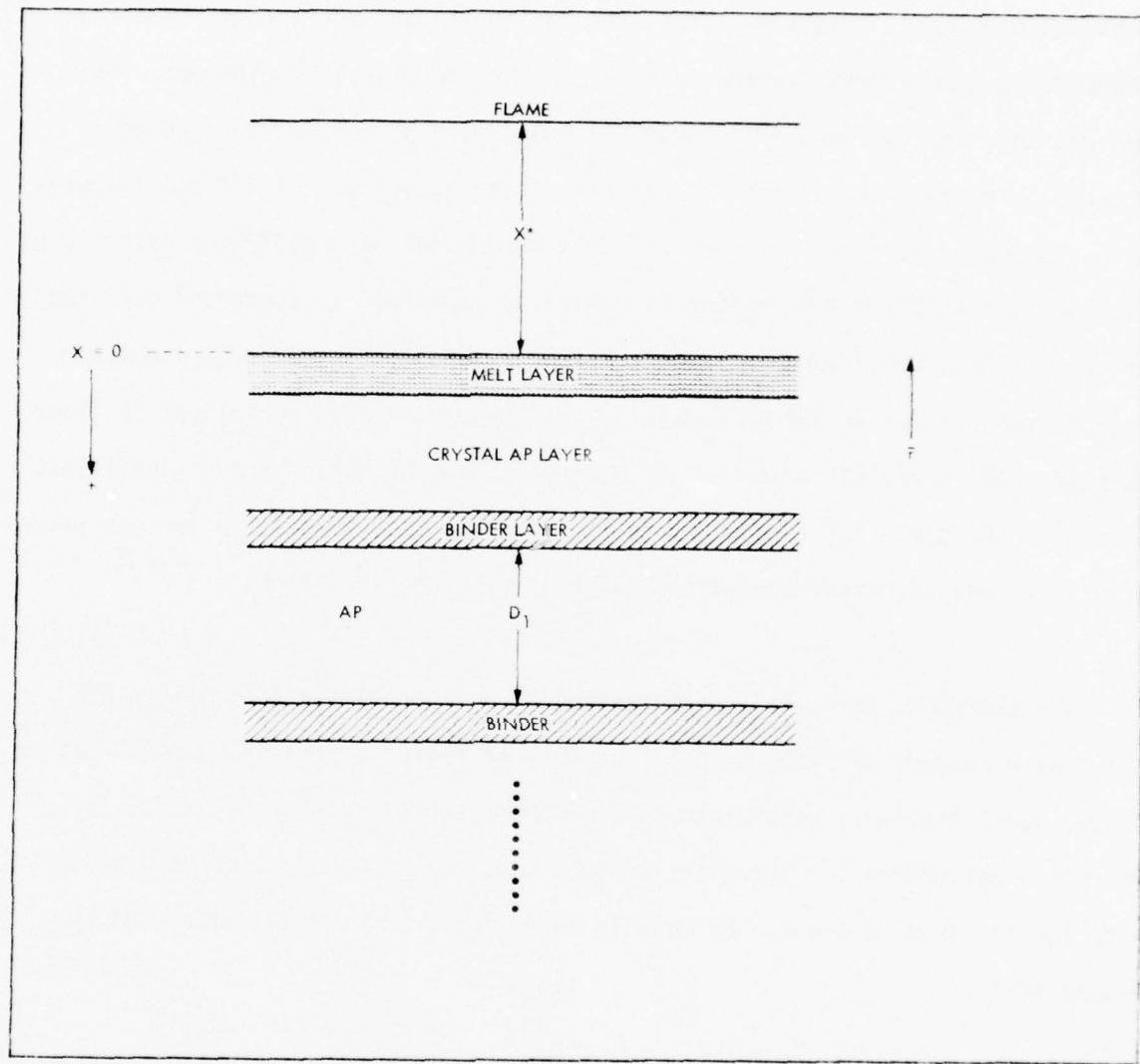


Figure 1. Physical Model Representation

Presuming that the condensed phase heterogeneity has the dominant effect upon the response function of composite propellants, it would not seem to matter what particular model were chosen to represent the gas so long as it provides a reasonable boundary condition. Thus, the Denison & Baum model could have been chosen to preserve some systematic order to the analytical development. This was not done for two reasons: First, it would have presumptuously ignored those developments addressing the gas phase heterogeneity in a BDP model framework. Second, the fact that the Denison & Baum model is heavily dependent upon fluctuations in flame temperature is coming to be viewed as a serious deficiency of that model. Variations in flame temperature are fourth order in magnitude with respect to variations in pressure. On the other hand, variations in flame standoff, which are not addressed by Denison & Baum but which are a significant aspect of the BDP model (and a key to the particle size effects in the gas phase), are first order of magnitude with respect to pressure variations.

The approach, then, is a perturbation of an approximate form of the BDP model with respect to flame standoff as well as flame temperature. Perturbation of the model itself is considered to be proper, whereas use of the model to calculate parameters for substitution into a different model is open to question. With the approximate model, the task is much simpler than that undertaken by Hamann (23).

### 2.3 REPRESENTATION OF MULTIMODAL PROPELLANTS

Multimodal propellants are represented by adjacent columns of layers, as shown by Figure 2. Each particle size, corrected by the factor  $\sqrt{2/3}$ , tops a column. The remaining AP layers consist of the finest size in the distribution.

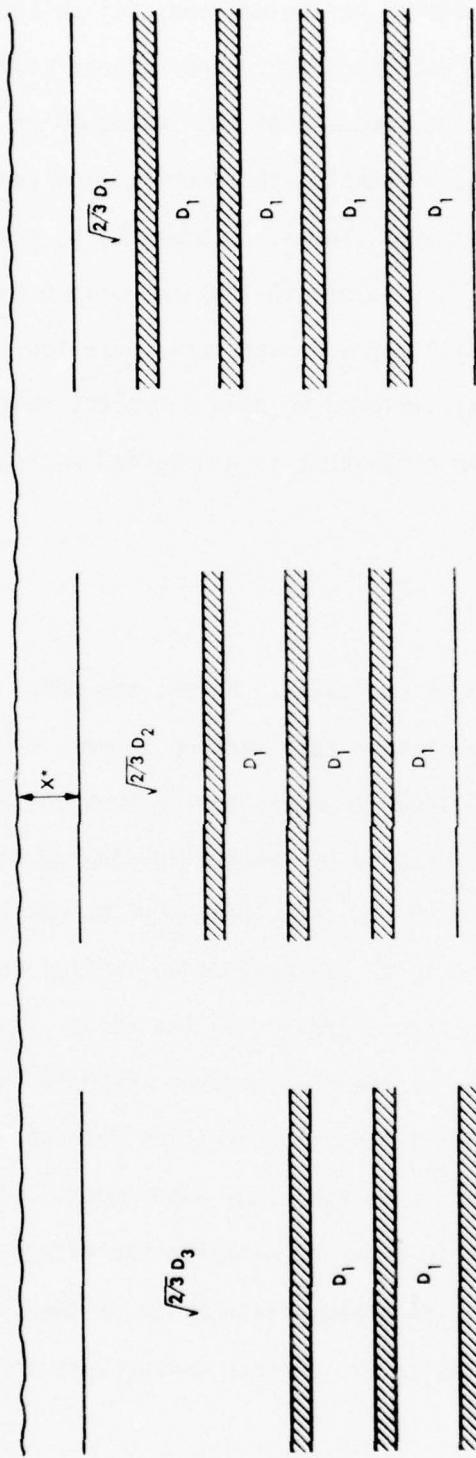


Figure 2. Layered Model of the Solid Phase for a Trimodal Propellant:  
Sizes  $D_1$ ,  $D_2$ ,  $D_3$ . Shaded Layers are Binder. The Top of the  
Surface AP Layer is a Thin Melt

This assumption is justified by the fact that the finest size will fill the smallest interstices between coarser particles, and will be valid so long as the thermal wave does not penetrate to a subsequent coarse sublayer. Validity is likely in practical propellants because of the influence of the fine size in raising the burning rate and decreasing the thermal wave penetration. The binder layers are all of the same thickness, as computed by the method of Ref. (30). All of the columns are constrained to the same mean burning rate, which implies one effective flame height or characteristic size for the diffusion flame. However, the columns are allowed to have different response functions and the aggregate value for the propellant is a weighted average from the constituent columns.

#### 2.4 APPROACH

The analysis is performed in two parts. First, the model is derived in its steady-state version. The steady-state version serves to calculate mean values required for the time-dependent model, verify that the boundary conditions will be reasonably accurate as measured by the ability to reproduce experimental (or formal BDP) results, establish the zero-frequency (no oscillation) limit, verify some of the model assumptions, and provide an initial check on the method of solving for the temperature profile in the solid. The steady-state model is one of the subroutines of the computerized response function model. Secondly, the time-dependent model for the combustion response function is derived. In calculating the response function, experimental values of mean burning rate are used as input in order to minimize the effects of uncertainties in the steady-state modeling. The steady-state model is then limited to calculation of other steady-state quantities (e.g., surface temperature and flame height).

SECTION 3  
THE STEADY-STATE MODEL

3.1 SOLID PHASE EQUATIONS

The heat conduction equation in the melt layer is written as:

$$k_a \frac{d^2 T}{dx^2} + \rho_a c_a r \frac{dT}{dx} = W_a \rho_a Q_a A \exp(-E/RT) \quad (1)$$

where  $k$  = thermal conductivity

$\rho$  = density

$c$  = heat capacity

$W$  = weight fraction

$Q$  = heat of decomposition

subscript  $a$  = denotes AP

$A$  = kinetics prefactor

$E$  = activation energy

$R$  = gas constant

$r$  = burning rate

$T$  = temperature

$x$  = distance into the solid

The boundary conditions are:

$$x = 0, -k_a \frac{dT}{dx} = \rho_s c_s r (T_w - T_o) + W_a \rho_s r (Q_a + Q_m) \quad (2a)$$

$$x = x_m, -k_a \frac{dT}{dx} = \rho_s c_s r (T_m - T_o) + W_a \rho_s r Q_m \quad (2b)$$

where subscript  $w$  = denotes wall or surface

subscript  $s$  = denotes mean propellant

subscript  $m$  = denotes melt

subscript  $o$  = denotes the deep solid

Equation (1) may be written in dimensionless form as follows:

$$\frac{d^2\tau}{dy^2} + \frac{d\tau}{dy} = B \exp \left[ \frac{-E/RT_w}{\left( \frac{T_w - T_0}{T_w} \right) (\tau - 1) + 1} \right] \quad (3)$$

where  $\tau = (T - T_0) / (T_w - T_0)$

$$y = \frac{r}{\kappa} x$$

$\kappa$  = thermal diffusivity of the medium,  $\kappa_a$  for Eq. (3)

$$B = A \frac{\kappa_a}{r^2} H_a \frac{c_s}{c_a}$$

$$H = \frac{WQ}{c_s (T_w - T_0)}$$

In the thin melt layer,  $\tau \approx 1$ , so Eq. (3) may be approximated as:

$$\frac{d^2\tau}{dy^2} + \frac{d\tau}{dy} = C \exp [-D(1-\tau)] \quad (4)$$

where  $C = B \exp(-E/RT_w)$

$$D = \frac{E}{RT_w^2} \frac{(T_w - T_0)}{r^2}$$

The boundary conditions become:

$$\text{surface: } y = 0, \frac{d\tau}{dy} = -Z_a (1 + H_a + H_m) \quad (5a)$$

$$\text{melt/crystal: } y = y_m, \frac{d\tau}{dy} = -Z_a (\tau_m + H_m) \quad (5b)$$

$$\text{where } Z_a = \frac{\rho_s c_s}{\rho_a c_a}$$

Making the following transformation:

$$\xi = \tau + \frac{d\tau}{dy} \quad (6)$$

$$\eta = D(1-\tau) \quad (7)$$

Eq. (4) becomes:

$$(\xi - 1 + \eta/D) \frac{d\xi}{d\eta} = -\frac{C}{D} \exp(-\eta) \quad (8)$$

Recognizing  $\eta/D \ll 1$  where  $\tau \approx 1$ , and letting  $K = \frac{C}{D}$ , Eq. (8) becomes:

$$-\xi \frac{d\xi}{d\eta} + \frac{d\xi}{d\eta} = K \exp(-\eta) \quad (9)$$

Eqs. (5a & b) become:

$$\eta=0, \xi = \xi_w = 1 - Z_a(1+H_a + H_m) \quad (10a)$$

$$\eta=\eta_m, \xi = \xi_m = \tau_m - Z_a(\tau_m + H_m) \quad (10b)$$

Eq. (9) may be integrated in closed form. Applying Eqs.(10) and some algebra yields an expression for burning rate in the following form:

$$K = \frac{\xi_w \left( \frac{\xi_w}{2} - 1 \right) - \xi_m \left( \frac{\xi_m}{2} - 1 \right)}{1 - \exp(-\eta_m)} \quad (11)$$

Making all substitutions, burning rate is expressed as a function of wall temperature and other constants as follows:

$$r^2 = \frac{2 \kappa A W_a Q_a R T_w^2}{C_a(T_w - T_0) E(T_w - T_0)} \exp\left(-\frac{E}{R T_w}\right) \left[ 1 - \exp\left(-\frac{E}{R T_w} \frac{T_w - T_m}{T_w}\right) \right] \quad (12)$$

$$\left\{ Z_a \left[ 1 + \frac{W_a(Q_a + Q_m)}{C_s(T_w - T_0)} \right] \right\}^2 - \left\{ \left( \frac{T_m - T_0}{T_w - T_0} \right) (1 - Z_a) - Z_a \frac{W_a Q_m}{C_s(T_w - T_0)} - 1 \right\}^2$$

This relation is to be matched with a relation between burn rate and wall temperature from the gas phase model.

Analysis of the steady-state problem and, as will appear later, solution of the time-dependent problem, also require a description of the steady-state temperature profile in the solid. The temperature profile in the melt layer is determined from Eq. (9). Integration and application of Eq.(10a) yields:

$$\xi = 1 \pm \sqrt{1 + 2[K \exp(-\eta) - C_M]} \quad (13)$$

$$\text{where } C_M = K - \frac{1}{2} [1 - Z_a(1 + H_a + H_m)]^2 + 1 - Z(1 + H_a + H_m)$$

The physics of the temperature decay requires the negative root. Substituting the definitions for  $\xi$  and  $\tau$  yields:

$$\frac{d\xi}{dy} = -\xi + D \sqrt{1+2[K \exp(-\xi) - C_M]} \quad (14)$$

An order of magnitude analysis shows that the square root term will always be much larger than  $\xi$  in the melt layer. Thus, Eq. (14) reduces to the form:

$$\frac{d\xi}{\sqrt{a+b \exp(-\xi)}} = D dy \quad (15)$$

$$\text{where } a = 1 - 2C_M$$

$$b = 2K$$

This equation can be integrated in closed form for  $y(\xi)$ ; it is transcendental as  $\xi = \xi(y)$ .

$$y = \frac{-1}{D\sqrt{a}} \ln \left[ \frac{1+z - \sqrt{z^2 + 2z}}{1+d - \sqrt{d^2 + 2d}} \right] \quad (16)$$

$$\text{where } d = 2a/b$$

$$z = d \exp(\xi)$$

The melt layer thickness may be calculated by evaluating Eq. (16) at  $\xi = \xi_m$ .

For all layers beneath the melt layer, the right-hand-side of Eq. (3) vanishes. The gradient condition at the top of each layer is similar to Eq. (5b), without the heat of fusion.

$$y = y_{\text{Top}}, \frac{d\tau}{dy} = -Z \tau_{\text{Top}} \quad (17)$$

where  $Z = Z_a$  when entering an AP layer

$Z = Z_b$  when entering a binder layer

Thus the temperatures in each layer beneath the melt layer follow the recurring form:

$$\tau = \tau_{\text{Top}} - Z \tau_{\text{Top}} [1 - \exp(-\Delta y)] \quad (18)$$

where  $\Delta y$  = thickness of the particular layer, and uses the appropriate  $\kappa$ .

For a homogeneous propellant,  $Z=1$ , so Eq. (18) properly reduces to the result for a homogeneous propellant. Note also that the temperature and the gradient will properly tend to zero together, as  $y$  approaches infinity.

### 3.2 GAS PHASE EQUATIONS

If it is assumed that all reactions occur at the flame height, the heat conduction equation has the form of Eq. (1) with a zero right-hand-side. Taking the flame to be at  $x=0$  and the wall at the flame height ( $x=x^*$ ), the temperature distribution is:

$$T = T_f - (T_f - T_w) \frac{1 - \exp(-\zeta)}{1 - \exp(-\zeta^*)} \quad (19)$$

where  $\zeta = ux/\kappa_g$

$u$  = gas velocity normal to the surface

subscript  $g$  = denotes gas

subscript  $f$  = denotes flame

For convenience,  $\zeta$  is set equal to  $y$  by employing the continuity relation,  $\rho_g u = \rho_s r$ , and assuming that the ratio of heat capacity to thermal conductivity is equal for gas and solid<sup>4</sup>. Then the gradient at the wall may be written, from differentiation of Eq. (16), as:

$$y=y^*, \frac{dT}{dy} = - (T_f - T_w) \frac{\exp(-y^*)}{1 - \exp(-y^*)} \quad (20)$$

$$\text{where } y^* = \frac{rx^*}{\kappa_s}$$

4 This assumption is comparable to the general assumption that these properties are temperature-insensitive. The conductivities of propellant gases may be calculated, but are not well-known.

At the same time, the gradient at the wall must satisfy the energy requirements of the condensed phase:

$$-k_g \frac{dT}{dx} = \rho_s c_s r (T_w - T_0) + W_a \rho_s r (Q_a + Q_m) + W_b \rho_s r Q_b \quad (21)$$

where subscript b = denotes binder.

Eq. (21), when compared to Eq. (2a), states that the binder heat of decomposition is being positioned on the gas side of the wall. The binder does not appear at the surface in the model of Fig. 1, but does in reality exist over portions of the surface. The model surface is the AP melt. Therefore, in the framework of this model, the decomposing binder is external to the melt layer so may be represented by a heat absorption on the gas side. Eq. (21) may be re-written as:

$$y = y^*, - \frac{dT}{dy} = (T_w - T_0) + F \quad (22)$$

$$\text{where } F = (H_a + H_m + H_b)(T_w - T_0)$$

Equating Eq. (20) and Eq. (22) yields:

$$T_w = (T_f + F - T_0) \exp(-y^*) - (F - T_0) \quad (23)$$

which is the required matching relation in burn rate and wall temperature.

The remaining unknown,  $x^*$ , is determined by an approximate fit of the effective flame height from the BDP model:

$$x^* = C_F \frac{r D_1}{p} \quad (24)$$

where  $D_1$  = particle size

$p$  = pressure

$C_F = 24.6$  for  $r$  in cm/sec,  $p$  in atmospheres,  $D_1$  in microns and  $x^*$  in microns.

This form does not take into consideration the relative importance of the components of the BDP multiple flame structure and their differing dependencies upon the parameters of Eq. (21). However, it is a reasonable representation selected for mathematical convenience and with the perturbation analysis in mind.

After substitution of Eq. (21) into Eq. (18), Eqs. (12) and (20) are two equations for the unknowns  $r$  and  $T_w$ . These equations are solved by iteration. Once  $r$  and  $T_w$  are known, it is possible to calculate the melt layer thickness and the thermal profile in the solid.

The steady-state model is not intended to be used to calculate burning rates for multimodal propellants. That would require some definition of an effective particle size or flame height for use of Eq. (4). Rather, experimental values of burning rate are used to determine the wall temperature from the solid phase model, whence the effective flame height and particle size may be determined from the gas phase model. This is the general method for determining the mean values for use in the response function model. An option is provided to predict these values for unimodal propellants, but is used in this work only to validate aspects of the modeling. Those results are discussed in Section 5.

Note that the effects of particle size appear only as gas phase effects in the steady-state model. This conforms with a generally-accepted view of steady-state combustion (34). Although Eq. (12) (from the solid phase) may influence the magnitude of the particle size effect, particle size does not appear in that equation. The thermal profile in the solid does not enter into the calculation for mean burning rate. However, this does not preclude the importance of solid phase effects in determining the role of particle size in the time-dependent model for the response function.

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34. Derr, R.L., "Review of Workshop on Steady State Combustion Modeling of Composite Solid Propellants", 7th JANNAF Combustion Meeting (CPIA Publication 204, Vol. I, 1971) pp 1-8.

## SECTION 4

## THE TIME-DEPENDENT MODEL: CALCULATION OF THE RESPONSE FUNCTION

## 4.1 SOLID PHASE EQUATIONS

Using dimensionless quantities as previously defined, the time-dependent heat conduction equation in the thin melt layer is written as:

$$\frac{\partial^2 \tau}{\partial y^2} + \frac{\partial \tau}{\partial y} - \frac{\kappa a}{r^2} \frac{\partial \tau}{\partial t} = C \exp[-D(1-\tau)] \quad (25)$$

Eq. (25) is the time-dependent form of Eq. (4). Denoting mean values as barred and perturbed values as primed, and employing Eq. (4) to describe the mean portion, Eq. (25) may be written as:

$$\frac{\partial^2 \bar{\tau}'}{\partial y^2} + \frac{\partial \bar{\tau}'}{\partial y} - \Omega \frac{\partial \bar{\tau}'}{\partial (\omega t)} = C \exp(\tilde{\eta}) [\exp(D\tau') - 1] \quad (26)$$

where  $\omega$  = frequency of oscillations

$$\Omega = \frac{\kappa}{r^2} \omega$$

For harmonic perturbations,  $\tau' = \exp(i\omega t)$ , the time-dependent term of Eq. (26) may be re-written to provide an ordinary differential equation:

$$\frac{d^2 \tau'}{dy^2} + \frac{d\tau'}{dy} - i\Omega\tau' = C \exp(-\tilde{\eta}) [\exp(D\tau') - 1] \quad (27)$$

If  $\tau'$  is of second order of magnitude and  $\Omega$  sufficiently small, Eq. (27) may be approximated as:

$$\frac{d^2 \tau'}{dy^2} + \frac{d\tau'}{dy} = CD\tau' \exp(-\tilde{\eta}) \quad (28)$$

The problem is linearized to small perturbations, and is therefore restricted to linear instability. Variations in burning rate are of the order of variations in pressure, but variations in surface temperature are second or third order with respect to variations in burning rate. Thus, for second-order pressure perturbations,  $\tau'$  is at most of third order. The exponential in  $\bar{n}$  is approximately unity in the melt layer, and the product CD is of the order  $10^2$ . This would permit frequencies as high as 10KHz to satisfy the approximation for cases of interest. Since the quasi-steady assumption for the gas-phase model will also restrict the frequencies to values less than 10KHz, use of Eq. (28) is consistent with that assumption.

In applying the boundary conditions at the surface, one must recognize that the surface is fluctuating relative to the mean surface ( $y=0$ ) position. Since the fluctuating burning rate will also be of the form,  $\exp(i\omega t)$ , in the linearized problem, it follows that the surface position is given by:

$$y_S = -\frac{i}{\Omega} \frac{r'}{r} \quad (29)$$

The boundary conditions are:

$$y = y_S, \quad \tau' = \tau'_w \quad (30a)$$

$$\frac{d\tau'}{dy} = Z_a (g'_w + \frac{r'}{r} H_b) \quad (30b)$$

where  $g'_w$  = the gradient in  $\tau'$  at the surface, on the negative (gas) side of the boundary.

Eq. (30b) is derived by substituting Eq. (2a) into Eq. (21), and perturbing in the non-dimensional form. For small perturbations, the quantities at the actual surface may be related to the quantities at the mean surface as:

$$y = y_S, \quad \tau' = \tau'|_{y=0} - \frac{i}{\Omega} \frac{r'}{\bar{r}} \bar{g}|_{y=0} \quad (31a)$$

$$\frac{d\tau'}{dy} = g'|_{y=0} - \frac{i}{\Omega} \frac{r'}{\bar{r}} \frac{dg}{dy}|_{y=0} \quad (31b)$$

where  $\bar{g}$  = the gradient in  $\bar{\tau}$

Eq. (28) is integrated numerically. The functions  $\exp(-\bar{n})$  and  $\bar{g}$  are available in terms of  $y$  from Eq. (16). The integration provides the mean surface values, which are then converted to the actual surface values by means of Eqs. (31). The actual surface values must satisfy Eqs. (30);  $g'_w$  is determined from the gas phase model, and  $\tau'_w$  is related to  $r'$  by perturbing Eq. (12). The perturbation of Eq. (12) yields:

$$\frac{r'}{\bar{r}} = V_5 \tau'_w \quad (32)$$

$$\text{where } V_5 = (1 + \frac{\theta}{2})x + \frac{D}{2} \frac{1-2x(1-\tau_m)}{\exp[D(1-\tau_m)]-1} = \frac{1}{Z_a(1+H_a+H_m)-\tau_m(1-Z_a)+Z_a H_m+1}$$

$$\theta = E/(R\bar{T}_w)$$

$$x = (\bar{T}_w - T_0)/\bar{T}_w$$

Although the solution appears to require iteration, it will be shown subsequently that it does not (cf. Subsection 4.3).

For all layers beneath the melt layer, the right-hand-side of Eq. (27) vanishes so the time-derivative term cannot be neglected. Thus:

$$\frac{d^2\tau'}{dy^2} + \frac{d\tau'}{dy} - i\Omega\tau' = 0 \quad (33)$$

The boundary conditions at each interface are generally:

$$y=y_{\text{Top}}, \tau'=\tau'_{\text{Top}} \quad (34a)$$

$$\frac{d\tau'}{dy} = \frac{Z_{a,b}}{Z_{b,a}} g'_{\text{Top}} \quad (34b)$$

where the first Z subscript is used when entering an AP layer and the second is used when entering a binder layer. Assuming that the product  $\rho c$  for the melt is equal to that for the solid AP, the ratio of Z does not appear for that first layer of solid AP which joins the melt. The  $g'_{\text{Top}}$  refers to that value of the perturbed gradient on the negative (upper) side of the boundary, which drives the behavior below. The  $\tau'_{\text{Top}}$ , however, is preserved on the positive side. Eq. (34b) is similar in form to Eq. (30b), but there is no phase change heat beneath the melt layer and the sublayers do not oscillate relative to the mean surface. Eq. (33) may be integrated to produce the following recurring formulas:

$$\tau'=\tau'_{\text{Top}} \exp(\lambda_1 \Delta y) - \frac{\lambda_1 \tau'_{\text{Top}} - \frac{Z_{a,b}}{Z_{b,a}} g'_{\text{Top}}}{\lambda_2 - \lambda_1} [\exp(\lambda_2 \Delta y) - \exp(\lambda_1 \Delta y)] \quad (35)$$

$$\frac{d\tau'}{dy} = \lambda_1 \tau'_{\text{Top}} \exp(\lambda_1 \Delta y) - \frac{\lambda_1 \tau'_{\text{Top}} - \frac{Z_{a,b}}{Z_{b,a}} g'_{\text{Top}}}{\lambda_2 - \lambda_1} [\lambda_2 \exp(\lambda_2 \Delta y) - \lambda_1 \exp(\lambda_1 \Delta y)] \quad (36)$$

$$\text{where } \lambda_1 = -\frac{1}{2} - \frac{1}{2} \sqrt{1+4i\Omega}$$

$$\lambda_2 = -\frac{1}{2} + \frac{1}{2} \sqrt{1+4i\Omega}$$

Each layer uses the appropriate ratio of Z, and the appropriate  $\kappa$  for  $\Delta y$ ,  $\lambda_1$  and  $\lambda_2$ .

Eqs. (35) and (36) properly reduce to the results for a homogeneous solid ( $Z=1$ , and the difference between  $g'$  and  $\lambda_1 \tau'$  vanishes throughout, leaving only the first term on the right-hand-side). However, these equations retain the growing exponential term (in  $\lambda_2$ , of positive real part) for the layered solid because the formulation of the problem does not explicitly impose the boundary condition at infinity upon each layer. This condition is the requirement that  $\tau'$  and  $d\tau'/dy$  vanish together. For the homogeneous solid, this condition would immediately set the exponential in  $\lambda_2$  equal to zero. For the layered solid, it can only be said that a layer will eventually be reached where this condition may be approximated for all practical purposes. Since the effect of the heterogeneity on the perturbations also disappears when the perturbations disappear, this approximate condition may be expressed in the form of the homogeneous solid:

$$\tau' \rightarrow 0, \frac{d\tau'}{dy} \rightarrow \lambda_1 \tau' \quad (37)$$

In other words, there is a depth below which the propellant can be treated as homogeneous for purposes of the perturbation problem. Consider that this occurs below the  $N^{\underline{\text{th}}}$  AP layer. Then Eq. (37) may be expressed as:

$$y=y_N, \tau' = \epsilon \quad (38a)$$

$$\frac{d\tau'}{dy} = \lambda_{1s} \epsilon \quad (38b)$$

where  $\epsilon$  = an extremely small number

$\lambda_{1s}$  = value of  $\lambda_1$  using  $\kappa_s$  for the homogeneous region.

Eq. (38b) represents the perturbed gradient at the top of the homogeneous region, on the positive (homogeneous) side of the boundary with the  $N^{\underline{\text{th}}}$  AP layer. This may be converted to the perturbed gradient on the negative (AP) side of the

boundary through use of Eq. (34b), recognizing that  $Z=1$  in the homogeneous region. Thus, Eqs. (38) become:

$$y = y_N, \quad \tau'_{TopN} = \epsilon \quad (39a)$$

$$g'_{TopN} = Z_a \lambda_{ls} \epsilon \quad (39b)$$

where subscript  $TopN$  = denotes the bottom of the  $N^{th}$  AP layer, which would be the "top" condition for the succeeding homogeneous region were the calculation to continue.

Thus, the problem of the solid phase is now properly closed. Eqs. (30) define the conditions at the "top", and Eqs. (39) define the conditions at the "bottom". The conditions at the bottom are now known, but the conditions at the top depend upon the gas phase. Additional discussion with respect to the solution for the solid phase is deferred to Subsection 4.3.

#### 4.2 GAS PHASE EQUATIONS

The perturbed form of Eq. (24) is simply:

$$\frac{x^*'}{\bar{x}^*} = \frac{r'}{\bar{r}} - \frac{p'}{\bar{p}} \quad (40)$$

Since the analysis will take into account flame temperature perturbations, a relation between the flame temperature perturbations and the wall temperature perturbations is required. This is obtained by perturbation of Eq. (23). Using dimensionless quantities as previously defined, Eq. (40) for the flame standoff perturbations, and linearizing the exponential in perturbed quantities, there results:

$$\tau'_f = \tau'_w \exp(\bar{y}^*) - (1+\tau_F)\bar{y}^* \exp(\bar{y}^*) \left[ \frac{p'}{\bar{p}} - 2 \frac{r'}{\bar{r}} \right] \quad (41)$$

$$\text{where } \tau_F = \frac{F}{\bar{T}_w - T_0}$$

The perturbed gradient on the gas side of the wall is derived from an energy balance. The energy being transmitted into the solid is the difference between the heat release in the gas and the energy required to raise the gas from the wall temperature to the flame temperature:

$$-k_g \frac{dT}{dx} = -\rho_s r Q_f - c_g (\bar{T}_f - \bar{T}_w) \quad (42)$$

where  $Q_f$  = heat release in the gas (negative for an exotherm).

Using the same relation between gas and solid thermal properties as led to Eq. (20), Eq. (42) may be written in dimensionless form as follows:

$$\bar{q}_w = H_f + (\bar{\tau}_f - 1) \quad (43)$$

where  $\bar{q}_w$  = gradient in  $\bar{\tau}$  at the wall on the negative (gas) side

$$H_f = \frac{Q_f}{c_g (\bar{T}_w - T_0)}$$

The perturbed dimensionless form of Eq. (42) is:

$$q_w' = \frac{r'}{r} [H_f + (\bar{\tau}_f - 1)] + (\bar{\tau}_f' - \bar{\tau}_w') \quad (44)$$

$H_f$  may be eliminated by combining the relations in Eqs. (43), (5a) and (21)<sup>5</sup>.

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5 For this purpose, Eq. (21) may be written as:  $d\bar{\tau}/dy = Z(\bar{q}_w + H_f)$ . This is the steady-state analog of Eq. (30b), and comes from substituting Eq. (2a) into Eq. (21) in dimensionless form.

$$H_f = -(\bar{\tau}_f - 1) - (1 + \tau_F) \quad (45)$$

Substitution into Eq. (44) yields:

$$g_w' = -\frac{r'}{r} (1 + \tau_F) + (\tau_f' - \tau_w') \quad (46)$$

Substitution of Eq. (41) into Eq. (46) yields, after combining terms:

$$g_w' = \frac{r'}{r} (1 + \tau_F) (2\bar{y}^* \exp(\bar{y}^*) - 1) + \tau_w' (\exp(\bar{y}^*) - 1) - \frac{p'}{p} (1 + \tau_F) \bar{y}^* \exp(\bar{y}^*) \quad (47)$$

Eq. (47) is the necessary matching relation for Eq. (30b). Thus, the formulation of the time-dependent problem is complete.

Eq. (45) also may be substituted into Eq. (43) to yield:

$$\bar{g}_w = -(1 + \tau_F) \quad (48)$$

Eq. (48) is the dimensionless form of Eq. (22), so consistency is verified in this respect.

#### 4.3 SOLUTION FOR THE RESPONSE FUNCTION

By combination of Eqs. (30b), (31a), (31b), (32) and (47), it is possible to derive an explicit expression for the response function in terms of solid phase constants, gas phase constants and one key parameter characteristic of the solution for the solid phase. This key parameter is the ratio of the perturbed gradient to the perturbed temperature at the mean surface:

$$\left. \frac{g'}{\tau'} \right|_{y=0} = K_2 \quad (49)$$

The components of this ratio appear individually in Eqs. (31), and the ratio is defined here as  $K_2$ . In the classical homogeneous theory, this ratio is always  $\lambda_1$ . In this work, the ratio will depend upon the modeled heterogeneity and  $\lambda_2$  as well as on  $\lambda_1$ .

The expression for the response function is:

$$R = \frac{\Omega_a V_{6B}}{\Omega_a \left[ \frac{V_{6A}}{V_5} + 2V_{6B} - \frac{V_3}{Z_a} \right] + i \frac{C}{Z_a} - \frac{K_2}{Z_a} \left[ \frac{\Omega_a}{V_5} - i V_3 \right]} \quad (50)$$

Where  $R$  = response function

$$V_3 = Z_a (1 + H_a + H_m) \text{ (see Eq. [5a])}$$

$$V_5 = \text{(see Eq. [32])}$$

$$C = \text{(see Eq. [4])}$$

$$V_{6A} = (\exp(\bar{y}^*) - 1) \text{ (see Eq. [47], appears as coefficient of } \tau_w' \text{)}$$

$$V_{6B} = (1 + \tau_F) \bar{y}^* \exp(\bar{y}^*) \text{ (see Eq. [47], appears as coefficient of } p'/\bar{p} \text{ and as part of the coefficient of } r'/\bar{r}).$$

If the ratio  $K_2$  depended upon  $\tau_w'$  and  $\tau_w$ ' separately, the problem would require an iterative solution. However, it turns out that  $K_2$  is an intrinsic property of the solid phase, independent of the surface boundary condition, just as is  $\lambda_1$  for the homogeneous solid. The reason is that the solid phase is described by linear homogeneous differential equations. All solutions of such equations of second order are of the form:

$$f = C_1 f_1(x) + C_2 f_2(x)$$

where  $f$  = denotes functions

$C_1$  = first arbitrary constant

$C_2$  = second arbitrary constant

The gradient is:

$$g = C_1 f_1'(x) + C_2 f_2'(x)$$

It is required that  $g/f$  go to  $\lambda_1$  in the deep solid. This constitutes one of the two boundary conditions that can be imposed. Therefore,  $C_1$  and  $C_2$  cannot be independent. Solving for  $C_2$  in terms of  $C_1$ :

$$C_2 = C_1 \frac{f_1'(\infty) - \lambda_1 f_1(\infty)}{\lambda_1 f_2(\infty) - f_2'(\infty)}$$

Substitution of this expression for  $C_2$  into the ratio,  $g/f$ , followed by algebraic simplification, leads to the result that  $g/f$  depends upon the ratio  $C_2/C_1$  and not upon  $C_1$  and  $C_2$  independently. Of course,  $g/f$  will vary from case to case and will vary with  $x$  for a given case; the important point is that it depends only on the ratio  $C_2/C_1$  and  $x$ . This property was first observed numerically in the course of a prototypal computer program which was based upon an iterative scheme. Accordingly, it suffices to go through Eqs. (35) and (36) in the layers, beginning with Eqs. (39)<sup>6</sup>, and then solve numerically through the melt layer, just one time for  $K_2^7$ . Knowing  $K_2^7$ , Eq. (50) for  $R$  is solved by complex arithmetic<sup>8</sup>.

It is of interest to examine the form of Eq. (50) in comparison to the form obtained from the homogeneous theory (Ref. 16). The latter can be written as:

$$R = \frac{\Omega n AB}{\Omega [AB - (1+A)] + iA - \lambda_1 [\Omega - iA]} \quad (51)$$

where  $n$  = pressure exponent

$A$  = a solid phase parameter, not to be confused with  $A$  as defined in Eq. (1)

$B$  = a gas phase parameter, not to be confused with  $B$  as defined in Eq. (3)

$\lambda_1$  = as defined in Eqs. (35, 36); it is of opposite sign in Ref. (16).

6 Subroutine LAYRSP of the computer program.

7 Subroutine MLTLRP of the computer program.

8 Subroutine GLTFP of the computer program.

It is noted that Eqs. (50) and (51) are identical in form and, to some extent, they are similar in substance. The parameter  $V_{6B}$  combines condensed phase and gas phase terms, as does  $(nAB)$  of Eq. (51). The parameters  $C$  and  $V_3$ , although different, are condensed phase terms as is  $A$  of Eq. (51). The parameter  $V_{6A}$  is a gas phase term, as is  $B$  of Eq. (51). The parameter  $V_5$  is related to  $C$ , and, therefore, a part of the analogy to  $A$ ; but important differences from  $A$  derive from the finite melt layer. The parameter  $K_2$  is the heterogeneous analog of  $\lambda_1$ . The parameter  $Z_a$  is purely a consequence of the heterogeneity, so there would be no analog for it in Eq. (51). The identity in form, and the similarity in substance, suggests that the heterogeneity as described by this model will not produce radical changes in the qualitative behavior of the response function.

The zero-frequency limit of Eq. (51) is the pressure-exponent,  $n$ . Pressure exponent does not appear explicitly as such in the steady-state model described herein. Nevertheless, it is of interest to examine the zero-frequency limit of Eq. (50). It is readily apparent that a non-zero response function at zero frequency requires that the following relationship be satisfied:

$$\lim_{\Omega_a \rightarrow 0} K_2 = -\frac{C}{V_3} \quad (52)$$

The satisfaction of Eq. (52) is verified by combining Eqs. (31), (32), (5a), the derivative of Eq. (15) applied at  $y=0$ , and a perturbation of Eq. (2a). In general,  $K_2$  must be solved numerically, but at zero frequency it is possible to derive an expression which reduces to  $-C/V_3$ . Since Eq. (52) is satisfied, the indeterminate form of Eq. (50) that results may be evaluated to yield the non-zero response function:

$$\lim_{\Omega_a \rightarrow 0} R = \frac{V_{6B}}{2V_{6B} + \frac{1}{V_5}(1+V_{6A})} \quad (53)$$

Eq. (53) may be thought of as an "effective" pressure exponent, extracting an implicit property of the model. Note that it depends upon condensed phase terms as well as gas phase terms. Numerically, it is found to be consistent with pressure-dependence as calculated from results of the steady-state model.

SECTION 5  
MODEL RESULTS

5.1 THE STEADY-STATE MODEL

Results of the steady-state model have been obtained in order to evaluate some of the important model premises. The essential results are tabulated in Table I.

Table I presents various results, compared with data and with BDP model results, for A-13 propellant used as a standard case. The first set of results compares burning rate as a function of pressure. The model results compare very well with the data. It should be emphasized, however, that these results should not be construed to imply that this model is "better than" the BDP model. The second set of results compares surface temperature. Experimental values of surface temperature are reportedly in the neighborhood of 850°K (26). It is observed that this model produces higher surface temperatures and a somewhat greater sensitivity to pressure than does the BDP model. However, the results are reasonable. The results also confirm the assumption that variations in surface temperature are second order (or smaller) with respect to variations in burning rate. The third set of results compares flame standoff distance. This model uses one flame. The BDP results are for the primary flame (sum of diffusion and reaction heights), and the values to the right of the slash are for the AP monopropellant flame when that flame moves closer to the surface than the primary flame. When that happens, the BDP model employs an energy partitioning which may be thought of as some single flame having an effective height between the two shown. On that basis, the flame heights from this model are roughly a factor of 3 greater than from the BDP model, but the qualitative behavior with pressure is the same. The value of  $C_F$  in Eq. (24) was adjusted to achieve good agreement with the burning rate data; values of other constants

TABLE I

## COMPARISONS OF BURNING RATE AND OTHER QUANTITIES FOR A-13 PROPELLANT

BURNING RATE

<u>PRESSURE (PSIA)</u>	<u>DATA (cm/sec)</u>	<u>FROM BDP MODEL</u>	<u>FROM THIS MODEL</u>
100	0.27	0.29	0.28
300	0.41	0.39	0.47
500	0.52	0.47	0.55
700	0.62	0.53	0.65
900	0.73	0.60	0.74
1100	0.85	0.65	0.83

WALL TEMPERATURE

100	---	824°K	864
300	---	836	900
500	---	844	937
700	---	851	973
900	---	855	982
1100	---	859	986

FLAME HEIGHT

100	---	25.6μm	82.9
300	---	20.7	50.8
500	---	19.9/18.3	35.7
700	---	19.5/5.7	30.2
900	---	19.4/3.1	25.8
1100	---	19.3/3.1	23.6

are the same as used in the BDP model. It is concluded that, for purposes of the time-dependent analysis, the model conforms reasonably well with steady-state reality.

The ability to reproduce measured effects of AP particle size on burning rate was tested with a series of propellants analogous to A-13. These propellants were the subject of a low pressure L\* instability study performed by Ramohalli (35). The comparison of burning rates at 100 psia is as follows:

PARTICLE SIZE ( $\mu\text{m}$ )	DATA (cm/sec)	MODEL (cm/sec)
40	0.41	0.38
90	0.27	0.28
200	0.23	0.19
360	0.19	0.13

Again, the agreement is reasonable.

There are two other aspects of the steady-state model results which merit discussion: The melt layer and the heterogeneity in relation to the thermal wave.

The melt layer thickness is computed to be of the order of microns or less, which is consistent with experimental observation and the thin melt layer assumption. Its dependence upon heating rate involves a tradeoff between surface temperature and the steepness of the thermal gradient. Theoretically, it will disappear at such low burning rate that the surface temperature does not reach the AP melting point, and also will approach zero at very high burning rate where the gradient is very steep. Although the layer is thin, it was considered improper to neglect it for mathematical convenience because the characteristic time of its dimension corresponds to the high frequencies of interest.

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35. Kumar, R. N. and McNamara, R. P., "Some Experiments Related to L-Star Instability in Rocket Motors", AIAA Paper 73-1300 (Nov., 1973).

For particle sizes in excess of  $40\mu\text{m}$ , the thermal wave will not penetrate the first AP layer under conditions of interest. The implication is that, except for the melt layer, the solid can be considered homogeneous in determining its role. However, this is not true for the fine sizes which are generally utilized in practical propellants. An estimate for a  $2\mu\text{m}$  AP propellant reveals that, at 1000 psi, the temperature does not fall to within 10 percent of the bulk temperature until about 5 pairs of AP-binder layers are traversed. Further, if the  $2\mu\text{m}$  AP is a component of a multimodal propellant, the burn rate will be lower such that the thermal wave will penetrate more layers of the column consisting of the  $2\mu\text{m}$  AP. As a result, it appears that the role of solid phase heterogeneity will be limited to melt layer heterogeneity in the intermediate-coarse size regime, but that in-depth heterogeneity can be important in the fine size regime. This distinction is one consequence of the present fixed-geometry model; were the layers permitted to move to evoke the pulsation mechanism, then the in-depth heterogeneity could be important for all sizes. The distinction was considered significant in view of the experimental importance of fine AP (15).

## 5.2 THE TIME-DEPENDENT MODEL

The effects of the solid phase heterogeneities are most likely to appear at combinations of fine AP and low burning rate. Therefore, a test case consisting of a  $2\mu\text{m}$  AP propellant at a burning rate of 0.47 cm/sec was selected for evaluation. Except for the particle size, this test case would correspond to A-13 propellant at 300 psi. Results are shown in Figure 3. The solid line is for the heterogeneous propellant. The long-dash line is for AP and binder thermal properties equal to mean propellant thermal properties; therefore, it is for melt layer

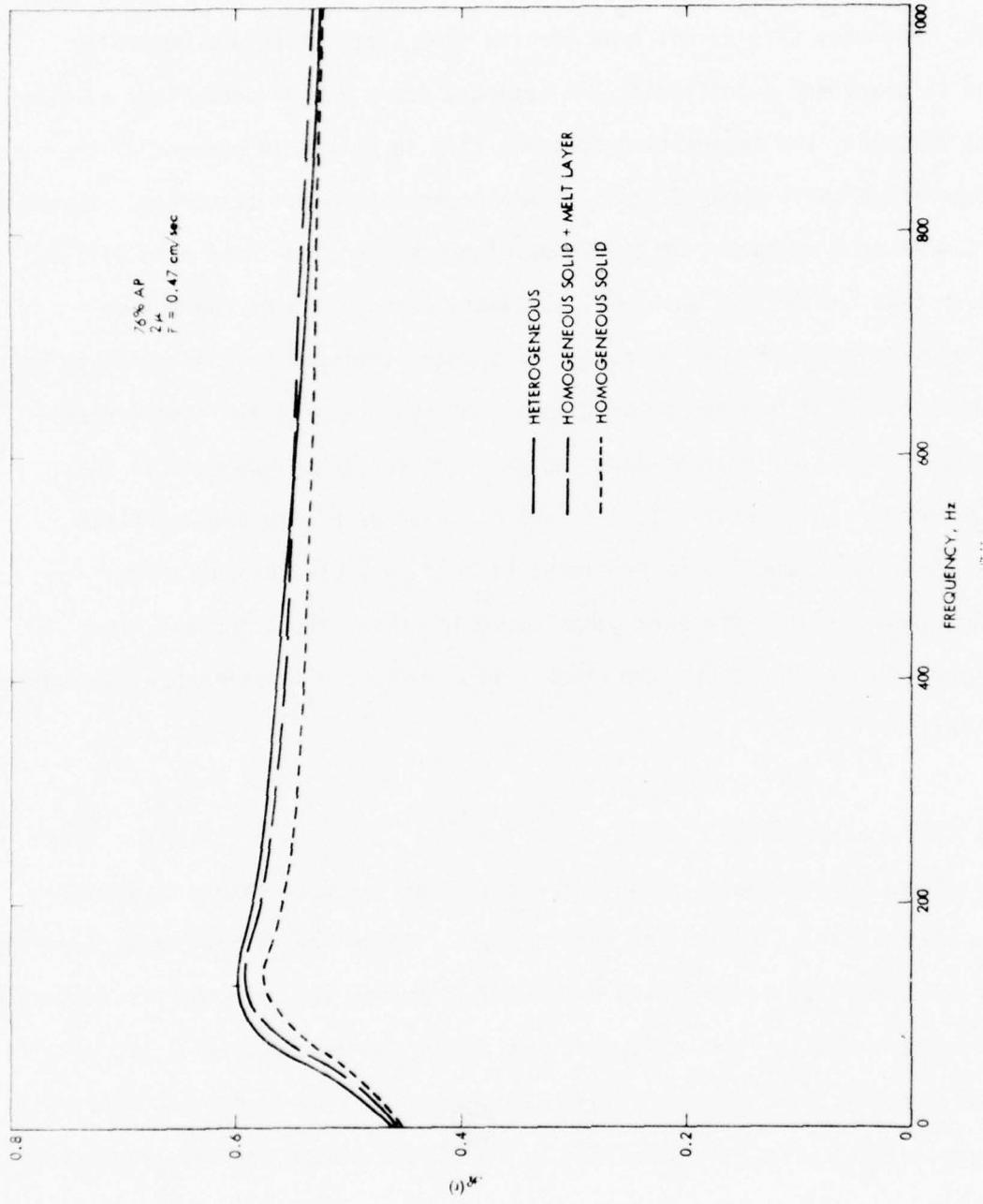


Figure 3. Response Function Calculations for a  $2 \mu$ AP Analog of A-13 Propellant

heterogeneity only, the propellant below the melt layer being homogeneous<sup>9</sup>. The short-dash line is for a completely homogeneous solid; i.e., the distributed heat release in the finite melt layer is now concentrated at the surface only and the entire region beneath the surface is homogeneous<sup>10</sup>. It is observed that the effects of the heterogeneities are small.

Figure 4 compares results for a 90 $\mu\text{m}$  AP propellant, which is A-13 propellant, with the Figure 3 results. Thus, the effect of particle size at a constant burning rate is shown. In the framework of this model, a constant burning rate implies a constant wall temperature and constant dimensionless flame properties; thus, any difference is due to solid phase heterogeneities. An effect of the heterogeneity does appear, but again, it is small. It is noted that the results for A-13 are virtually identical to the homogeneous solution displayed in Figure 3. In the case of A-13, the thermal wave does not penetrate the surface AP layer and the melt layer thickness is about 1 percent of the particle size; thus, the solid is homogeneous for all practical purposes. In the case of the 2 $\mu\text{m}$  propellant the thermal wave penetrates 15 AP layers and the melt layer thickness is about one-third (1/3) of the particle size; thus, the solid is heterogeneous, but the effect of the heterogeneity appears to be small. Significantly, the effect is small with respect to peak response

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9  $k_a = k_b = k_s$ ;  $\rho_a = \rho_b = \rho_s$ ;  $c_a = c_b = c_s$ ;  $Z = 1$ .

10  $V_3 = C = Z = 1$ ;  $K_2 = \lambda_1$ ;  $V_5 = 0 \cdot x$ . This would correspond to the Denison and Baum model except for differences in the modeling of the gas phase, and differences in the values of combustion constants due to the use of this model (including the finite melt layer) to reproduce steady-state burning rates.

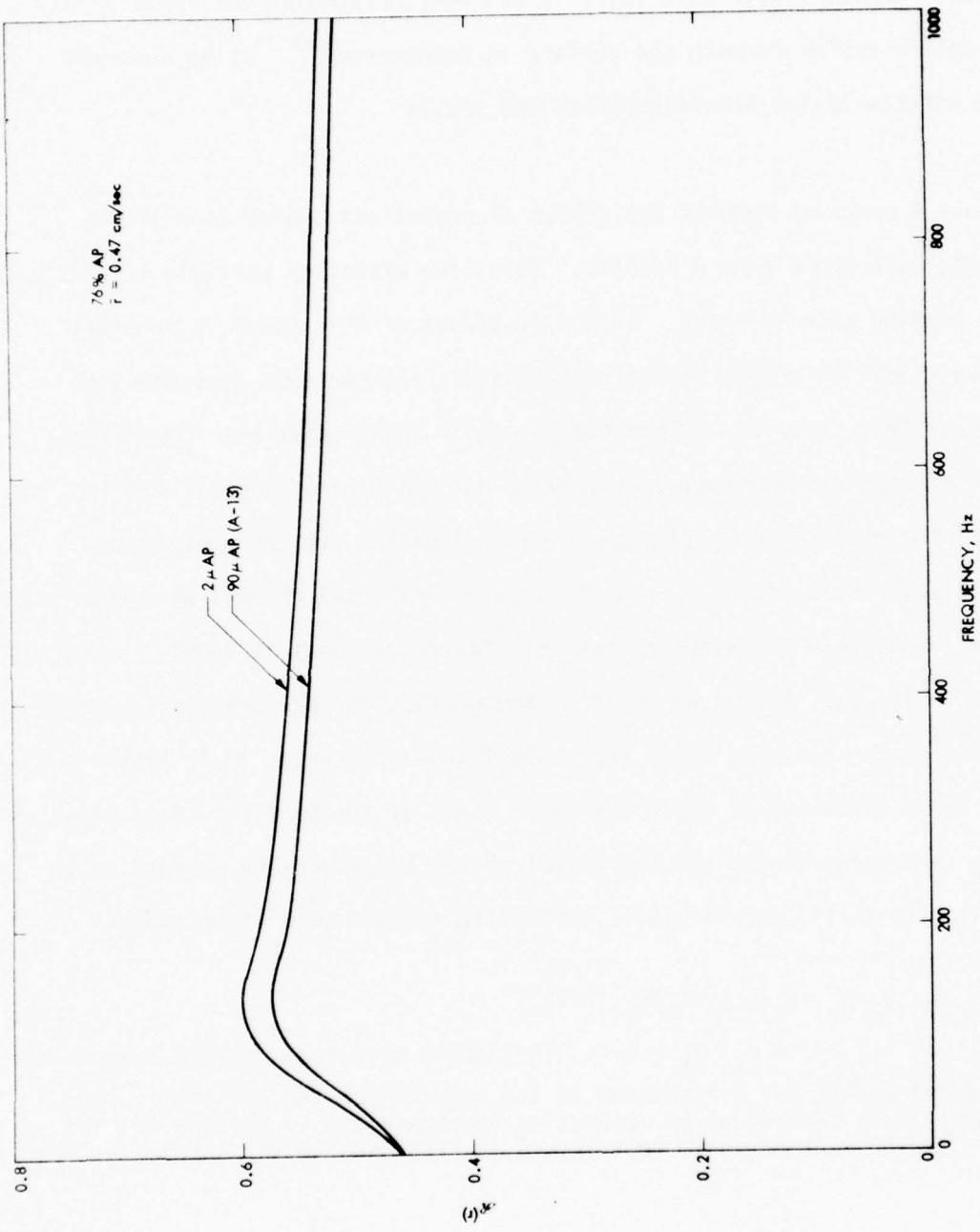


Figure 4. Effect of AP Particle Size at Constant Burning Rate for A-13 Type Propellant

frequency as well as magnitude. Thus, it can be concluded that the expected effects of the heterogeneity are not being represented by this model.

The theoretical results for the A-13 propellant, moreover, do not agree with experimental data. The A-13 is a JANNAF standard propellant, and has been well-characterized in T-burner testing (Ref. 36). The experimental peak response is about 4 and occurs at roughly 300 Hz. Thereafter, the response declines to a value of approximately 1.5 at 1000 Hz. The theoretical results presented in Figure 4 show a peak response of 0.58 at 125 Hz, and a value of 0.51 at 1000 Hz. Therefore, the theory shows a relatively slight peak and at too low a frequency. Such theoretical results are a consequence of the combustion parameters, analogous to the "A" and "B" (or " $\alpha$ ") parameters of the Denison & Baum model. Presumably, the agreement with data could be improved by selection of a different set of parameters. However, a ground rule of this study was that the parameters would be predetermined by considerations of a credible steady-state model. Given that model, it is inappropriate to change the constants arbitrarily. According to Ref. (27), a relatively large value of the "B" (or " $\alpha$ ") parameter will constrain the time-dependent model to the prediction of small peaks, and a relatively small value of the "A" parameter will produce low peak response frequencies. By analogy, that is the situation here. Since it would be inappropriate to juggle parameters, it must be concluded that there is a mechanistic deficiency in the time-dependent model that has been postulated here.

Figure 5 presents theoretical results showing the effect of burning rate for a constant particle size. The  $2\mu\text{m}$  AP propellant was selected for this illustration.

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36. "T-Burner Manual", CPIA Publication 191 (Nov., 1969).

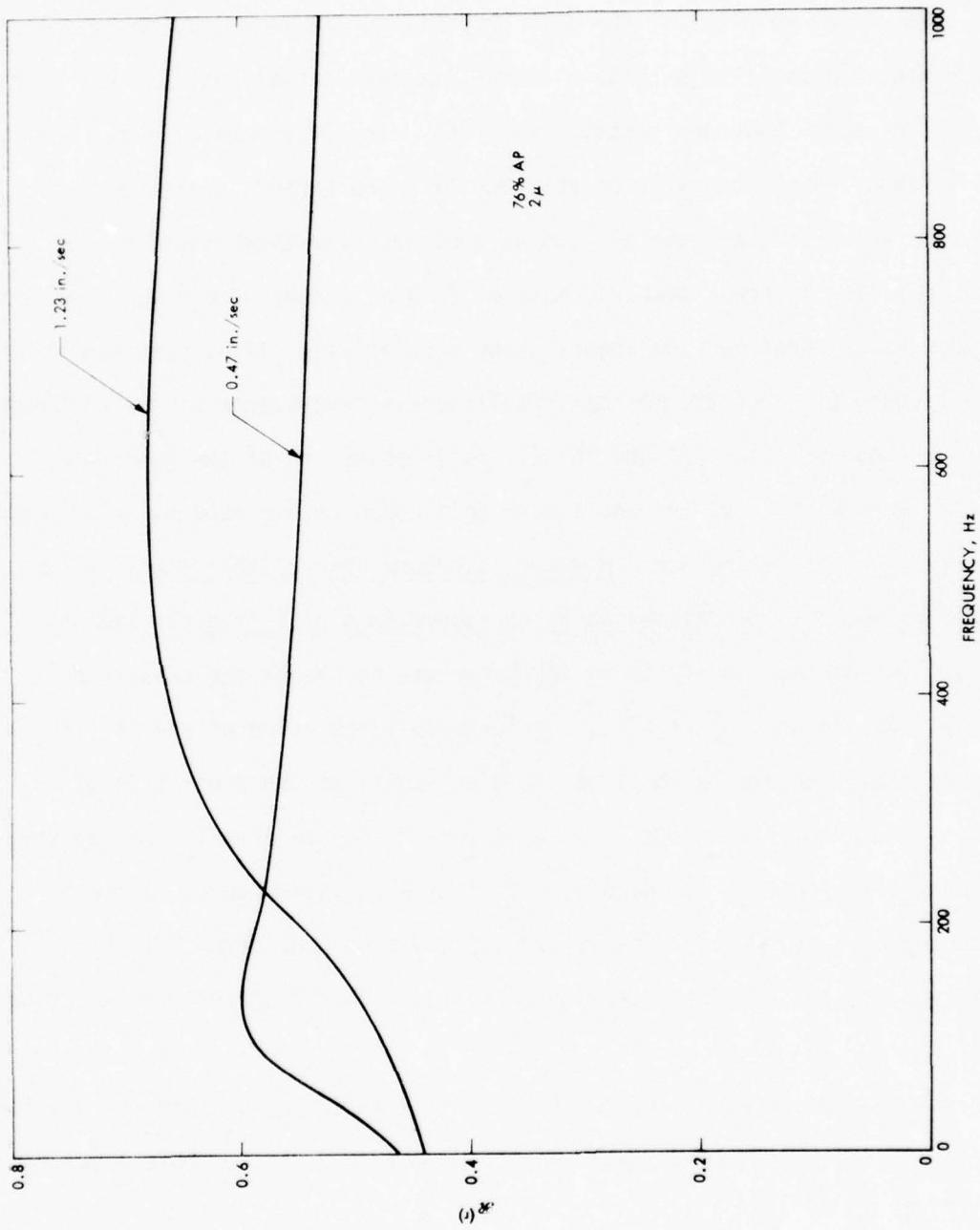


Figure 5. Effect of Burning Rate at Constant AP Particle Size for the  $2\mu$  Analog of  
A-13 Propellant

The higher burning rate is representative of this propellant; the lower burning rate may be thought of as a suppression for purposes of Figures 3 and 4. The effect on peak response frequency demonstrates further that the modeled heterogeneities are of little consequence. It is observed that the peak response frequency varies nearly with the square of the burning rate, which is the result for homogeneous propellants. On the other hand, the Figure 3 and 4 results show that the effect of the heterogeneity on peak response frequency is about 10 percent. According to the Cohen postulates for the effect of heterogeneity, the peak response frequency in Figure 5 should vary with the first power of burning rate, and in Figure 4 it should vary inversely with particle size. These effects are not being produced by this model.

Figure 6 compares theoretical results with experimental data for a bimodal propellant. Although the shape of the theoretical curve is reasonable, the peak response magnitude and frequency are again underpredicted. Also, the zero frequency limit is overpredicted, reflecting a deviation from the measured steady-state pressure exponent. It appears that further work is necessary in order to implement a proper mechanism for the combustion response.

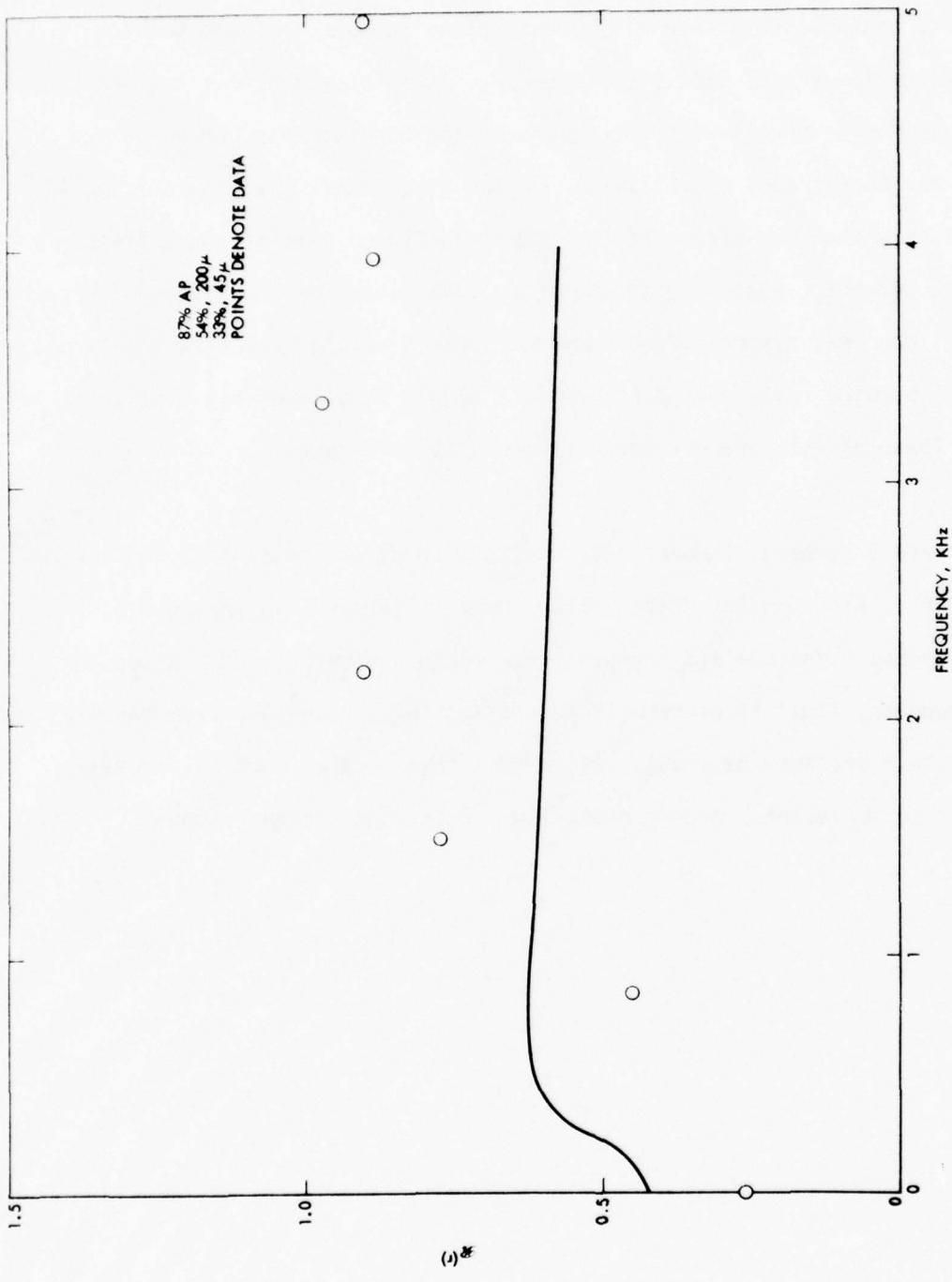


Figure 6. Comparison of Theory and Experiment for SP-540 Propellant at 500 psi

SECTION 6  
CONCLUSIONS AND RECOMMENDATIONS

An analytical model has been developed which incorporates mechanisms of solid phase and gas phase heterogeneities into the calculation of steady-state and linear time-dependent combustion properties of composite solid propellants. Although the model satisfactorily describes the steady-state combustion properties, it is deficient in describing the time-dependent combustion response characteristics in several respects. Use of a consistent set of combustion constants produces peak response magnitudes and frequencies which are too low in comparison to experimental data and which are not significantly affected by the AP particle size per se. Although an effect of the solid phase heterogeneities is predicted by this model, the effect is quantitatively so small as to allow it to be neglected in future work. Therefore, the role of AP cannot be attributed to the solid phase alone unless some other mechanism is incorporated into the theory. It is recommended that the concept of moving layers be re-examined, including justification for the coherence of such a mechanism. It is further recommended that the perturbed BDP model be examined as a potentially useful way in which to represent the heterogeneity of the gas phase. It is desired not only to achieve the effects of the heterogeneity, but also to justify a set of values of the combustion constants that will properly position the response function curve. It appears necessary to modify both the solid phase and gas phase models in order to achieve those purposes in a consistent manner.

## SECTION 7

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APPENDIX A  
COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL COMPUTER PROGRAM

This appendix presents information essential to the utilization of the composite Solid Propellant Combustion Response Model (CSP CRM) computer program. This information is presented under the following headings and in the order listed:

1. Definitions of Input Data
2. Input Deck Corresponding to the Example Problem.
3. Definitions of Output Data
4. Card Image Listing of Program.
5. Description of Program Logic, Subroutines and Use of Text Equations
6. Solutions to Example Problem

#### A-1. DEFINITIONS OF INPUT DATA

All input to the Composite Solid Propellant Combustion Response Model Computer Program is made by means of a NAMELIST/INPUT statement and an associated read statement, both of which appear in the DATAIN subroutine. The FORTRAN names of the input variables and parameters, together with their corresponding algebraic symbols and brief definitions are presented below in the exact order that they appear in the INPUT list:

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
CA	$c_a$	specific heat at constant pressure for the oxidizer (cal g <sup>-1</sup> °K <sup>-1</sup> , real)
CB	$c_b$	specific heat at constant pressure for the binder (cal g <sup>-1</sup> °K <sup>-1</sup> , real)
CG	$c_g$	specific heat at constant pressure for the combustion gas mixture that exists between the gas-condensed phase interface and the flame front (cal g <sup>-1</sup> °K <sup>-1</sup> , real)
KA	$k_a$	thermal conductivity of the oxidizer (cal sec <sup>-1</sup> cm <sup>-1</sup> °K <sup>-1</sup> , real)
KB	$k_b$	thermal conductivity of the binder (cal sec <sup>-1</sup> cm <sup>-1</sup> °K <sup>-1</sup> , real)
RØA	$\rho_a$	density of the oxidizer (g cm <sup>-3</sup> , real)
RØB	$\rho_b$	density of the binder (g cm <sup>-3</sup> , real)
WAC(J)	$w_a(j)$	fraction of composite solid propellant mass attributable to the jth size component of the oxidizer ( $j \leq 4$ ) (dimensionless, real)
SMLA(J)	$a_j$ or $D_j$	diameter of jth size component oxidizer particles ( $j \leq 4$ ) (cm, real) Note: Must be listed in order of increasing particle size.
E	E	activation energy for decomposition of the oxidizer (cal. g-mole <sup>-1</sup> , real)
R	R	universal gas constant (cal. g-mole <sup>-1</sup> °K <sup>-1</sup> , real)

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
PRXFAC	A	prefactor in the Arrhenius expression for oxidizer decomposition (sec <sup>-1</sup> , real)
QS	Q <sub>a</sub>	gross heat of decomposition of the oxidizer (equals net heat of decomposition of the oxidizer minus latent heat of melting of the oxidizer) cal g <sup>-1</sup> , real)
QB	Q <sub>b</sub>	heat of decomposition of the binder ( cal g <sup>-1</sup> , real)
QLM	Q <sub>m</sub>	latent heat of melting of the oxidizer ( cal g <sup>-1</sup> , real)
KFLMHT	CF	CF = $\bar{p}x^*/(\bar{r}D_1)$ constant of proportionality in the rational algebraic approximation to BDP effective flame height (atmos sec $\mu\text{m}^{-1}$ , real)
TFLM	T <sub>f</sub>	adiabatic temperature of the gas-phase combustion flame sheet ( $^{\circ}\text{K}$ , real)
TM	T <sub>m</sub>	melting temperature of the oxidizer ( $^{\circ}\text{K}$ , real)
TZRØ	T <sub>o</sub>	temperature in the composite solid propellant far from the gas-condensed phase interface ( $^{\circ}\text{K}$ , real)
PBAR	$\bar{p}$	temporal mean pressure in the gas phase---assumed to be uniform (atmos, real)
RBR	$\bar{r}$	temporal mean rate of regression of the composite solid propellant; no input if ITERA=1 (cm sec <sup>-1</sup> , real)
TØL	-	arbitrary tolerance employed in the steady-state part of the computer program to evaluate convergence of the steady-state solution (dimensionless, real, usually $10^{-3} \leq TØL \leq 10^{-5}$ )
ITERA	-	specifies the mode of operation of the computer program: If ITERA=0, the program determines the combustion response parameters for a CSP whose temporal mean regression rate is specified; if ITERA=1, the program determines the temporal mean regression rate for a propellant whose basic physical and chemical characteristics have been specified (dimensionless, integer).

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
N5MAX	-	<p>if ITERA=1 and if a satisfactory value for RBR has not been achieved after N5MAX-1 one-percent increments or decrements of RBR, the solution will be terminated and an appropriate comment will be printed in the computer output (dimensionless, integer, <math>5 \leq N5MAX \leq 20</math>)</p> <p>Note: This mode of program termination indicates an injudicious initial choice for RBR.</p>
NPP	$p'/\bar{p}$	<p>normalized pressure perturbation (dimensionless, polar complex) Note: This is the exciter of the perturbation; as such, its phase is arbitrarily set equal to zero</p>
TAPIN	$\tau'_{y>0}$	<p>normalized temperature perturbation applied in the solid phase at a distance from the gas-condensed phase interface that is several times the characteristic transient thermal depth within the solid. (dimensionless polar complex)</p> <p>Note: Since the ratio, <math>(g'/\tau')_{y=0}</math>, obtained from the solid phase solution is independent of the argument assumed for <math>\tau'</math>, the argument is ordinarily arbitrarily set equal to zero.</p>
YTD		<p>factor which, when multiplied by SQRT (KAPS/OMEGA), provides a value of <math>x&gt;0</math>, viz., XTD (dimensionless, usually assumed to be an integer <math>\geq 3</math>)</p> <p>Note: SQRT (KAPS/OMEGA) is a measure of the depth of penetration of the perturbation into the CSP</p>
OMEGA	$\omega$	assumed angular frequency of the perturbation (radians sec <sup>-1</sup> , real)
NEQ	-	number of differential equations solved in subroutine SVDQ---always equal to one in this computer program (dimensionless integer)
KD	-	order of the differential equations solved in subroutine SVDQ--- always equal to two in this computer program (dimensionless, integer)
MXSTEP	-	maximum number of steps allowed between output points in subroutine SVDQ---usually set equal to one hundred in this computer program (dimensionless, integer)
EP	-	parameter used to control local error in subroutine SVDQ---refer to description of subroutine for guidance in setting the value of this parameter (dimensionless, real)

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
IHOMO	-	When IHOMO=0, certain pertinent physical and thermal properties of the propellant binder, oxidizer, and gaseous products specified in namelist/input/are generally distinct; however, when IHOMO=1, these properties are set equal to corresponding properties of the oxidizer. Thus, specifying IHOMO=1 implies a homogeneous propellant (dimensionless, integer)

## A-2. INPUT DECK CORRESPONDING TO THE EXAMPLE COMPUTER RUN

### A-3. DEFINITIONS OF OUTPUT DATA

All permanent output of the Composite Solid Propellant Combustion Response Model (CSP CRM) Computer Program is made by means of NAMELIST/OUTPUT statements and corresponding associated write statements. All of the NAMELIST/OUTPUT statements and associated write statements appear in the DTAOUT.

Although some temporary NAMELIST/TPOUT statements and associated write statements are located in various intermediate subprograms of the CSP CRM Computer Program, the FORTRAN names therein are, with rare and inconsequential exception, reprinted in one or the other of the write statements associated with NAMELIST/OUTPUT statements. For this reason, only FORTRAN names associated with permanent output are presented here.

Each NAMELIST/OUTPT and, within each list, each FORTRAN name appearing in DTAOUT are presented below in the exact order of appearance in the resulting print-out.

#### NAMELIST/OUTPT 1

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
JMAX	$j_{\max}$	maximum number of size components of the oxidizer ( $j_{\max} \leq 4$ ) (dimensionless, integer)
WA	$W_a$	$W_a = \sum W_a(j)$ fraction of solid propellant mass attributable to all size components of the oxidizer (dimensionless, real)
DNM	-	denominator in formula for SMLB in subroutine DATAIN $\Sigma [W_a(j)/a_j]$ (cm <sup>-1</sup> , real)
WB	$W_b$	$W_b = 1 - W_a$ fraction of solid propellant mass attributable to the binder (dimensionless, real)
VFA	v	volume of the oxidizer expressed as a fraction of solid propellant volume (dimensionless, real)
SMLATP	$a_{top}$	$a_{top} = \sqrt{\frac{2}{3}} A_{jm}$ Hermance equivalent mean size of the oxidizer size component assumed to exist in the topmost lamina of the solid propellant ( $j_m$ ) (cm, real)

FØRTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
DLTYTP	$\Delta\bar{y}_{top}$	$\Delta\bar{y}_{top} = a_{top} \bar{r}/\kappa_a$ thickness of any oxidizer lamina other than the topmost (dimensionless, real)
SMLB	b	$b=W_a \{[\pi/6v]\}^{1/3} - \sqrt{2/3} \} / \Sigma [W_a(j)/a_j]$ idealized thickness of a binder lamina calculated on the basis of oxidizer packing factor (cm, real)
DLTYBB	$\Delta\bar{y}_b$	$\Delta\bar{y}_b = b\bar{r}/\kappa_b$ thickness of any binder lamina (dimensionless, real)
KS	$\kappa_s$	bulk equivalent thermal conductivity of the CSP (cal sec <sup>-1</sup> cm <sup>-1</sup> °K <sup>-1</sup> , real)
RØS	$\rho_s$	bulk mean density of the CSP (g cm <sup>-3</sup> , real)
CS	$C_s$	bulk equivalent specific heat at constant pressure of the CSP (cal g <sup>-1</sup> °K <sup>-1</sup> , real)
KAPA	$\kappa_a$	$\kappa_a = \kappa_s / (\rho_s C_s)$ thermal diffusivity of the oxidizer (cm <sup>2</sup> sec <sup>-1</sup> , real)
KAPB	$\kappa_b$	$\kappa_b = \kappa_s / (\rho_s C_s)$ bulk equivalent thermal diffusivity of the CSP (cm <sup>2</sup> sec <sup>-1</sup> , real)
KAPS	$\kappa_s$	$\kappa_s = \kappa_s / (\rho_s C_s)$ bulk equivalent thermal diffusivity of the CSP (cm <sup>2</sup> sec <sup>-1</sup> , real)
Z	Z	$Z = \rho_s C_s / (\rho_a C_a)$ ratio of thermal capacity per unit volume of the bulk CSP to that of the oxidizer (dimensionless, real)
Z'	Z'	$Z' = \rho_s C_s / (\rho_b C_b)$ ratio of thermal capacity per unit volume of the bulk CSP to that of the binder (dimensionless, real)

## NAMELIST/OUTPT 2

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
THETAA	$\theta_a$	$\theta_a = E / (R \bar{T}_w)$ (dimensionless, real)
CHI	x	$x = \frac{\bar{T}_w - T_o}{\bar{T}_w}$ (dimensionless, real)
D	D	$D = \theta_a \cdot x$ (dimensionless, real)
QSDMLS	$H_a$	$H_a = W_a Q_a / [C_a (\bar{T}_w - T_o)]$ (dimensionless, real)
QMMLS	$H_m$	$H_m = W_m Q_m / [C_a (\bar{T}_w - T_o)]$ (dimensionless, real)
FDMLS	$\tau_f$	$\tau_f = \bar{r} / (\bar{T}_w - T_o)$ (dimensionless, real)
B	B	$B = \kappa_a A W_a Q_a / [C_a (\bar{T}_w - T_o) \bar{r}^2]$ (dimensionless, real)
KMLTR	K	$K = B \exp(-\theta_a) / D$ (dimensionless, real)

## NAMELIST/OUTPT 3

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
TWBAR	$\bar{T}_w$	mean temperature of the gas-liquid interface at the mean position of this interface, i.e., at $\bar{y}=0$ ( $^{\circ}$ K, real)
YSSTBR	$\bar{y}_s^* = \frac{\bar{x}^* \bar{r}}{\kappa_s}$	dimensionless flame mean stand-off distance (dimensionless, real)
XSTBAR	$\bar{x}^*$	flame mean stand-off distance (cm, real)
AMM	$a_m$	equivalent mean particle diameter (cm, real)
TAUMLT(M-1)	$\bar{\tau}_{m-1}$	dimensionless_mean temperature within the melt layer Note: $T_0=1.0$ , and $\bar{T}_{100}=T_{melt}$ , the dimensionless melting temperature of the oxidizer. (dimensionless, real)
XMLT(M-1)	$x_{m-1}$	distance from the mean position of the gas-liquid interface to the location at which $\bar{\tau}=\bar{\tau}_{m-1}$ (cm, real)
M	m	index of the increments in $\bar{T}$ and x that are calculated and tabulated through the melt layer $2 \leq M \leq 101$ (dimensionless, integer)
N	n	index of laminae from the gas-liquid interface ( $n=0$ ), through the liquid-solid interface ( $n=1$ ), through the first oxidizer-to-binder interface ( $n=2$ ) through the first binder-to-oxidizer interface ( $n=3$ ), and so on to as far into the CSP as $n=101$ , if necessary (dimensionless, integer)
RBR	$\bar{r}$	temporal mean rate of regression of the composite solid propellant ( $cm sec^{-1}$ , real)
ITERA	-	specifies the mode of operation of the computer program: If ITERA=0, the program determines the combustion response parameters for a CSP whose temporal mean regression rate is specified; if ITERA=1, the program determines the temporal mean regression rate for a propellant whose basic physical and chemical characteristics have been specified (dimensionless, integer)
N5	-	when ITERA=1, N5 is the number of the iteration in the iterative attempt to determine RBR ( $1 \leq N5 \leq N5MAX$ ) (dimensionless, integer)
N5MAX	-	if ITERA=1 and if a satisfactory value for RBR has not been achieved after N5MAX-1 one-percent increments or decrements of RBR, the solution will be terminated and an appropriate comment will be printed in the computer output (dimensionless, integer) Note: This mode of program termination indicates an injudicious initial choice for RBR.

## NAMELIST/OUTPT 3 (continued)

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
LFLAG	-	LFLAG is set to zero each time SUBROUTINE SLDFAZ is entered in a normal manner. If ITERA=0, LFLAG is then immediately reset to 1 and control of the program is returned to SUBROUTINE CNTRL, the main program, as soon as explicit values of certain required variables are determined in SUBROUTINES SLDFAZ, GASFAZ, and AMULTI. If ITERA=1, LFLAG is only reset to 1 and program control is only returned to the main program when a suitable value has been found for RBR or when N5=N5MAX (dimensionless, integer)
GWBRS	$\bar{g}_{w_s}$	$\bar{g}_{w_s} = \left( \frac{d\bar{\tau}}{dy_s} \right)_{y_s=0}$ (dimensionless, real)
DGWBRs	$\left( \frac{d\bar{q}}{dy_s} \right)_{y_s=0}$	$\left( \frac{d\bar{q}}{dy_s} \right)_{y_s=0} = \left( \frac{d^2\bar{\tau}}{dy_s^2} \right)_{y_s=0}$ (dimensionless, real)
QLDMLS	$H_l$	sometimes set equal to $H_s$ ; at other times, calculated as non-dimensionalized sum of $H_m$ and the actual heat absorbed as a result of oxidizer degradation as it is transported through the melt layer. Note: The two methods of determining $H_l$ ordinarily lead to virtually identical results. (dimensionless, real)

## NAMELIST/OUTPT 4

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
TAULR(N)	$\bar{\tau}_n$	dimensionless mean temperature at distance SLR(N) from the mean gas-liquid interface (dimensionless, real)
DTAULR(N)	$[\frac{d\bar{\tau}}{dy}]_n^a$	dimensionless mean temperature gradient at distance, XLR(N), from the mean gas-liquid interface and on the side of the N,N+1 interface nearest the mean gas-liquid interface. Note: For n even, $y=y_a$ ; for n odd, $y=y_b$ (dimensionless, real)
XLR (N)	$x_n$	distance from the mean position of the gas-liquid interface to the N,N+1 interface (cm, real)
DSCRIM(N)	$\bar{\tau}_n + (\frac{d\bar{\tau}}{dy})_n^-$	because, deep in the CSP, the exponentially decaying nature of the solution requires that DSCRIM(N) approach zero, DSCRIM(N) furnishes an indication as to whether the solution in this region has proceeded to a depth sufficient to provide a satisfactory steady-state solution (dimensionless, real)
N	n	index of laminae from the gas-liquid interface ( $n=0$ ), through the liquid-solid interface ( $n=1$ ), through the first oxidizer-to-binder interface ( $n=2$ ) through the first binder-to-oxidizer interface ( $n=3$ ), and so on to as far into the CSP as $n=101$ , if necessary (dimensionless, integer)
XTD	-	SQRT (KAPS/OMEGA)*YTD (cm, real)
CAPØA	$\Omega_a$	$\Omega_a = \frac{\omega_k a}{\bar{r}^2}$ (dimensionless, real)
CAPØB	$\Omega_b$	$\Omega_b = \frac{\omega_k b}{\bar{r}^2}$ (dimensionless, real)
CAPØS	$\Omega_s$	$\Omega_s = \frac{\omega_k s}{\bar{r}^2}$ (dimensionless, real)

## NAMELIST/OUTPT 5

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
N2	$n_2$	index of the laminae from the deep-solid side of the first oxidizer laminae for which XLR ( $N2=N2MXP1$ ) > XTD, through the adjacent overlying binder lamina for which XLR ( $N2=N2MXP1-1$ ) > XTD, through successive laminae of oxidizer and binder and, finally, of melt layer to $N2=0$ . Note: $XLR(N2=N) \equiv XLR(N)$ The index N2 is used in the step-by-step calculation of the perturbed solution, whereas N is used in the step-by-step calculation of the steady-state solution. (dimensionless, integer)
N2MXP1	$n_{2_{\max}} + 1$	maximum value of N2 determined as indicated in the definition of N2 (dimensionless, integer)
TAPIN	$\tau'_{n_{2_{\max}} + 1}$	normalized temperature perturbation applied in the solid phase at a distance from the gas-condensed phase interface that is several times the characteristic transient thermal depth within the solid. (dimensionless, complex)
DTAPIN	$g'_{n_{2_{\max}} + 1}$	$g'_{n_{2_{\max}} + 1} = (\frac{d\tau'}{dy_a})_{n_{2_{\max}} + 1}$ (dimensionless, complex)
XLR(N2)	$x_{n_2}$	distance from the mean position of the gas-liquid interface to the $N_2$ , $N_2+1$ interface (cm, real)
TAPLR(N2)	$\tau'_{n_2}$	dimensionless perturbed temperature at the $N_2$ , $N_2+1$ interface (dimensionless, complex)
DTAPLR(N2)	$g'_{n_2}$	first derivative of dimensionless perturbed temperature with respect to $y_a$ when $N_2$ is even, or with respect to $y_b$ when $N_2$ is odd, at the $N_2$ , $N_2+1$ interface (dimensionless, complex)
TAUOPS	$\tau'_{y=0}$	dimensionless perturbed temperature at the mean position of the gas-liquid interface, i.e., at $y=0$ (dimensionless, complex)
GOPPS	$g'_{y=0}$	first derivative of dimensionless perturbed temperature with respect to $y_a$ at $y=0+$ (dimensionless, complex)
DGOPPS	$g''_{y=0}$	second derivative of dimensionless perturbed temperature with respect to $y_a$ at $y=0+$ (dimensionless, complex)
RF	R	$R = (\frac{r'/\bar{r}}{p'/\bar{p}})$ , the response function (dimensionless, complex)

NAMELIST/OUTPT 5 (continued)

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
NRP	$\frac{p'}{\bar{p}}$	normalized perturbed pressure in the gas phase (quasi-static gas-phase behavior assumed) (dimensionless, complex)
YSWP	$y'_{S_w}$	dimensionless displacement of the instantaneous gas-liquid interface with respect to the mean gas-liquid interface, i.e., with respect to $y=0$ ; displacement non-dimensionalized on the basis of bulk CSP properties (dimensionless, complex)
XWP	$x'_{w}$	$x'_{w} = \frac{\kappa_S y'_{S_w}}{\bar{r}}$ (cm, complex)
NXSTP	$\frac{x^{*'}}{\bar{x}^*}$	perturbed displacement of the flame front with respect to the mean position of the flame front; normalized with respect to the mean position of the flame front (dimensionless, complex)
XSTP	$x^{*'}_{}$	$x^{*'} = \bar{x}^* \cdot \frac{x^{*'}}{\bar{x}^*}$ (cm, complex)
NYSTP	$\frac{y_S^{*'}}{\bar{y}_S^*}$	$\frac{y_S^{*'}}{\bar{y}_S^*} = \frac{x^{*'}}{\bar{x}^*}$ (dimensionless, complex)
YSSTP	$y_S^{*'}_{}$	$y_S^{*'} = \bar{y}_S^* \cdot \frac{x^{*'}}{\bar{x}^*}$ (dimensionless, complex)
RFNMLT	$R_{NML}$	response function under the assumption that no melt layer (NML) exists in the oxidizer lamina, that is contiguous with the gas phase (dimensionless, complex)
NRPNM	$(\frac{p'}{\bar{p}})_{NML}$	normalized perturbed pressure in the gas phase under the assumption that no melt layer exists (dimensionless, complex)
YSWPNM	$y'_{S_w NML}$	$y'_{S_w}$ under the assumption that no melt layer exists (dimensionless, complex)
XWPNM	$x'_{w NML}$	$x'_{w}$ in the absence of a melt layer (cm, complex)

## NAMELIST/OUTPT 5 (continued)

FORTRAN NAME	ALGEBRAIC SYMBOL	DEFINITION
NXSTPN	$(\frac{x^*}{\bar{x}^*})_{NML}$	$\frac{x^*}{\bar{x}^*}$ in the absence of a melt layer (dimensionless, complex)
XSTPNM	$x^*_{NML}$	$x^*$ in the absence of a melt layer (cm, complex)
YSSTPN	$y_s^*_{NML}$	$y_s^*$ in the absence of a melt layer (dimensionless, complex)

A-4. CARD IMAGE LISTING OF PROGRAM

C  
C  
CSTEAD PROC  
C  
C

THIS RUN HAS BEEN MADE WITH PROGRAM DECK NO. 9A

C  
C IMPLICIT REAL (K)  
COMMON/STEADY/ AMM,B,C,CA,CB,CG,CHI,CM,CS,D,DLTYAB,DLTYBB,DLTYTP,  
1DELTAT,DELTAU,DNM,DNOM,DTAULR,DSCRIM,E,ETA,FDMLS,JMAX,KA,KAPA,  
2KAPB,KAPS,KB,KFLMHT,KMLTLR,KS,PBAR,PRXFAC,QB,QBDMLS,QLM,QMDMLS,  
3QS,QSDMLS,R,RBR,ROA,ROB,ROS,SMLA,SMLATP,SMLB,TAULR,BUFFR1,TAUMLT,  
4TFLM,THETAA,TM,TOL,TWBAR,TZRO,VFA,W,A,WAC,WB,XLR,BUFFR2,XMLT,  
5XSTBAR,YSSTBR,BUFFR3,YABRML,Z,ZL,ZPR,RBROLD,DLTRBR,ITERA,N5,N5MAX,  
6FLAG,CAPOA,CAPOB,CAPOS,GWBRS,DGWBRS,QLDMLS,IHOMO

C  
C  
C  
C  
C  
C BUFFR1, BUFFR2, AND BUFFR3 ARE REQUIRED TO BUFFER THE STORAGE  
LOCATIONS JUST PRECEDING TAUMLT(1), XMLT(1), AND YABRML(1),  
RESPECTIVELY. THIS PROCEDURE IS MADE NECESSARY BY MAKING TAUT(2)  
EQUIVALENT TAUMLT(1), XMLTT(2), TO XMLT(1), AND YABRT(2), TO  
YABRML(1).

DIMENSION DSCRIM(110),DTAULR(110),SMLA(4),TAULR(110),TAUMLT(110),  
1TAUT(110),WAC(+),XLR(110),XMLT(110),XMLTT(110),YABRML(110),  
2YABRT(110)  
EQUIVALENCE (TAUT(2),TAUMLT(1)),(XMLTT(2),XMLT(1)),  
1(YABRT(2),YABRML(1))  
EQUIVALENCE (GWBRS,GOBRS),(DGWBRS,DGOBRS)

END

C  
C  
CUNSTD PROC  
C  
COMMON/UNSTDY/NPP,TAPIN,XTD,YTD,OMEGA,NEQ,KD,MXSTEP,KQ,EP,  
1DTAPIN,TAPLR,DTAPLR,N2MXP1,RF,NRP,YSWP,XWP,NXSTP,XSTP,NYSSTP,  
2YSSTP,D2TAPR,D2TAPI,TAUOPPS,GOPPS,DGOPPS,  
3RFNMLT,NRPNM,YSWPNM,XWPNM,NXSTPN,XSTPNM,YSSTPN  
C  
COMPLEX NPP,TAPIN,DTAPIN,TAPLR,DTAPLR,RF,NRP,YSWP,XWP,NXSTP,XSTP,  
1NYSSTP,YSSTP,TAUOPPS,GOPPS,DGOPPS,  
2RFNMLT,NRPNM,YSWPNM,XWPNM,NXSTPN,XSTPNM,YSSTPN  
C  
DIMENSION TAPLR(110),DTAPLR(110)  
END

C  
C  
C      CONTROL PROVIDES THE SEQUENCE OF CALLS TO  
C      SUBROUTINES THAT IS REQUIRED TO OBTAIN THE DESIRED SOLUTION  
C      OF THE COMBUSTION RESPONSE PROBLEM.  
C  
C  
INCLUDE CSTEAD, LIST  
INCLUDE CUNSTD, LIST  
C  
C  
10 CONTINUE  
CALL OVRFLOW(3)  
CALL DATAIN  
IF (ITERA .EQ. 0 .AND. OMEGA .EQ. 0.) GO TO 70  
CALL SLDFAZ  
CALL MELTLR  
CALL LAYERS  
IF (ITERA .NE. 0) GO TO 60  
CALL LAYRSP  
CALL MLTLRP  
CALL GLIFP  
60 CALL DTAOUT  
IF (ITERA .EQ. 0 .AND. OMEGA .NE. 0.) GO TO 10  
70 CONTINUE  
STOP  
END

```

C
C      SUBROUTINE DATAIN
C
C      SUBROUTINE DATAIN LOADS THE INPUT DATA AND DERIVES CERTAIN WIDELY
C      USED PARAMETERS FROM THESE DATA.
C
INCLUDE CSTEAD, LIST
INCLUDE CUNSTD, LIST
INTEGER KD,KQ
DIMENSION TNPP(2),TTAPIN(2)
EQUIVALENCE (TNPP,NPP),(TTAPIN,NRP)

C
C      CAUTION***NAMELIST/INPUT/ REQUIRES THE ENTRY OF NPP AND TAPIN IN
C      TERMS OF THE NUMBER PAIR, MODULUS (AS A DECIMAL FRACTION) AND
C      ARGUMENT (AS A PHASE ANGLE IN DEGREES). NPP AND TAPIN ARE THEN
C      REDEFINED BY THEIR CARTESIAN REAL AND IMAGINARY COMPONENTS IN
C      SUBROUTINE DATAIN.
C
C
NAMELIST/INPUT/CA,CB,CG,KA,KB,ROA,ROB,WAC,SMLA,E,R,PRXFAC,QS,QB,
1QLM,KFLMHT,TFLM,TM,TZRO,PBAR,RBR,TOL,ITERA,N5MAX,NPP,TAPIN,YTD,
2OMEGA,NEQ,KD,MXSTEP,EP,IHOMO
READ(5,INPUT)
IF(OMEGA .EQ. 0.) RETURN
DO 10 I=1,101
TAPLR(I)=0.0
DTAPLR(I)=0.0
10 CONTINUE
IF(IDATA .EQ. 1) GO TO 106
IDATA=1
WRITE(6,INPUT)
WA=0.
DNM=0.
JMAX=0
IF(WAC(1) .GT. 0.) JMAX=1
IF(WAC(2) .GT. 0.) JMAX=2
IF(WAC(3) .GT. 0.) JMAX=3
IF(WAC(4) .GT. 0.) JMAX=4
IF(JMAX .EQ. 0) WRITE(6,150)
150 FORMAT(//T6,-NO AP PARTICLES OF ANY FINITE DIAMETER HAVE BEEN INCL
IUED IN THE INPUT DATA-//)
IF(JMAX .EQ. 0) STOP
DO 105 J=1,JMAX
WA=WA+WAC(J)
DNM=DNM+WAC(J)/SMLA(J)
105 CONTINUE
106 IF(IHOMO .EQ. 0) GO TO 107
C
C      WHEN IHOMO=0, CERTAIN PERTINENT PHYSICAL AND THERMAL PROPERTIES OF
C      THE PROPELLANT BINDER, OXIDIZER, AND GASEOUS PRODUCTS SPECIFIED
C      IN NAMELIST/INPUT/ ARE GENERALLY DISTINCT$ HOWEVER, WHEN
C      IHOMO=1, THESE PROPERTIES OF THE OXIDIZER AND GASEOUS PRODUCTS
C      ARE SET EQUAL TO CORRESPONDING PROPERTIES OF THE OXIDIZER.
C      THUS, SPECIFYING IHOMO=1 IMPLIES A HOMOGENEOUS PROPELLANT.
C

```

CB=CA  
CG=CA

```

KB=KA
ROB=ROA
107 CONTINUE
WB=1.-WA
VFA=WA/ROA/(WA/ROA+WB/ROB)
SMLATP=SQRT(2./3.)*SMLA(JMAX)
SMLB=WA*VFA/DNM
KS=KA
ROS=ROA*ROB/(ROA*WB+ROB*WA)
CS=CA*WA+CB*WB
KAPA=KA/ROA/CA
KAPB=KB/ROB/CB
KAPS=KS/ROS/CS
DLTYTP=SMLATP*RBR/KAPA
DLTYAB=RBR*SMLA(1)/KAPA
DLTYBB=RBR*SMLB/KAPB
Z=ROS/ROA*CS/CA
ZPR=ROS/ROB*CS/CB
TNPP(1)=REAL(NPP)*COS(AIMAG(NPP/57.29578))
TNPP(2)=REAL(NPP)*SIN(AIMAG(NPP/57.29578))
TTAPIN(1)=REAL(TAPIN)*COS(AIMAG(TAPIN)/57.29578)
TTAPIN(2)=REAL(TAPIN)*SIN(AIMAG(TAPIN)/57.29578)
110 CONTINUE
CAPOA=OMEGA*KAPA/RBR**2
CAPOB=OMEGA*KAPB/RBR**2
CAPOS=OMEGA*KAPS/RBR**2
XTD=YTD*SQRT(KAPS/OMEGA)
RETURN
END

```

```
C  
C      FUNCTION TAU(TW,TZRO,T)  
C      FUNCTION TAU DETERMINES A DIMENSIONLESS TEMPERATURE THAT IS WIDELY  
C      USED THROUGHOUT THIS PROGAM.  
C  
      TAU=(T-TZRO)/(TW-TZRO)  
      RETURN  
      END
```

```

C
C
C      SUBROUTINE SLDFAZ
C
C      FOR A GIVEN VALUE OF MEAN BURNING RATE, RBR, SUBROUTINE SLDFAZ
C      CALCULATES MEAN WALL TEMPERATURE, TWBAR.
C
C      INCLUDE CSTEAD, LIST
C      INCLUDE CUNSTD, LIST
C
C      NAMELIST/TPOUT1/TWBAR,QSDMLS,QMDMLS,QBDMLS,THETAA,CHI,D,B,KMLTLR,
C      QLDMLS,FDMLS,GWBRS,DGWBRS
C
C
C      LFLAG=0
C      N5=1
C      DAM=0.
202 IF(LFLAG .EQ. 1) RETURN
      IF(ITERA .EQ. 0 .OR. N5 .EQ. N5MAX) LFLAG=1
      RBROLD=RBR
      TWBAR=TM
      TRLRBR=0.
      DO 205 I=1,100
      OLDTWB=TWBAR
      OLDRBR=TRLRBR
      DELTAT=.01*(TFLM-TM)
      TWBAR=OLDTWB+DELTAT
      QSDMLS=WA*QS/CA/(TWBAR-TZRO)
      QMDMLS=WA*QLM/CA/(TWBAR-TZRO)
      QLDMLS=QSDMLS
      THETAA=E/R/TWBAR
      CHI=(TWBAR-TZRO)/TWBAR
      TRLRBR=SQRT(2.*KAPA*PRXFAC*QSDMLS*EXP(-THETAA)*
      1(1.-EXP(-THETAA*CHI*(1.-TAU(TWBAR,TZRO,TM))))*
      2/(THETAA*CHI*((Z*(1.+(QLDMLS+QMDMLS)*CA/CS))**2
      3-(TAU(TWBAR,TZRO,TM)*(1.-Z)-Z*QMDMLS*CA/CS)-1.)**2)))
      IF(TRLRBR .GT. RBR) GO TO 210
205 CONTINUE
      WRITE(6,208)
208 FORMAT(//,T6,-NUMBER OF ITERATIONS FOR RBR HAS REACHED 100 IN SUBR
      IOUTINE SLDFAZ-//)
      STOP
210 TWBAR=OLDTWB+(TWBAR-OLDTWB)*(RBR-OLDRBR)/(TRLRBR-OLDRBR)
      QSDMLS=WA*QS/CA/(TWBAR-TZRO)
      QMDMLS=WA*QLM/CA/(TWBAR-TZRO)
      QLDMLS=QSDMLS
      QBDMLS=WB*QB/CB/(TWBAR-TZRO)
      THETAA=E/R/TWBAR
      CHI=(TWBAR-TZRO)/TWBAR
      D=THETAA*CHI
      B=KAPA*PRXFAC*QSDMLS/RBR/RBR
      KMLTLR=B*EXP(-THETAA)/D
      FDMLS=(QLDMLS+QMDMLS)*CA/CS+QBDMLS*CB/CS
      GWBRS=-Z*(1.+(QLDMLS+QMDMLS)*CA/CS)
      DGWBRS=-GWBRS+B*EXP(-THETAA)
      WRITE(6,TPOUT1)
      CALL GASFAZ($202)
      RETURN
      END

```

C  
C SUBROUTINE GASFAZ(\$)  
C  
C GIVEN RBR AND TWBAR, SUBROUTINE GASFAZ CALCULATES FLAME STAND-OFF  
C DISTANCES, YSSTBR AND XSTBAR.  
C  
INCLUDE CSTEAD, LIST  
INCLUDE CUNSTD, LIST  
300 YSSTBR=ALOG((TAU(TWBAR,TZRO,TFLM)+FDMLS)/(1.+FDMLS))  
XSTBAR=YSSTBR\*KAPS/RBR  
CALL AMULTI (\$310)  
310 RETURN1  
END

C  
C  
SUBROUTINE AMULTI(\$)  
C  
C SUBROUTINE AMULTI CALCULATES A VIRTUAL UNIMODAL AP PARTICLE  
C DIAMETER CORRESPONDING TO RBR AND YSSTBR.  
C  
INCLUDE CSTEAD, LIST  
500 AMM=KAPS\*PBAR\*YSSTBR/(KFLMHT\*RBR\*RBR )  
IF(LFLAG .EQ. 1) RETURN  
DAMOLD=DAM  
DAM=AMM-SMLA(JMAX)  
IF(ABS(DAM-DAMOLD) .GT. ABS(ABS(DAM)-ABS(DAMOLD))) GO TO 550  
DLTRBR=.01\*RBR  
IF(DAM)510,520,530  
510 RBR=RBR-DLTRBR  
GO TO 540  
520 GO TO 540  
530 RBR=RBR+DLTRBR  
GO TO 540  
540 NS=NS+1  
RETURN1  
550 RBR=RBROLD-(RBR-RBROLD)\*DAMOLD/( DAM-DAMOLD)  
LFLAG=1  
RETURN  
END

C  
C SUBROUTINE MELTLR

C  
C SUBROUTINE MELTLR DETERMINES TEMPORAL MEAN TEMPERATURE AND THE  
C DERIVATIVE OF THIS TEMPERATURE WITH RESPECT TO DIMENSIONLESS  
C DISTANCE AS FUNCTIONS OF DIMENSIONAL DISTANCE INTO THE LIQUID  
C PROPELLANT (MEASURED FROM THE TEMPORAL MEAN POSITION OF THE  
C MELTING SURFACE OF THE PROPELLANT).  
C

INCLUDE CSTEAD, LIST  
INCLUDE CUNSTD, LIST  
COMMON/M/ M  
COMMON/N/ N  
COMMON/MLTINT/ P,NDEG

C  
C  
DELTAU=.01\*(1.-TAU(TWBAR,TZRO,TM))  
TAUT(1)=1.  
YABRT(1)=0.  
DO 505 I=2,101  
TAUT(I)=TAUT(I-1)-DELTAU  
ETA=D\*(1.-TAUT(I))  
CM=0.5+KMLTLR-0.5\*(Z\*(1.+(QLDMLS+QMDMLS)\*CA/CS))\*\*2  
C=(1.-2.\*CM)/KMLTLR  
ZI=C\*EXP(ETA)  
DNOM=1.+C-SQRT(C\*\*2+2.\*C)  
YABRT(I)= ALOG((1.+ZI-SQRT(ZI\*\*2+2.\*ZI))/DNOM)/(D\*SQRT(1.-2.\*CM))  
XMLTT(I)=KAPA\*YABRT(I)/RBR  
M=I  
505 CONTINUE  
DIMENSION P(10),W(200)  
CALL PFIT(M,YABRT,TAUT,-1.,6.,TRUE,,TRUE,,P,NDEG,  
SIGFAC,W)  
NP3=NDEG+3  
WRITE(6,510) NDEG,SIGFAC,(P(I),I=1,NP3)  
510 FORMAT(//T5,-NDEG=-,I2,T17,-SIGFAC=-,F6.4/T5,-P(1),...,P(NDEG+3)=-  
1,T24,3F15.8/(T24,3F15.8))  
DO 530 I=1,M  
TAUFIT=SCPVAL(P,NDEG,YABRT(I))  
TAUERR=TAUT(I)-TAUFIT  
530 CONTINUE  
TAURL(1)=TAUMLT(100)  
DTAURL(1)=-Z\*(TAUMLT(100)+QMDMLS\*CA/CS)  
XLR(1)=YABRML(100)\*KAPA/RBR  
DSCRIM(1)=TAURL(1)+DTAURL(1)  
N=2  
RETURN  
END

```

C
C          SUBROUTINE LAYERS
C
C          SUBROUTINE LAYERS DETERMINES TEMPORAL MEAN TEMPERATURE AND THE
C          DERIVATIVE OF THIS TEMPERATURE WITH RESPECT TO DIMENSIONLESS
C          DISTANCE AS FUNCTIONS OF DIMENSIONAL DISTANCE INTO THE SOLID
C          PROPELLANT (MEASURED FROM THE TEMPORAL MEAN POSITION OF THE
C          MELTING SURFACE OF THE PROPELLANT).
C
C          INCLUDE CSTEAD, LIST
C          INCLUDE CUNSTD, LIST
C          COMMON/N/ N
C
601 IF(N .EQ. 2) GO TO 610
602 IF(MOD(N,2) .EQ. 0) GO TO 615
605 DELTAY=DLTYBB
      DELTAX=SMLB
      C1=(1.-ZPR)*TAULR(N-1)
      GO TO 630
610 DELTAY=DLTYTP
      DELTAX=SMLATP
      C1=(1.-Z)*TAULR(1)
      GO TO 630
615 DELTAY=DLTYAB
      DELTAX=SMLA(1)
      C1=(1.-Z)*TAULR(N-1)
630 TAULR(N)=C1-(C1-TAULR(N-1))*EXP(-(DELTAY))
      DTAULR(N)=C1-TAULR(N)
      XLR(N)=XLR(N-1)+DELTAX
      DSCRIM(N)=TAULR(N)+DTAULR(N)
      IF(MOD(N,2) .EQ. 0) GO TO 6540
      ITOL=0
      IN=0
      IXTD=0
6400 IF(ABS(ABS(DSCRIM(N))-ABS(DSCRIM(N-1))) .EQ. ABS(DSCRIM(N)-
      1DSCRIM(N-1)) .AND. ABS(DSCRIM(N)) .LT. TOL .AND. ABS(TAULR(N))-
      2.LT. TOL) GO TO 6410
      GO TO 6420
6410 ITOL=1
      WRITE(6,6415)
6415 FORMAT(//6X,-TOLERANCE TESTS FOR A SATISFACTORY STEADY-STATE SOLUT
      ION HAVE BEEN MET.-//)
6420 IF(N .LE. 100) GO TO 6430
      WRITE(6,6425)
6425 FORMAT(//6X,-MORE THAN FIFTY PAIR OF OXIDIZER AND BINDER LAYERS HA
      IVE BEEN TRaversed.-//)
      GO TO 6440
6430 IN=1
6440 IF(XLR(N-1) .GT. XTD) GO TO 6450
      WRITE(6,6445)
6445 FORMAT(//6X,-NUMBER OF LAYERS TRAVERSED IS INSUFFICIENT TO INSURE
      1SATISFACTORY ACCURACY OF THE PERTURBED SOLUTION.-//)
      GO TO 6460
6450 IXTD=1
6460 CONTINUE
6500 IF(ITOL .EQ. 1) GO TO 6510
      IF(IN .EQ. 1) GO TO 6530
      IF(IXTD .EQ. 1) GO TO 6550
6510 IF(IN .EQ. 1) GO TO 6520

```

GO TO 6550  
6520 IF(IXTD .EQ. 1) GO TO 6560  
6530 GO TO 6540  
6540 N=N+1  
GO TO 602  
6550 IF(ABS(ABS(DSCRIM(N))-ABS(DSCRIM(N-2))) .EQ. ABS(DSCRIM(N))-  
1DSCRIM(N-2))) WRITE(6,660)  
660 FORMAT(/6X,-DISCRIMINANTS N AND N-2 HAVE THE SAME ALGEBRAIC SIGN.-)  
IF(ABS(DSCRIM(N)) .LT. TOL) WRITE(6,665)  
665 FORMAT(/6X,-ABS(DSCRIM(N)) MEETS REQUIREMENTS FOR A SATISFACTORY S  
1LUTION.-)  
IF(ABS(TAULR(N)) .LT. TOL) WRITE(6,670)  
670 FORMAT(/6X,-ABS(TAULR(N)) MEETS REQUIREMENTS FOR A SATISFACTORY SO  
1LUTION.-)  
WRITE(6,6555)  
6555 FORMAT(/6X,-THE ACCURACY OF THIS STEADY-STATE SOLUTION MAY BE SAT  
1ISFACTORY\$/-6X,-HOWEVER, IT HAS NOT MET ALL CONVERGENCE CRITERIA.-  
2/6X,-REFER TO THE PRECEDING DIAGNOSTIC REMARKS TO DETERMINE WHICH  
3CRITERIA-/6X,-HAVE BEEN MET AND WHICH HAVE NOT.-//)  
RETURN  
6560 WRITE(6,6565)  
6565 FORMAT(/6X,-A SATISFACTORY STEADY-STATE SOLUTION HAS BEEN OBTAINED  
1D.-//)  
RETURN  
END

C  
C SUBROUTINE LAYRSP

C IN SUBROUTINE LAYRSP, AN INITIAL DEPTH WITHIN THE SOLID, ADEQUATE  
C TO EXCEED SOME CHOSEN MULTIPLE OF THERMAL DEPTH AND TERMINATING  
C ON THAT SURFACE OF A BINDER LAYER WHICH IS FARTHEST FROM THE  
C BURNING SURFACE, IS DETERMINED. INTIAL VALUES OF DIMENSIONLESS  
C TEMPERATE AND ITS DERIVATIVE WITH RESPECT TO DIMENSIONLESS  
C DISTANCE ARE THEN SPECIFIED ON THE FAR SIDE OF THE NEXT UNDERLY-  
C ING OXIDIZER LAYER. DIMENSIONLESS TEMPERATURE IS ARBITRARILY  
C ASSUMED. ITS DERivate IS APPROXIMATED FROM A REQUIREMENT THAT IS  
C STRICTLY VALID ONLY FOR A HOMOGENEOUS SEMI-INFINITE SLAB.

C  
C INCLUDE CSTEAD, LIST  
INCLUDE CUNSTD, LIST

C COMMON/N2/N2

C COMPLEX LAM1, LAM2, C1, C2, TAP, GPM

C N2=3

1601 IF(XLR(N2) .GT. XTD) GO TO 1605  
N2=N2+2  
GO TO 1601  
1605 N2MXP1=N2+1  
CAPO=CAPOA  
A1=SQRT((SQRT(1.+16.\*CAPO\*\*2)+1.)/2)  
B1=SQRT((SQRT(1.+16.\*CAPO\*\*2)-1.)/2)  
LAM1=CMPLX(-0.5\*(1.+A1),-0.5\*B1)  
DTAPIN=LAM1\*TAPIN  
N2=N2MXP1  
DELTAY=-DLTYAB  
TAPLR(N2)=TAPIN  
TAP=TAPIN  
DTAPLR(N2)=DTAPIN  
GPM=DTAPIN  
GO TO 1655  
1607 IF(N2 .EQ. 2) GO TO 1630  
1609 IF(MOD(N2,2) .EQ. 0) GO TO 1620  
1610 DELTAY=-DLTYBB  
CAPO=CAPOB  
TAP=TAPLR(N2)  
GPM=ZPR/Z\*DTAPLR(N2)  
GO TO 1655  
1620 DELTAY=-DLTYAB  
CAPO=CAPOA  
TAP=TAPLR(N2)  
GPM=Z/ZPR\*DTAPLR(N2)  
GO TO 1655  
1630 DELTAY=-DLTYTP  
CAPO=CAPOA  
TAP=TAPLR(2)  
GPM=Z/ZPR\*DTAPLR(2)  
1655 A1=SQRT((SQRT(1.+16.\*CAPO\*\*2)+1.)/2)  
B1=SQRT((SQRT(1.+16.\*CAPO\*\*2)-1.)/2)

```
LAM1=CMPLX(-0.5*(1.+A1),-0.5*B1)
LAM2=CMPLX(-0.5*(1.-A1),+0.5*B1)
C1=(LAM2*TAP-GPM)/(LAM2-LAM1)
C2=-(LAM1*TAP-GPM)/(LAM2-LAM1)
TAPLR(N2-1)=C1*EXP(LAM1*DELTAY)+C2*EXP(LAM2*DELTAY)
DTAPLR(N2-1)=C1*LAM1*EXP(LAM1*DELTAY)+C2*LAM2*EXP(LAM2*DELTAY)
1665 N2=N2-1
IF(N2 .EQ. 1) RETURN
GO TO 1607
END
```

C  
C SUBROUTINE MLTLRP

C  
C GIVEN TAUCLR(1) AND DTAULR(1), SUBROUTINE MLTLRP INTEGRATES  
C STEP-BY-STEP FROM THE LIQUID-SOLID INTERFACE IN THE TOPMOST  
C OXIDIZER LAYER TO THE GAS-LIQUID INTERFACE THAT IS THE BURNING  
C SURFACE. TAUOPS AND GOPPS ARE THUS DETERMINED FOR THE LIQUID  
C SIDE OF THE BURNING SURFACE.

C  
INCLUDE CSSTEAD, LIST  
INCLUDE CUNSTD, LIST

C  
COMMON/M/ M  
COMMON/MLTINT/ P,NDEG  
COMMON/N2/N2

C  
DIMENSION P(10)

C  
1500 INTEGER NEQ,KD,IFLAG,MXSTEP,KSTEP,KEMAX,KQ  
REAL EP,HMINA,HMAXA,EMAX  
REAL D2TAP,DT(10,1)  
REAL YABRV,DEPVAR(2)  
H=-.01\*YABRT(M)  
HMINA=.1\*H  
HMAXA=10.\*H  
YABRVF=0.  
DELT=10.\*H

1501 L=1  
YABRV=YABRT(M)  
DEPVAR(1)=REAL(TAPLR(1))  
DEPVAR(2)=REAL(DTAPLR(1))  
WRITE(6,1504)  
1504 FORMAT(//T11,-YABRV-,T26,-TAPR-,T41,-DTAPR-,T55,-D2TAPR-//)  
GO TO 1507

1502 L=2  
YABRV=YABRT(M)  
DEPVAR(1)=AIMAG(TAPLR(1))  
DEPVAR(2)=AIMAG(DTAPLR(1))  
WRITE(6,1506)  
1506 FORMAT(//T11,-YABRV-,T26,-TAPI-,T41,-DTAPI-,T55,-D2TAPI-//)

1507 CALL SVDQ(NEQ,YABRV,DEPVAR,D2TAP,KD,EP,IFLAG,H,HMINA,HMAXA,DELT,  
1YABRVF,MXSTEP,KSTEP,KEMAX,EMAX,KQ,YN,DT)  
GO TO 20

10 CALL SVDQ1  
20 GO TO 130,30,40,40,50,60,70,701, IFLAG  
30 TAUFIT=SCPVAL(P,NDEG,YABRV)  
T3=KMLTLR\*D\*D\*EXP(-D\*(1.-TAUFIT))\*DEPVAR(1)  
D2TAP=-DEPVAR(2)+T3  
GO TO 10

40 WRITE(6,1540) IFLAG, H  
1540 FORMAT(//T6,-IFLAG=-,I2,T21,-H=-,E15.6)  
45 WRITE(6,1545) YABRV,DEPVAR(1),DEPVAR(2),D2TAP  
1545 FORMAT(//T6,4E15.6)  
IF(IFLAG .EQ. 3) GO TO 10  
IF(L .EQ. 1) GO TO 1552  
IF(L .EQ. 2) GO TO 1554  
50 WRITE(6,1540) IFLAG, H

```
GO TO 10
60 EP=32.*EMAX*EP
WRITE(6,1560) YABRV,EP
1560 FORMAT(1T6,-OLD EP WAS TOO SMALL. NEW EP HAS BEEN ESTABLISHED AT Y
          1ABRV-/T8,-YABRV=-,E15.6,T36,-EP=-,E15.6)
          GO TO 10
70 WRITE(6,1540) IFLAG, H
          GO TO 10
1552 TAPR=DEPVAR(1)
        DTAPR=DEPVAR(2)
        D2TAPR=D2TAP
        GO TO 1502
1554 TAPI=DEPVAR(1)
        DTAPI=DEPVAR(2)
        D2TAPI=D2TAP
        TAUUPS=CMPLX(TAPR,TAPI)
        G0PPS=CMPLX(DTAPR,DTAPI)
        DG0PPS=CMPLX(D2TAPR,D2TAPI)
        N2=0
        RETURN
        END
```

```

C
C      SUBROUTINE GLIPP
C
C      SUBROUTINE GLIPP DETERMINES THE RESPONSE FUNCTION AND OTHER
C      DEPENDENT VARIABLES ASSOCIATED WITH THE PERTURBED SOLUTION.
C      THE EFFECT OF THE CONDENSED-PHASE ON THESE RESULTS IS DETERMINED
C      SOLELY BY THE RATIO, GOPPS/TAUOPS, WHICH APPEARS IN THE FORMULA
C      FOR RESPONSE FUNCTION,RF.
C
C
C      INCLUDE CSTEAD,LIST
C      INCLUDE CUNSTD,LIST
C
C
C      COMPLEX K2
C
C      NAMELIST/TPOUT3/K2,V3,V5,V6A,V6B,V7,RF0,K2NM,V5NM
C
C      K2=GUPPS/TAUOPS
C      V3=Z*(1.+ (QMDMLS+QLDMLS)*CA/CS)
C      V5=(1.+THETAA/2.)*CHI
C      1+(D/2.)*(1.-TAU(TWBAR,TZRO,TM))*CHI)
C      2/(EXP(D*(1.-TAU(TWBAR,TZRO,TM)))-1.)
C      3-1./(V3-(TAU(TWBAR,TZRO,TM)*(1.-Z)-Z*QMDMLS*CA/CS-1.))
C      V6A=EXP(YSSTBR)-1.
C      V6B=(1.+FDMLS)*YSSTBR*EXP(YSSTBR)
C      V7=Z*QBDMLS*CB/CS
C      RFU=V6B/(2.*V6B+V6A/V5+1./V5)
C      RF=CAPOA*V6B/(CAPOA*(2.*V6B+V6A/V5-V3/Z)+(0.,1.)*KMLTLR*D/Z
C      1-(CAPOA/V5-(0.,1.)*V3)*K2/Z)
C      NRP=RF*NPP
C      YSWP=(0.,-1.)*NRP/CAPOS
C      XWP=KAPS*YSWP/RBR
C      NXSTP=(1.-CMPLX(0.,-1.)/(CAPOS*YSSTBR)))*NRP-NPP
C      XSTP=NXSTP*XSTBAR
C      NYSTP=NXSTP
C      YSSTP=NYSTP*YSSTBR
C      IF(IHOMO.EQ.0) GO TO 1650
C      K2NM=DTAPIN/TAPIN
C      CAPCNM=1.
C      V3NM=1.
C      V5NM=THETAA*CHI
C      RFNMLT=CAPOA*V6B/(CAPOA*(2.*V6B+V6A/V5NM-V3NM/Z)+(0.,1.)*CAPCNM/Z
C      1-(CAPOA/V5NM-(0.,1.)*V3NM)*K2NM/Z)
C      NRPNM=RFNMLT*NPP
C      YSWPNM=(0.,1.)*NRPNM/CAPOS
C      XWPNM=KAPS*YSWPNM/RBR
C      NXSTPN=(1.-CMPLX(0.,-1.)/(CAPOS*YSSTBR)))*NRPNM-NPP
C      XSTPN=NXSTPN*XSTBAR
C      YSSTPN=NXSTPN*YSSTBR
1650 CONTINUE
      WRITE(6,TPOUT3)
      RETURN
      END

```

```
C
C      SUBROUTINE DTAOUT
C
C      SUBROUTINE DTAOUT PROVIDES A PRINTED RECORD OF THE RESULTS THAT
C      HAVE ACCUMULATED DURING THE COURSE OF THE RUN.
C
C      INCLUDE CSTEAD, LIST
C      INCLUDE CUNSTD, LIST
C
C      INTEGER KD,KQ
C
C      COMMON/M/ M
C      COMMON/N/ N
C      COMMON/N2/N2
C
C      NAMELIST/INPUT/CA,CB,CG,KA,KB,ROA,ROB,WAC,SMLA,E,R,PRXFAC,QS,QB,
1QLM,KFLMHT,TFLM,TM,TZRO,PBAR,RBR,TOL,ITERA,N5MAX,NPP,TAPIN,YTD,
2OMEGA,NEQ,KD,MXSTEP,EP,IHOMO
NAMELIST/OUTPT1/ JMAX,WA,DNM,WB,VFA,SMLATP,DLTYTP,DLTYAB,SMLB,
1DLTYBB,KS,ROS,CS,KAPA,KAPB,KAPS,Z,ZPR
NAMELIST/OUTPT2/ THETAA,CHI,D,QSDMLS,QBDMLS,QMDMLS,FDMLS,B,KMLTLR
NAMELIST/OUTPT3/TWBAR,YSSTBR,XSTBAR,AMM,TAUMLT,XMLT,M,N,RBR,ITERA,
JNS,N5MAX,LFLAG,GWBRS,DGWBRS,QLDMLS
NAMELIST/OUTPT4/ TAULR,DTAULR,XLR,DSCRIM,N,XTD,CAPOA,CAPOB,CAPOS
NAMELIST/OUTPT5/N2,N2MXP1,TAPIN,DTAPIN,XLR,TAPLR,DTAPLR,TAUOPS,
1GOPPS,DGUPPS,RF,NRP,YSWP,XWP,NXSTP,XSTP,NYSSTP,YSSTP,
2RFNMLT,IRPNM,YSWPNM,XWPNM,NXSTPN,XSTPNM,YSSTPN
      WRITE(6,INPUT)
      WRITE(6,OUTPT1)
      WRITE(6,OUTPT2)
      WRITE(6,OUTPT3)
      WRITE(6,OUTPT4)
      IF(ITERA .NE. 0) RETURN
      WRITE(6,OUTPT5)
      RETURN
      END
```

SUBROUTINE PFIT (M,X,Y,SIG,NMAX,SEEKN,COMTRN,CHBBAS,P,NFIT,SIGFAC,PFT00100  
 IW) PFT00200  
 C C.L.LAWSON, JPL, 1969 DEC 10 PFT00300  
 C C.L.LAWSON, JPL, 1970 JAN 12 CALLING SEQUENCE CHANGED PFT00400  
 C LEAST SQUARES POLYNOMIAL FIT TO DISCRETE DATA. PFT00500  
 C M NO. OF DATA POINTS PFT00600  
 C PFT00700  
 C (X(I),I=1,M) ABSISSAS OF DATA PFT00800  
 C PFT00900  
 C (Y(I),I=1,M) ORDINATES OF DATA PFT01000  
 C PFT01100  
 C (SIG(I),I=1,M) STANDARD DEVIATIONS OF DATA Y() PFT01200  
 C IF SIG(I) .LT. 0., THE SUBR WILL FUNCTION AS PFT01300  
 C THOUGH ALL SIG(I) ARE EQUAL TO ABS(SIG(1)) PFT01400  
 C PFT01500  
 C NMAX NMAX SPECIFIES HIGHEST DEGREE POLYNOMIAL TO PFT01600  
 C BE CONSIDERED. PFT01700  
 C PFT01800  
 C SEEKN IF .TRUE. THE SUBR WILL DETERMINE OPTIMUM PFT01900  
 C NFIT NOT EXCEEDING NMAX. PFT02000  
 C IF .FALSE. THE SUBR WILL SET NFIT = NMAX PFT02100  
 C UNLESS THIS PRODUCES A NEAR-SINGULAR PROBLEM, IN PFT02200  
 C WHICH CASE NFIT WILL BE REDUCED. PFT02300  
 C PFT02400  
 C COMTRN = .TRUE. SUBR WILL COMPUTE TRANSFORMATION PARAMETERS, PFT02500  
 C P(1) AND P(2) SO THAT THE TRANSFORMED VARIABLE PFT02600  
 C RANGES FROM -1. TO +1. PFT02700  
 C = .FALSE. SUBR WILL USE P(1) AND P(2) AS SET BY USER. PFT02800  
 C PFT02900  
 C CHBBAS = .TRUE. MEANS USE CHEBYSHEV BASIS PFT03000  
 C = .FALSE. MEANS USE MONOMIAL BASIS PFT03100  
 C PFT03200  
 C (P(J),J=1,NMAX+3) P(1) AND P(2) DEFINE A TRANSFORMATION OF THE PFT03300  
 C INDEPENDENT VARIABLE AS FOLLOWS.. PFT03400  
 C PFT03500  
 C S = ( X - P(1) ) / P(2) PFT03600  
 C PFT03700  
 C (P(I+3),I=0,...,NMAX) ARE POLY COEFFS COMPUTED PFT03800  
 C BY THE SUBR. P(I+3) IS THE COEFF OF S\*\*I PFT03900  
 C IF MONOMIAL BASIS IS USED AND OF THE I-TH PFT04000  
 C DEGREE CHEBY POLY IF THE CHEBY BASIS IS USED. PFT04100  
 C PFT04200  
 C IF NFIT .LT. NMAX THE COEFFS P(I+3) FOR PFT04300  
 C I .GT. NFIT WILL BE SET TO ZERO. PFT04400  
 C PFT04500  
 C PFT04600  
 C NFIT DEGREE OF POLY AS DETERMINED BY SUBROUTINE. PFT04700  
 C PFT04800  
 C SIGFAC FACTOR BY WHICH THE GIVEN SIG() VALUES SHOULD PFT04900  
 C BE MULTIPLIED TO IMPROVE CONSISTENCY WITH THE PFT05000  
 C FIT. SIGFAC IS THE SQUARE ROOT OF THE PFT05100  
 C RATIO OF (THE SUM OF SQUARES OF RESIDUALS) PFT05200  
 C TO(M-NFIT-1). PFT05300  
 C PFT05400  
 C W() WORKING SPACE. MUST BE DIMENSIONED AT LEAST PFT05500  
 C ( MAX(2\*NMAX,201)\*(NMAX+2) PFT05600  
 C PFT05700  
 C LOGICAL SEEKN, COMTRN, CHBBAS PFT05800  
 C REAL X(M),Y(M),SIG(M),P(1),W(1) PFT05900

```

C           EPS = 2**(-27)          PFT06000
DATA        EPS/.745E-8/          PFT06100
DATA        TOL/1.E-7/          PFT06200
DATA        ONE,TWO,HALF/1.E0,2.E0,.5E0/, ZERO/0.E0/    PFT06300
C           DEFINE A(,) TO BE A FUNCTION          PFT06400
C           A(I,J)=W(I+(J-1)*IDIM)          PFT06500
C           A(I,J)=W(-IDIM+I+J*IDIM)          PFT06600
C
C           N=NMAX          PFT06700
C           NP1=N+1          PFT06800
C           NP2=NP1+1          PFT06900
C           IF (N.LT.0.OR.M.LE.0) GO TO 320          PFT07000
C           IDIM=MAX0(2*NMAX,20)          PFT07100
C           SIGMA=ABS(SIG(1))          PFT07200
C           ZERO FIRST N+2 LOCATIONS OF COLUMN N+2          PFT07300
C           THIS IS DONE TO CLEAN UP OUTPUT IN CASES IN          PFT07400
C           WHICH M IS LESS THAN N+2. IT IS NOT          PFT07500
C           NECESSARY FOR THE COMPUTATION.          PFT07600
C           DO 10 I=1,NP2          PFT07700
10  A(I,NP2)=ZERO          PFT07800
C           COMPUTE P(1),P(2) IF REQUESTED          PFT07900
C
C           CHANGE OF INDEPENDENT VARIABLE IS GIVEN BY S=(X-P(1))/P(2)          PFT08000
C           OR X=P(1) + P(2)*S          PFT08100
C
C           IF (COMTRN) GO TO 20          PFT08200
C           IF (P(2)) 60,320,60          PFT08300
20  CONTINUE          PFT08400
XMIN=X(1)          PFT08500
XMAX=XMIN          PFT08600
IF (M.EQ.1) GO TO 40          PFT08700
DO 30 I=2,M          PFT08800
XMIN=AMIN1(XMIN,X(I))          PFT08900
30  XMAX=AMAX1(XMAX,X(I))          PFT09000
40  CONTINUE          PFT09100
P(1)=(XMAX+XMIN)*HALF          PFT09200
P(2)=(XMAX-XMIN)*HALF          PFT09300
IF (P(2)) 60,50,60          PFT09400
50  P(2)=ONE          PFT09500
C
C           60  CONTINUE          PFT09600
C           INITIALIZE FOR ACCUMULATION          PFT09700
C           CALL BHSLR1 (W,IDIM,NP1,A(1,NP2),IDIM,1,IR)          PFT09800
I=1          PFT09900
C
C           ACCUMULATION LOOP BEGINS HERE          PFT10000
C
70  MEQ=MIN0(IDIM-IR,M-I)+1          PFT10100
IF (MEQ.LE.0) GO TO 150          PFT10200
KMAX=IR+MEQ-1          PFT10300
DO 140 K=IR,KMAX          PFT10400
S=(X(I)-P(1))/P(2)          PFT10500
IF (SIG(1)) 90,320,80          PFT10600
80  SIGMA=SIG(I)          PFT10700
IF (SIGMA) 320,320,90          PFT10800
90  CONTINUE          PFT10900
A(K,1)=ONE/SIGMA          PFT11000
A(K,NP2)=Y(I)/SIGMA          PFT11100

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```

      IF (N.LE.0) GO TO 130          PFT11900
      IF (CHBBAS) GO TO 110          PFT12000
C
      DO 100 J=2,NP1                MONOMIAL BASIS
      100 A(K,J)=S*A(K,J-1)
      GO TO 130
C
      110 CONTINUE                   CHEBYSHEV BASIS
      A(K,2)=S/SIGMA
      IF (N.EQ.1) GO TO 130
      FAC=TWO*S
      DO 120 J=3,NP1
      120 A(K,J)=FAC*A(K,J-1)-A(K,J-2)
C
C
C
      130 CONTINUE
      I=I+1
      140 CONTINUE
      CALL BHSLR2 (MEQ,IR)
      GO TO 70
      150 CONTINUE
C
C
C
      160 CONTINUE                   END OF ACCUMULATION LOOP
C
C
C
      TEMPORARILY COPY RT-SIDE VECTOR INTO P()
C
      DO 160 I=1,NP1
      160 P(I+2)=A(I,NP2)
C
C
C
      USUALLY IR WILL EQUAL NMAX+3. IF M .LE. NMAX+1, OR POSSIBLY FOR
      OTHER REASONS, IR WILL BE LESS THAN NMAX+3. IN THIS CASE SET ROW
      IR TO ZERO AND REPLACE IR BY IR+1. THIS SIMPLIFIES LATER
      LOGIC BY ASSURING THAT NFIT WILL BE .LE. IR-3.
C
      IF (IR.GE.NMAX+3) GO TO 180
      DO 170 J=1,NP2
      170 A(IR,J)=ZERO
      IR=IR+1
      180 CONTINUE
C
C
      COMPUTE NORMS OF SUCCESSIVE RESIDUAL VECTORS
C
      K=IR-2
      A(K+1,NP2)=ABS(A(K+1,NP2))
      190 IF (K.LE.0) GO TO 200
      CALL SL2NRM (2,A(K,NP2),A(K,NP2))
      K=K-1
      GO TO 190
      200 CONTINUE
C
C
      DIVIDE NORM IN ROW I           BY SQRT(M - (I-1) )
      AND LOCATE SMALLEST RESULT
      IRM1=IR-1
      IMIN=1
      TEMP=M
      AMIN=A(1,NP2)
      BIAS=AMIN*EPS
      DO 210 I=1,IRM1
      210 A(I,NP2)=A(I,NP2)/SQRT(TEMP)

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```

TEMP=AMAX1(TEMP-ONE,ONE) PFT17800
IF (A(I,NP2).GE.AMIN) GO TO 210 PFT17900
AMIN=A(I,NP2)-BIAS PFT18000
IMIN=I PFT18100
210 CONTINUE PFT18200
C PFT18300
C OPTION TO USE BEST N OR MAXIMUM N PFT18400
C PFT18500
C IF (SEEKN) GO TO 220 PFT18600
NFT=MINU(NMAX,IR-3) PFT18700
GO TO 230 PFT18800
220 NFT=IMIN-2 PFT18900
230 CONTINUE PFT19000
NFT=MAXU(NFT,0) PFT19100
C PFT19200
C TEST THE FIRST NFT+1 DIAG ELTS FOR NEAR-SINGULARITY PFT19300
C PFT19400
C PFT19500
C PFT19600
C PFT19700
C N2=NFT+1 PFT19800
IF (N2.LT.2) GO TO 260 PFT19900
DO 240 I=2,N2 PFT20000
CALL SL2NRM (I-1,A(I,I),T) PFT20100
IF (ABS(A(I,I)).LE.TOL*T) GO TO 250 PFT20200
240 CONTINUE PFT20300
GO TO 260 PFT20400
250 NFT=I-2 PFT20500
260 CONTINUE PFT20600
NFIT=NFT PFT20700
C PFT20800
C SOLVE FOR COEFFS FOR DEGREE NFT PFT20900
C PFT21000
C SIGFAC=A(NFT+2,NP2) PFT21100
NFP1=NFT+1 PFT21200
DO 290 I=NFP1,1,-1 PFT21300
IP1=I+1 PFT21400
T=P(I+2) PFT21500
IF (I.EQ.NFP1) GO TO 280 PFT21600
DO 270 J=IP1,NFP1 PFT21700
270 T=T-A(I,J)*P(J+2) PFT21800
280 P(I+2)=T/A(I,I) PFT21900
290 CONTINUE PFT22000
IF (NFT.EQ.NMAX) GO TO 310 PFT22100
N1=NFT+2 PFT22200
N2=NMAX+1 PFT22300
DO 300 I=N1,N2 PFT22400
300 P(I+2)=ZERO PFT22500
310 CONTINUE PFT22600
RETURN PFT22700
C PFT22800
***** ERROR TERMINATION *****
320 CONTINUE PFT22900
WRITE (6,330) M,SIG(1),N,COMTRN,P(2),SIGMA PFT23000
NFIT=-1 PFT23100
RETURN PFT23200
330 FORMAT (48H0BAD VALUES INPUT TO PFIT. NO FIT WILL BE DONE.,12X,1H PFT23300
1M,7X,6HSIG(1),9X,4HNMAX,7X,6HCOMTRN,9X,4HP(2),8X,5HSIGMA/48X,T13,E PFT23400
213.5,T13,L13,2E13.5/) PFT23500
END PFT23600

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CIBFTC BHSLR• LIST BASIC SEQ. LEAST SQUARES WITH H.H. TRANS. 30 APR 68BHSL 10
C BHSLR• S.P. BASIC SEQ. LEAST SQUARES WITH H.H. TRANS. 30 APR 68BHSL 20
C R. HANSON, J.P.L.
C ENTRY POINTS BHSLR1,BHSLR2..
C *****
C SUBROUTINE BHSLR1 (A,NDA,N,B,NDB,NB,RI)
C *****
C INTEGER SMI,RI,NDA,N,NDB,NB
C
C START PLACING EQUS. OF COND. AND RT. HAND SIDES IN ROW INDEXED
C WITH RI AND PROCEED DOWNWARD FOR MEQ EQUS.
C
C THE SPACE A(I,J),(I = 1,....,RI-1 ,J=1,....,I-1) IS FREE AND
C NEVER REFERENCED AGAIN BY THIS PROGRAM AS RI INCREASES TOWARD N+2.BHSL 160
C
C NOW USE THE SECOND ENTRY BHSLR2.
C ..
C REAL A(NDA,N),B(NDB,NB),UP,ZERO
C DATA ZERO/0.E0/
C RI=1
C SMI=0
C RETURN
C
C PRIMARY ENTRY TO PACK ARRAY TO UPPER TRIANGULAR FORM.
C ..
C ENTRY BHSLR2(MEQ,RI)
C *****
C ..
C MEQ NEW EQUS. AND RT. HAND SIDES ENTER.
C
C IF (MEQ.LE.0) RETURN
C ..
C NO TRANSFORMATIONS NEEDED.
C
C SMI=SMI+MEQ
C M=RI+MEQ-1
C NT=MINU(M,N)
C DO 20 IP=1,NT
C IF (IP.EQ.M) GO TO 20
C L=MAXU(U,RI-IP-1)
C CALL AHLR1 (A(1,IP),1,UP,IP-1,L,M,A(1,IP+1),1,NDA,N-IP)
C ..
C COMPUTE TRANSFORMATION AND APPLY TO THE REMAINING COLUMNS.
C
C CALL AHLR3 (A(1,IP),1,UP,IP-1,L,M,B,1,NDB,NB)
C ..
C APPLY TRANSFORMATIONS TO B,IF PRESENT.
C
C L=L+IP+1
C DO 10 I=L,M
C 10 A(I,IP)=ZERO
C ..
C CLEAR AREA JUST MADE IMPLICITLY ZERO.
C
C 20 CONTINUE
C RI=MINU(SMI,N+1)+1

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```

IF (M.LE.N) RETURN          BHS 600
IF (NB.LE.0) RETURN          BHS 610
DO 30 J=1,NB                BHS 620
30 CALL SL2NRM (M-N,B(N+1,J),B(N+1,J))          BHS 630
C
C      ** PACK LENGTHS OF RT. HAND SIDES OUTSIDE THE COL. SPACE OF A
C      TO SINGLE LOCATIONS EACH.          BHS 640
C
C      ** ADVANCE NEW ORIGIN OF ROW TO START EQUS. OF CONDITION AND RT.SIDES          BHS 650
C
C      L=N+2          BHS 660
C      IF(L.GT.M) RETURN          BHS 670
C      DO 40 J=1,NB          BHS 680
C      DO 40 I=L,M          BHS 690
40 B(I,J)=ZERO          BHS 700
      RETURN          BHS 710
C
C      ** IF A SOLUTION IS DESIRED WITH FURTHER ACCUMULATION INTENDED,
C      SAVE THE UPPER TRIANGULAR PART OF THE A ARRAY AND THE FIRST          BHS 720
C      N+1 ROWS OF THE B ARRAY. FOLLOWING CALCULATION OF THE SOLUTION,          BHS 730
C      RESTORE THESE DATA AND ZERO THE PART OF A BELOW THE MAIN          BHS 740
C      DIAGONAL TOGETHER WITH THE (N+1)ST ROW. SEQ. ACCUMULATION MAY THEN          BHS 750
C      CONTINUE AS BEFORE. THE NUMBER OF ROWS IN THE PROCESSED MATRIX          BHS 760
C      TO BE SOLVED WILL BE RI-1.          BHS 770
C
C      END          BHS 780

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C      BHTFLR LIST BASIC H.H. TRANS. FROM THE LEFT. S.P.      10 JUN 68HTR00100
C      ENTRY POINTS..                                         HTR00200
C      HTR00300
C      AHLR1, AHLR2, AHLR3                                     HTR00400
C      11 FEB 1970                                         HTR00600
C      HTR00700
C      HTR00800
C      **
C      SUBROUTINE AHLR1 (U,NDU,UP,L1,L2,M,P,IRA,ICA,NCOLS) HTR00900
C      **
C      REAL U(NDU,M),UP,P(1),CL,ZERO                         HTR01000
C      DOUBLE PRECISION SM,DZERO,BETA                         HTR01100
C      LOGICAL SRCLAV,N1GTM,CMPU                            HTR01200
C      DATA DZERO/0.D0/                                       HTR01300
C      DATA ZERO/0.E0/                                       HTR01400
C      HTR01500
C      ..
C      DEFINE DATA FOR LITERALLY NAMED PROGRAM CONSTANTS.   HTR01600
C
C      REAL AV,SR,AM,SGN                                     HTR01700
C      AV(DUM)=ABS(DUM)                                    HTR01800
C      SR(DUM)=SQRT(DUM)                                   HTR01900
C      AM(D1,D2)=AMAX1(D1,D2)                             HTR02000
C      SGN(D1,D2)=SIGN(D1,D2)                            HTR02100
C
C      ..
C      DEFINE FUNCTIONS USED IN THIS SUBROUTINE.           HTR02200
C
C      CMPU=.TRUE.                                         HTR02300
C      SRCLAV=.FALSE.                                       HTR02400
C
C      ..
C      ENTIRE RAW U VECTOR IN THE FIRST ROW OF U.          HTR02500
C
C      GO TO 10                                           HTR02600
C
C      **
C      ENTRY AHLR2(U,NDU,UP,SRCL,L1,L2,M,P,IRA,ICA,NCOLS) HTR02700
C
C      **
C      REAL SRCL                                         HTR02800
C      CMPU=.TRUE.                                         HTR02900
C      SRCLAV=.TRUE.                                       HTR03000
C
C      ..
C      ENTIRE RAW U VECTOR IN THE FIRST ROW OF U. LENGTH OF U VECTOR IS HTR03100
C      AVAILABLE IN SRCL.                                 HTR03200
C
C      GO TO 10                                           HTR03300
C
C      **
C      ENTRY AHLR3(U,NDU,UP,L1,L2,M,P,IRA,ICA,NCOLS)     HTR03400
C
C      **
C      CMPU=.FALSE.                                         HTR03500
C      SRCLAV=.FALSE.                                       HTR03600
C
C      ..
C      U TRANSFORMATION CALCULATED AND IN U. PIVOT ELEMENT IS IN UP NOW. HTR03700
C
C      10 IF (L1.LT.0.OR.L2.LT.0.OR.M.LE.0) RETURN        HTR03800
C
C      ..
C      RETURN IF TRANSFORMATION IS ABSENT OR NOT WELL-DEFINED. HTR03900
C
C      N1=L1+L2+2                                         HTR04000
C      N1GTM=N1.GT.M                                      HTR04100
C      L1P1=L1+1                                         HTR04200
C      IF (.NOT.CMPU) GO TO 50                           HTR04300
C
C      CL=SRCL                                         HTR04400
C
C      ..
C      RETURN IF TRANSFORMATION IS ABSENT OR NOT WELL-DEFINED. HTR04500
C
C      ..
C      N1=L1+L2+2                                         HTR04600
C      N1GTM=N1.GT.M                                      HTR04700
C      L1P1=L1+1                                         HTR04800
C
C      ..
C      U TRANSFORMATION CALCULATED AND IN U. PIVOT ELEMENT IS IN UP NOW. HTR04900
C
C      10 IF (L1.LT.0.OR.L2.LT.0.OR.M.LE.0) RETURN        HTR05000
C
C      ..
C      RETURN IF TRANSFORMATION IS ABSENT OR NOT WELL-DEFINED. HTR05100
C
C      ..
C      N1=L1+L2+2                                         HTR05200
C      N1GTM=N1.GT.M                                      HTR05300
C      L1P1=L1+1                                         HTR05400
C
C      ..
C      RETURN IF TRANSFORMATION IS ABSENT OR NOT WELL-DEFINED. HTR05500
C
C      ..
C      N1=L1+L2+2                                         HTR05600
C      N1GTM=N1.GT.M                                      HTR05700
C      L1P1=L1+1                                         HTR05800
C
C      ..
C      RETURN IF TRANSFORMATION IS ABSENT OR NOT WELL-DEFINED. HTR05900
C
C      ..
C      N1=L1+L2+2                                         HTR06000
C      N1GTM=N1.GT.M

```

```

IF (SRCLAV) GO TO 40 HTR06100
CL=U(1,L1P1) HTR06200
IF (CL.LT.ZERO) CL=-CL HTR06300
IF (N1GTM) GO TO 40 HTR06400
DO 20 J=N1,M HTR06500
20 CL=AM(AV(U(1,J)),CL) HTR06600
IF (CL.LE.ZERO) RETURN HTR06700
SM=(U(1,L1P1)/CL)**2 HTR06800
DO 30 J=N1,M HTR06900
30 SM=SM+(U(1,J)/CL)**2 HTR07000
CL=CL*SR(SM) HTR07100
C   ..
C   COMPUTE LENGTH OF U VECTOR IF SRCLAV = .FALSE..
C
40 IF (CL.LE.ZERO) RETURN HTR07500
CL=-SGN(CL,U(1,L1P1)) HTR07600
UP=U(1,L1P1)-CL HTR07700
U(1,L1P1)=CL HTR07800
50 IF (NCOLS.LE.0) RETURN HTR07900
C   ..
C   RETURN IF MATRIX P IS ABSENT. HTR08000
C
BETA=U(1,L1P1)*UP HTR08300
IF (BETA.EQ.DZERO) RETURN HTR08400
C   ..
C   IF BETA.EQ.ZERO, NO TRANSFORMATION IS NECESSARY. HTR08500
C
DO 90 J=1,NCOLS HTR08800
C
C   APPLY HOUSEHOLDER TRANSFORMATION (I - 2*U*U**T) TO P HTR09000
C   FROM THE LEFT. HTR09100
C
C   IRA = NUMBER OF ROWS CELLS OF P ARE APART. HTR09300
C
C   ICA = NUMBER OF CELLS COLUMNS OF P ARE APART. HTR09500
C
C   U = (0,...,(L1 ZEROS), UP,0,...,(L2 ZEROS), U(L1+L2+21,...,U(M)) HTR09800
C   L1 .GE. 0, L2 .GE. 0. HTR09900
C   ..
I1=ICA*(J-1) HTR10100
I2=I1+L1*IRA+1 HTR10200
I4=I1+(N1-1)*IRA+1 HTR10300
SM=P(I2)*UP HTR10400
IF (N1GTM) GO TO 70 HTR10500
I3=I4 HTR10600
DO 60 I=N1,M HTR10700
SM=SM+P(I3)*U(1,I) HTR10800
60 I3=I3+IRA HTR10900
70 IF (SM.EQ.DZERO) GO TO 90 HTR11000
C   ..
C   TRANSFORMATION LEAVES THAT COLUMN OF P ALONE. HTR11200
SM=SM/BETA HTR11300
P(I2)=P(I2)-UP*SM HTR11400
IF (N1GTM) GO TO 90 HTR11500
I3=I4 HTR11600
DO 80 I=N1,M HTR11700
P(I3)=P(I3)-SM*U(1,I) HTR11800
80 I3=I3+IRA HTR11900

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AD-A060 045

JET PROPULSION LAB PASADENA CALTF  
COMBUSTION RESPONSE MODELING FOR COMPOSITE SOLID PROPELLANTS.(U)

F04611-76-X-0050

JUN 78 N S COHEN, J M BOWYER

F/G 19/1

JPL-PUB-78-59

AFRPL-TR-78-39

NL

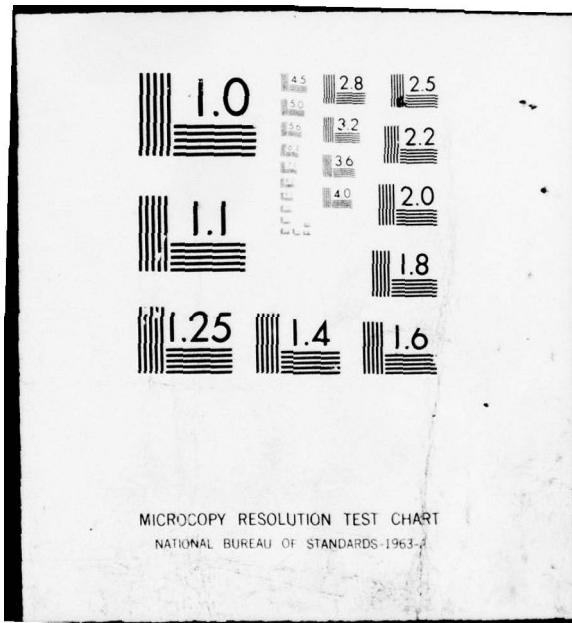
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MICROCOPY RESOLUTION TEST CHART  
NATIONAL BUREAU OF STANDARDS-1963-2

C .. HTR12000  
C BASIC STEP OF HOUSEHOLDER TRANSFORMATION. HTR12100  
C HTR12200  
C 90 CONTINUE HTR12300  
C .. HTR12400  
C RETURN WITH TRANSFORMATION APPLIED FROM THE LEFT. HTR12500  
C HTR12600  
C RETURN HTR12700  
C END HTR12800

```

C SUBROUTINE SL2NRM (N,U,G) L2N00100
C MODIFIED BY C J DEVINE 3/21/72 TO ALLOW ADDRESS OF .GT. 16 BITS FOR ARGS
C IN CALLING SEQ DUMMY DIMENSION ARRAY G(1),
C WAS DEFINED . THIS ALLOWS PROGRAM TO REFERENCE LOCATIONS IN EXT. CORE
C ENR2. S.P. AND D.P. L2 NORM FOR ARRAY BASED VECTORS 22 APR 68L2N00200
C 11 FEB 1970 L2N00300
REAL U(1), G(1) L2N00400
F1=0.E0 L2N00500
F2=0.E0 L2N00600
IF (N.LE.0) GO TO 20 L2N00700
DO 10 J=1,N L2N00800
10 F1=AMAX1(F1,ABS(U(J))) L2N00900
IF (F1.NE.0.) GO TO 30 L2N01000
20 G(1)=0.E0 L2N01100
RETURN L2N01200
30 DO 40 J=1,N L2N01300
T=U(J)/F1 L2N01400
40 F2=F2+T*T L2N01500
G(1)=F1*SQRT(F2) L2N01600
RETURN L2N01700
END L2N01800

```

```

FUNCTION SCPVAL (P,NDEGP,X)
C
C   C.L.LAWSON,JPL, 1969 DEC 17    MODIFIED 1973 JULY 24
C
C   MODIFIED 1974 NOV 19
C
C   EVALUATE A POLYNOMIAL OF DEGREE NDEGP GIVEN TRANSFORMATION
C   PARAMETERS, P(1) AND P(2), AND COEFFICIENTS RELATIVE TO THE
C   CHEBYSHEV BASIS.
C
C   NDEGP          DEGREE OF POLYNOMIAL
C   (P(I),I=1,NDEGP+3)  PARAMETERS DEFINING THE POLYNOMIAL
C   X              INPUT ARGUMENT
C   THE POLYNOMIAL-S VALUE AT X IS DEFINED AS FOLLOWS.
C
C   S = ( X - P(1) ) / P(2)
C
C   SCPVAL=SUM OF P(I+3)*T(I,S) FOR I=0,1,...NDEGP
C
C   WHERE T(I,S) DENOTES THE CHEBYSHEV
C   POLYNOMIAL OF DEGREE I EVALUATED AT S .
C
REAL          P(1),W(3),S,S2,X
W(1)=0.
W(2)=0.
C
C   TRANSFORM X TO S
S=(X-P(1))/P(2)
S2=S+S
J=NDEGP+3
C
C   EVALUATE POLYNOMIAL USING RECURSION
C
10   IF(J .LE. 3) GO TO 20
      W(3)=W(2)
      W(2)=W(1)
      W(1)=(S2*W(2)-W(3))+P(J)
      J = J - 1
      GO TO 10
20 SCPVAL=(S*W(1)-W(2))+P(3)
RETURN
END

```

```

SUBROUTINE SVDQ (NEQ,T,Y,F,KD,EP,IFLAG,H,HMINA,HMAXA,DELT,
1 TFINAL,MXSTEP,KSTEP,KEMAX,EMAX,KQ,YN,DT) SVDQ0001
C SVDQ0002
C VARIABLE ORDER INTEGRATION SUBROUTINE FOR THE SVDQ0003
C SOLUTION OF ORDINARY DIFFERENTIAL EQUATIONS SVDQ0004
C ANALYSIS AND CODING BY FRED T. KROGH, AT THE JET PROPULSION SVDQ0005
C LABORATORY, PASADENA, CALIF. APRIL 1, 1969. SVDQ0006
C THIS SUBROUTINE DESIGNED FOR THE IBM 7094 AND THE UNIVAC 1108. SVDQ0007
C AT THE END OF THIS LISTING INSTRUCTIONS ARE GIVEN FOR REMOVING SVDQ0008
C SOME FEATURES AND FOR ADDING OTHERS. THE GSTOP FEATURE IS SVDQ0009
C EXPLAINED NEAR THE END OF THE LISTING. SVDQ0010
C VARIABLES IN THE CALLING SEQUENCE HAVE THE FOLLOWING TYPES. SVDQ0011
C INTEGER NEQ,KD(1)+IFLAG,MXSTEP,KSTEP,KEMAX,KQ(1) SVDQ0012
C REAL F(1),EP(1),HMINA,HMAXA,EMAX,DT(10,1) SVDQ0013
C REAL T,Y(1)+H+DELT,TFINAL,YN(1) SVDQ0014
C PARAMETERS WHICH MUST BE ASSIGNED VALUES BEFORE CALLING SVDQ0015
C SVDQ ARE NEQ, T, Y, KD, H, HMINA, HMAXA, DELT, SVDQ0016
C TFINAL, AND MXSTEP. SVDQ0017
C SVDQ IS USED ONLY ON THE INITIAL ENTRY. ALL OTHER SVDQ0018
C ENTRIES ARE MADE BY CALLING SVDQ1. IN ADDITION TO SVDQ0019
C THE PARAMETERS MENTIONED ABOVE THE USER MUST ASSIGN SVDQ0020
C VALUES TO F (ONCE PER STEP INITIALLY, AND TWICE PER STEP SVDQ0021
C AFTER GETTING STARTED) AND EP (EITHER INITIALLY, OR DURING SVDQ0022
C THE INTEGRATION IF A RELATIVE ERROR TEST IS USED). SVDQ0023
C THE FOLLOWING PARAMETERS GIVE ADDITIONAL INFORMATION ABOUT THE SVDQ0024
C INTEGRATION AND ARE USED FOR STORAGE. THEY SHOULD NOT BE SVDQ0025
C CHANGED BY THE USER. IFLAG,KSTEP,KEMAX,EMAX,KQ,YN, AND DT. SVDQ0026
C
C
C AN EXAMPLE OF HOW ONE MIGHT SET UP THE CALLS TO SVDQ IS GIVEN SVDQ0027
C BELOW. SVDQ0028
C CALL SVDQ(NEQ,....,DT) SVDQ0029
C GO TO YYY SVDQ0030
C XXX CALL SVDQ1 SVDQ0031
C YYY GO TO (N1,N2,...,N8), IFLAG SVDQ0032
C AFTER THE INITIAL CALL, RETURN TO SVDQ WITH SVDQ0033
C GO TO XXX SVDQ0034
C IF NO ERROR HAS BEEN MADE, IFLAG WILL EQUAL 1 AFTER THE INITIAL SVDQ0035
C CALL INDICATING THE DERIVATIVES ARE TO BE COMPUTED. SVDQ0036
C
C
C THE USAGE OF THE VARIABLES IS GIVEN BELOW. SVDQ0037
C
C NEQ=NUMBER OF EQUATIONS (INPUT) SVDQ0038
C T=INDEPENDENT VARIABLE (INITIAL VALUE SUPPLIED BY THE USER) SVDQ0039
C Y=CURRENT VALUE OF DEPENDENT VARIABLE. THE INITIAL SVDQ0040
C VALUE OF Y MUST BE SPECIFIED BY THE USER BEFORE SVDQ0041
C THE FIRST ENTRY. THE DIMENSION OF Y MUST BE SVDQ0042
C AT LEAST AS GREAT AS THE SUM OF THE ORDERS OF SVDQ0043
C THE DIFFERENTIAL EQUATIONS WHICH ARE BEING SVDQ0044
C INTEGRATED. IF WE LET KD(I) DENOTE THE ORDER SVDQ0045
C OF THE I-TH DIFFERENTIAL EQUATION, THEN Y(J) SVDQ0046

```

C IS THE K-TH DERIVATIVE OF THE L-TH COMPONENT,  
 WHERE L IS THE SMALLEST INTEGER FOR WHICH  
 KD(1)+KD(2)+...+KD(L).GE.J AND K=KD(L)+J-1-(KD(1)  
 +KD(2)+...+KD(L)), J=1,2,...,(KD(1)+KD(2)+...+KD(NEQ)).  
 (FOR EXAMPLE, FOR THE SYSTEM F(1)=UPP, F(2)=VPP, WHERE P  
 DENOTES A PRIME, Y(1)=U, Y(2)=UP, Y(3)=V, Y(4)=VP.) SVDQ0060  
 SVDQ0061  
 SVDQ0062  
 SVDQ0063  
 SVDQ0064  
 SVDQ0065  
 SVDQ0066  
 SVDQ0067  
 SVDQ0068  
 SVDQ0069  
 SVDQ0070  
 SVDQ0071  
 SVDQ0072  
 SVDQ0073  
 SVDQ0074  
 SVDQ0075  
 SVDQ0076  
 SVDQ0077  
 SVDQ0078  
 SVDQ0079  
 SVDQ0080  
 SVDQ0081  
 SVDQ0082  
 SVDQ0083  
 SVDQ0084  
 SVDQ0085  
 SVDQ0086  
 SVDQ0087  
 SVDQ0088  
 SVDQ0089  
 SVDQ0090  
 SVDQ0091  
 SVDQ0092  
 SVDQ0093  
 SVDQ0094  
 SVDQ0095  
 SVDQ0096  
 SVDQ0097  
 SVDQ0098  
 SVDQ0099  
 SVDQ0100  
 SVDQ0101  
 SVDQ0102  
 SVDQ0103  
 SVDQ0104  
 SVDQ0105  
 SVDQ0106  
 SVDQ0107  
 SVDQ0108  
 SVDQ0109  
 SVDQ0110  
 SVDQ0111  
 SVDQ0112  
 SVDQ0113  
 SVDQ0114  
 SVDQ0115  
 SVDQ0116  
 SVDQ0117  
 SVDQ0118

C F(I)=KD(I)-TH DERIVATIVE OF THE I-TH COMPONENT WITH RESPECT  
 TO T, I=1,2,...,NEQ. THE USER MUST PROVIDE  
 THE CODE WHICH COMPUTES F GIVEN Y AND T. SVDQ0060  
 SVDQ0061  
 SVDQ0062  
 SVDQ0063  
 SVDQ0064  
 SVDQ0065  
 SVDQ0066  
 SVDQ0067  
 SVDQ0068  
 SVDQ0069  
 SVDQ0070  
 SVDQ0071  
 SVDQ0072  
 SVDQ0073  
 SVDQ0074  
 SVDQ0075  
 SVDQ0076  
 SVDQ0077  
 SVDQ0078  
 SVDQ0079  
 SVDQ0080  
 SVDQ0081  
 SVDQ0082  
 SVDQ0083  
 SVDQ0084  
 SVDQ0085  
 SVDQ0086  
 SVDQ0087  
 SVDQ0088  
 SVDQ0089  
 SVDQ0090  
 SVDQ0091  
 SVDQ0092  
 SVDQ0093  
 SVDQ0094  
 SVDQ0095  
 SVDQ0096  
 SVDQ0097  
 SVDQ0098  
 SVDQ0099  
 SVDQ0100  
 SVDQ0101  
 SVDQ0102  
 SVDQ0103  
 SVDQ0104  
 SVDQ0105  
 SVDQ0106  
 SVDQ0107  
 SVDQ0108  
 SVDQ0109  
 SVDQ0110  
 SVDQ0111  
 SVDQ0112  
 SVDQ0113  
 SVDQ0114  
 SVDQ0115  
 SVDQ0116  
 SVDQ0117  
 SVDQ0118

C KD GIVES THE ORDER OF THE DIFFERENTIAL EQUATIONS IN THE  
 SYSTEM. KD MUST BE LESS THAN OR EQUAL TO 4.  
 (FOR DIFFERENTIAL EQUATIONS WITH DIFFERENT ORDERS SET  
 KD.LT.U. IF THIS IS DONE IT IS ASSUMED THAT KD IS A VECTOR  
 AND THAT ABS(KD(I)) GIVES THE ORDER OF THE I-TH EQUATION.) SVDQ0060  
 SVDQ0061  
 SVDQ0062  
 SVDQ0063  
 SVDQ0064  
 SVDQ0065  
 SVDQ0066  
 SVDQ0067  
 SVDQ0068  
 SVDQ0069  
 SVDQ0070  
 SVDQ0071  
 SVDQ0072  
 SVDQ0073  
 SVDQ0074  
 SVDQ0075  
 SVDQ0076  
 SVDQ0077  
 SVDQ0078  
 SVDQ0079  
 SVDQ0080  
 SVDQ0081  
 SVDQ0082  
 SVDQ0083  
 SVDQ0084  
 SVDQ0085  
 SVDQ0086  
 SVDQ0087  
 SVDQ0088  
 SVDQ0089  
 SVDQ0090  
 SVDQ0091  
 SVDQ0092  
 SVDQ0093  
 SVDQ0094  
 SVDQ0095  
 SVDQ0096  
 SVDQ0097  
 SVDQ0098  
 SVDQ0099  
 SVDQ0100  
 SVDQ0101  
 SVDQ0102  
 SVDQ0103  
 SVDQ0104  
 SVDQ0105  
 SVDQ0106  
 SVDQ0107  
 SVDQ0108  
 SVDQ0109  
 SVDQ0110  
 SVDQ0111  
 SVDQ0112  
 SVDQ0113  
 SVDQ0114  
 SVDQ0115  
 SVDQ0116  
 SVDQ0117  
 SVDQ0118

C EP IS A PARAMETER USED TO CONTROL THE LOCAL ERROR.  
 IF EP IS POSITIVE THE LOCAL ERROR IS KEPT LESS  
 THAN EP IN ALL COMPONENTS OF THE DIFF. EQ.  
 (THE ESTIMATED LOCAL ERROR IS KEPT LESS THAN EP IN  
 THE (KD(I)-1)-ST DERIVATIVE OF THE I-TH COMPONENT. THUS  
 FOR EQUATIONS WITH ORDER GREATER THAN ONE, THE ERROR  
 IN A DERIVATIVE IS ESTIMATED. IN THIS CASE THE VALUE OF  
 EP REQUIRED TO OBTAIN A GIVEN ACCURACY IN THE DEPENDENT  
 VARIABLE DEPENDS ON THE SCALING.) SVDQ0060  
 SVDQ0061  
 SVDQ0062  
 SVDQ0063  
 SVDQ0064  
 SVDQ0065  
 SVDQ0066  
 SVDQ0067  
 SVDQ0068  
 SVDQ0069  
 SVDQ0070  
 SVDQ0071  
 SVDQ0072  
 SVDQ0073  
 SVDQ0074  
 SVDQ0075  
 SVDQ0076  
 SVDQ0077  
 SVDQ0078  
 SVDQ0079  
 SVDQ0080  
 SVDQ0081  
 SVDQ0082  
 SVDQ0083  
 SVDQ0084  
 SVDQ0085  
 SVDQ0086  
 SVDQ0087  
 SVDQ0088  
 SVDQ0089  
 SVDQ0090  
 SVDQ0091  
 SVDQ0092  
 SVDQ0093  
 SVDQ0094  
 SVDQ0095  
 SVDQ0096  
 SVDQ0097  
 SVDQ0098  
 SVDQ0099  
 SVDQ0100  
 SVDQ0101  
 SVDQ0102  
 SVDQ0103  
 SVDQ0104  
 SVDQ0105  
 SVDQ0106  
 SVDQ0107  
 SVDQ0108  
 SVDQ0109  
 SVDQ0110  
 SVDQ0111  
 SVDQ0112  
 SVDQ0113  
 SVDQ0114  
 SVDQ0115  
 SVDQ0116  
 SVDQ0117  
 SVDQ0118

C IFLAG IS USED FOR COMMUNICATION BETWEEN THE INTEGRATOR  
 AND THE PROGRAM WHICH CALLS IT. THE VALUE  
 OF IFLAG SHOULD NOT BE CHANGED BY THE USER.  
 THE FOLLOWING VALUES OF IFLAG HAVE THE FOLLOWING MEANINGS.  
 =1 THE VALUE OF Y FOR THE CURRENT STEP HAS BEEN  
 PREDICTED. THE USER SHOULD COMPUTE F AND CALL SVDQ1.  
 IF A RELATIVE ERROR TEST IS USED THE NEW VALUE  
 OF EP SHOULD ALSO BE COMPUTED HERE. SVDQ0060  
 SVDQ0061  
 SVDQ0062  
 SVDQ0063  
 SVDQ0064  
 SVDQ0065  
 SVDQ0066  
 SVDQ0067  
 SVDQ0068  
 SVDQ0069  
 SVDQ0070  
 SVDQ0071  
 SVDQ0072  
 SVDQ0073  
 SVDQ0074  
 SVDQ0075  
 SVDQ0076  
 SVDQ0077  
 SVDQ0078  
 SVDQ0079  
 SVDQ0080  
 SVDQ0081  
 SVDQ0082  
 SVDQ0083  
 SVDQ0084  
 SVDQ0085  
 SVDQ0086  
 SVDQ0087  
 SVDQ0088  
 SVDQ0089  
 SVDQ0090  
 SVDQ0091  
 SVDQ0092  
 SVDQ0093  
 SVDQ0094  
 SVDQ0095  
 SVDQ0096  
 SVDQ0097  
 SVDQ0098  
 SVDQ0099  
 SVDQ0100  
 SVDQ0101  
 SVDQ0102  
 SVDQ0103  
 SVDQ0104  
 SVDQ0105  
 SVDQ0106  
 SVDQ0107  
 SVDQ0108  
 SVDQ0109  
 SVDQ0110  
 SVDQ0111  
 SVDQ0112  
 SVDQ0113  
 SVDQ0114  
 SVDQ0115  
 SVDQ0116  
 SVDQ0117  
 SVDQ0118

C =2 THE VALUE OF Y FOR THE CURRENT STEP HAS BEEN  
 CORRECTED. THE USER SHOULD COMPUTE F AND CALL SVDQ1.  
 =3 AN OUTPUT POINT HAS BEEN REACHED (SEE DESCRIPTION  
 OF DELTI), PRINT RESULTS AND CALL SVDQ1.  
 =4 T=TFINAL IF SVDQ1 IS CALLED WITH T=TFINAL AND  
 IFLAG=4, IFLAG IS SET EQUAL TO 8. IF THE VALUE OF  
 TFINAL IS CHANGED THE INTEGRATION WILL CONTINUE.  
 =5 KSTEP=KSOUT (SEE THE DESCRIPTION OF MXSTEP).  
 =6 EMAX.GT..1 AND IT APPEARS TO THE SUBROUTINE THAT  
 REDUCING H WILL NOT HELP BECAUSE OF ROUND-OFF ERROR.  
 IF THIS OCCURS A LARGER VALUE OF EP (OR OF ABS(EP(KEMAX))) IF

C EP IS A VECTOR) SHOULD PROBABLY BE USED. IF EP IS NOT SVDQ0119  
 C INCREASED, TOO SMALL A STEPSIZE IS LIABLE TO BE USED. (WE HAVE SVDQ0120  
 C FOUND THAT REPLACING EP WITH 32.\*EMAX\*EP WORKS QUITE WELL.) SVDQ0121  
 C INCREASING EP IN THIS WAY WILL NOT DEGRADE THE ACCURACY, SVDQ0122  
 C HOWEVER IF THE NATURE OF THE PROBLEM CHANGES IT MAY PAY TO SVDQ0123  
 C USE A SMALLER VALUE OF EP LATER IN THE INTEGRATION. SVDQ0124  
 C =7 ABS(H).LT.HMINA. TO CONTINUE WITH THE CURRENT SVDQ0125  
 C VALUE OF H, SET HMINA.LE.ABS(H) AND CALL SVDQ1. SVDQ0126  
 C IF THE INTEGRATOR HAS JUST HALVED H ONE MAY CONTINUE SVDQ0127  
 C WITH TWICE THE STEPSIZE BY SIMPLY CALLING SVDQ1. (SUCH SVDQ0128  
 C AN ACTION IS RISKY WITHOUT A CAREFUL ANALYSIS OF THE SVDQ0129  
 C SITUATION.) IF THE STEPSIZE HAS NOT JUST BEEN HALVED SVDQ0130  
 C (ABS(H).LT.HMINA MAY BE DUE TO THE USER INCREASING THE SVDQ0131  
 C VALUE OF HMINA OR TO HAVING TOO SMALL AN H AT THE END SVDQ0132  
 C OF THE STARTING PHASE.) THE INTEGRATION WILL CONTINUE SVDQ0133  
 C WITH THE CURRENT VALUE OF H AND A RETURN TO THE USER WITH SVDQ0134  
 C IFLAG=7 WILL BE MADE ON EVERY STEP UNTIL ABS(H).GE.HMINA. SVDQ0135  
 C =8 ILLEGAL PARAMETER IN THE CALLING SEQUENCE. IF SVDQ1 SVDQ0136  
 C IS CALLED WITH IFLAG=8 THE PROGRAM IS STOPPED. SVDQ0137  
 C SVDQ0138  
 C H=CURRENT VALUE OF THE STEPSIZE. IN SELECTING THE INITIAL SVDQ0139  
 C VALUE FOR H, THE USER SHOULD REMEMBER THE FOLLOWING-- SVDQ0140  
 C 1. THE INTEGRATOR IS CAPABLE OF CHANGING H QUITE QUICKLY AND SVDQ0141  
 C THUS THE INITIAL CHOICE IS NOT CRITICAL. SVDQ0142  
 C 2. IF IT DOES NOT LEAD TO PROBLEMS IN COMPUTING THE DERIVATIVES SVDQ0143  
 C (E.G. BECAUSE OF OVERFLOW OR TRYING TO EXTRACT THE SQUARE SVDQ0144  
 C ROOT OF A NEGATIVE NUMBER), IT IS BETTER TO CHOOSE H MUCH SVDQ0145  
 C TOO LARGE THAN MUCH TOO SMALL. SVDQ0146  
 C 3. IF HDELT.LE.0 INITIALLY, AN IMMEDIATE RETURN IS MADE SVDQ0147  
 C WITH IFLAG=8. THE SIGN OF H IS WHAT DETERMINES THE SVDQ0148  
 C DIRECTION OF INTEGRATION. SVDQ0149  
 C 4. IF DELT=H\*(2\*\*K) K A NONNEGATIVE INTEGER THEN OUTPUT SVDQ0150  
 C VALUES WILL BE OBTAINED WITHOUT DOING AN INTERPOLATION. SVDQ0151  
 C SVDQ0152  
 C HMINA AFTER GETTING STARTED, AND WHENEVER H SVDQ0153  
 C IS HALVED, ABS(H) IS COMPARED WITH HMINA. SVDQ0154  
 C IF ABS(H).LT.HMINA CONTROL IS RETURNED TO SVDQ0155  
 C THE USER WITH IFLAG=7. SVDQ0156  
 C SVDQ0157  
 C HMAXA THE STEPSIZE IS NOT DOUBLED IF SVDQ0158  
 C DOING SO WOULD MAKE ABS(H).GT.HMAXA SVDQ0159  
 C SVDQ0160  
 C DELT ENABLES THE USER TO SPECIFY THE POINTS WHERE SVDQ0161  
 C OUTPUT IS DESIRED. LET TOUT=DELT + THE VALUE OF T THE LAST SVDQ0162  
 C TIME CONTROL WAS RETURNED TO THE USER WITH IFLAG=3. (INITIALLY SVDQ0163  
 C TOUT=THE INITIAL VALUE OF T.) CONTROL IS RETURNED TO THE SVDQ0164  
 C USER WITH IFLAG=3 WHENEVER T=TOUT. IF TOUT DOES NOT FALL SVDQ0165  
 C ON AN INTEGRATION STEP, OUTPUT VALUES ARE OBTAINED BY SVDQ0166  
 C INTERPOLATION ON THE FIRST STEP THAT (T-TOUT)\*H.GT.0. SVDQ0167  
 C INTERPOLATED VALUES FOR BOTH Y AND F ARE COMPUTED. SVDQ0168  
 C (NOTE THAT A RETURN WITH IFLAG=3 IS ALWAYS MADE SVDQ0169  
 C BEFORE TAKING THE FIRST STEP.) SVDQ0170  
 C SVDQ0171  
 C TFINAL CONTROL IS RETURNED TO THE USER WITH IFLAG=4 WHEN SVDQ0172  
 C T REACHES TFINAL. IF TFINAL DOES NOT FALL ON AN INTEGRATION SVDQ0173  
 C STEP VALUES AT TFINAL ARE OBTAINED BY EXTRAPOLATION. SVDQ0174  
 C SVDQ0175  
 C MXSTEP ON THE INITIAL ENTRY, AND ON ENTRIES SVDQ0176  
 C WITH 2.LT.IFLAG.LT.6 KSOUT IS SET EQUAL TO SVDQ0177

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C KSTEP+MXSTEP. AT THE END OF EACH STEP KSTEP IS INCREMENTED      SVDQ0178
C AND COMPARED WITH KSOUT. IF KSTEP.GE.KSOUT CONTROL IS           SVDQ0179
C RETURNED TO THE USER WITH IFLAG=5. (THUS IF DELT IS           SVDQ0180
C SUFFICIENTLY LARGE, CONTROL WILL BE RETURNED TO THE USER       SVDQ0181
C WITH IFLAG=5 EVERY MXSTEP STEPS.)                               SVDQ0182
C                                                               SVDQ0183
C KSTEP=NUMBER OF INTEGRATION STEPS TAKEN (COMPUTED             SVDQ0184
C BY THE INTEGRATOR.)                                         SVDQ0185
C                                                               SVDQ0186
C KEMAX=INDEX OF COMPONENT RESPONSIBLE FOR THE                 SVDQ0187
C VALUE OF EMAX (SEE BELOW).                                     SVDQ0188
C                                                               SVDQ0189
C EMAX=LARGEST VALUE IN ANY COMPONENT OF (ESTIMATED ERROR)/EP   SVDQ0190
C ORDINARILY THE STEPSIZE IS HALVED IF EMAX.GT..1. WITH A        SVDQ0191
C RECENT HISTORY OF LOCAL ROUND-OFF PROBLEMS VALUES OF EMAX AS  SVDQ0192
C LARGE AS 1 ARE PERMITTED. THE STEPSIZE IS NOT HALVED ON ANY     SVDQ0193
C STEP THAT ROUND OFF ERROR APPEARS TO BE LIMITING THE PRECISION. SVDQ0194
C                                                               SVDQ0195
C KQ(I)=HIGHEST ORDER DIFFERENCE USED IN INTEGRATING          SVDQ0196
C THE I-TH EQUATION. (COMPUTED BY THE INTEGRATOR)               SVDQ0197
C                                                               SVDQ0198
C YN=A VECTOR WITH THE DIMENSION OF Y USED TO STORE            SVDQ0199
C THE VALUE OF Y AT THE END OF EACH INTEGRATION STEP.           SVDQ0200
C                                                               SVDQ0201
C DT=AN ARRAY WITH DIMENSION DT(10,NEQ) USED TO                SVDQ0202
C STORE THE DIFFERENCE TABLE.                                 SVDQ0203
C                                                               SVDQ0204
C                                                               SVDQ0205
C REAL TOUT,TL,TPD,TPD1,TPD2,HH,FAC                         SVDQ0206
C DIMENSION DD(12),D(11),GAM(10,4),GAS(10),PT(11),FAC(3)    SVDQ0207
C EQUIVALENCE(DD(2),D(1))                                    SVDQ0208
C                                                               SVDQ0209
C DATA KMAX0/4/                                              SVDQ0210
C KMAX0 IS THE MAXIMUM ORDER DIFFERENTIAL EQUATION          SVDQ0211
C THIS SUBROUTINE WILL INTEGRATE.                            SVDQ0212
C                                                               SVDQ0213
C DATA FAC/1.E0,,5E0,,166666667E0/                          SVDQ0214
C FAC(J)=1/(FACTORIAL J), J=1,2,...,MAX(2,KMAX0-1)         SVDQ0215
C                                                               SVDQ0216
C DATA KQMAX/9/                                              SVDQ0217
C KQMAX GIVES THE MAXIMUM ORDER.                           SVDQ0218
C THERE IS LITTLE POINT IN HAVING KQMAX MUCH BIGGER THAN THE NUMBER SVDQ0219
C OF DECIMAL DIGITS IN THE MANTISSA.                      SVDQ0220
C IF KQMAX IS SET LESS THAN 6, DT, D, AND PT SHOULD BE DIMENSIONED SVDQ0221
C AS IF KQMAX=6.                                         SVDQ0222
C                                                               SVDQ0223
C DATA RND•KBIT2/5.0E-8,56/                                SVDQ0224
C RND IS APPROXIMATELY 2**(-B) WHERE B IS                  SVDQ0225
C THE NUMBER OF BITS IN THE MANTISSA.                      SVDQ0226
C KBIT2=2*B+2 WHERE B IS THE NUMBER OF BITS IN THE MANTISSA. SVDQ0227
C IF THE DERIVATIVES ARE NOT COMPUTED TO THE ACCURACY EXPECTED SVDQ0228
C FROM THE WORD LENGTH OF THE COMPUTER (FOR EXAMPLE BECAUSE OF SVDQ0229
C CANCELLATION PROBLEMS OR TABULAR DATA), THEN THESE CONSTANTS SVDQ0230
C CAN BE CHANGED TO REFLECT THE NUMBER OF BITS WHICH ARE      SVDQ0231
C SIGNIFICANT IN THE COMPUTED DERIVATIVES. (THIS IS NOT NECESSARY, SVDQ0232
C BUT IS WISE IF THE ACCURACY REQUESTED IS DIFFICULT TO OBTAIN SVDQ0233
C BECAUSE THE DERIVATIVES HAVE SO FEW SIGNIFICANT DIGITS.)     SVDQ0234
C                                                               SVDQ0235
C DATA P1,P01,P25,P3E1/.1,.01,.25,3./                     SVDQ0236

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C THE ABOVE DATA STATEMENT CONTAINS VARIOUS CONSTANTS  
 C USED IN THE SUBROUTINE. SVDQ0237  
 C  
 C DATA PT/1.,2.,4.,8.,16.,32.,64.,128.,256.,512.,1024./ SVDQ0238  
 C PT(J)=2\*\*(J-1), J=1,2,...,KQMAX+2 SVDQ0239  
 C EQUIVALENCE (PT(1),PTS1),(PT(2),PTS2),(PT(3),PTS3),(PT(4),PTS4), SVDQ0240  
 1 (PT(5),PTS5),(GAM(2,1),P5) SVDQ0241  
 C  
 C DATA GAS/1.,-.5,-8.3333333E-02,-4.1666667E-02, SVDQ0242  
 1 -2.6388889E-02,-1.875E-02,-1.42691799E-02, SVDQ0243  
 2 -1.13673942E-02,-9.35653660E-03, SVDQ0244  
 3 -7.89255401E-03/ SVDQ0245  
 C GAS(I) GIVES THE I-TH ADAMS-MOULTON CORRECTOR SVDQ0246  
 C COEFFICIENT, I=1,2,...,KQMAX+1. SVDQ0247  
 C  
 C DATA GAM/1.,.5,.416666667,.375,.348611111,.329861111, SVDQ0248  
 1 .315591931 ,.304224537,.294868000,.286975446, SVDQ0249  
 2 .5,.166666667,.125,.105555556,9.375E-02, SVDQ0250  
 3 8.56150794E-02,7.95717593E-02,7.48522928E-02, SVDQ0251  
 4 7.10329861E-02,6.78584998E-02, SVDQ0252  
 5 .166666667,4.1666667E-02,2.9166667E-02, SVDQ0253  
 6 2.36111111E-02,2.03373016E-02,1.81299603E-02, SVDQ0254  
 7 1.65181327E-02,1.52772266E-02,1.42851882E-02, SVDQ0255  
 8 1.34693966E-02, SVDQ0256  
 9 4.15666667E-02,8.3333333E-03,5.55555556E-03, SVDQ0257  
 \$ 4.36507937E-03,3.67890212E-03,3.22365520E-03, SVDQ0258  
 \$ 2.89544753E-03,2.64543584E-03,2.44737491E-03, SVDQ0259  
 \$ 2.28579544E-03/ SVDQ0260  
 C GAM(I,J) GIVES THE I-TH ADAMS-FALKNER PREDICTOR SVDQ0261  
 C COEFFICIENT FOR INTEGRATING J-TH ORDER DIFFERENTIAL SVDQ0262  
 C EQUATIONS, I=1,2,...,KQMAX+1, J=1,2,...,KMAX0. SVDQ0263  
 C  
 C DIMENSION LTA(8,8) SVDQ0264  
 C DATA (ETA(I, 1), I=1, 8)/ 3.3333330E-01, 2.50000000E-01, SVDQ0265  
 1 1.13636360E-01, 6.73076930E-02, 4.60526330E-02, 3.43749980E-02, SVDQ0266  
 2 2.71381590E-02, 2.22547310E-02/ SVDQ0267  
 C DATA (ETA(I, 2), I=1, 8)/ 2.00000000E-01, 4.00000000E-01, SVDQ0268  
 1 3.40909090E-01, 2.01923080E-01, 1.38157900E-01, 1.03124990E-01, SVDQ0269  
 2 8.14144780E-02, 6.67641930E-02/ SVDQ0270  
 C DATA (ETA(I, 3), I=1, 8)/ 1.42857140E-01, 2.85714280E-01, SVDQ0271  
 1 3.42857140E-01, 3.46153840E-01, 2.45614040E-01, 1.87500000E-01, SVDQ0272  
 2 1.50303650E-01, 1.24626490E-01/ SVDQ0273  
 C DATA (ETA(I, 4), I=1, 8)/ 1.11111110E-01, 2.22222220E-01, SVDQ0274  
 1 2.85714280E-01, 2.53968250E-01, 3.07017540E-01, 2.50000000E-01, SVDQ0275  
 2 2.08755060E-01, 1.78037850E-01/ SVDQ0276  
 C DATA (ETA(I, 5), I=1, 8)/ 9.09090910E-02, 1.81818180E-01, SVDQ0277  
 1 2.42424240E-01, 2.42424240E-01, 1.73160170E-01, 2.50000000E-01, SVDQ0278  
 2 2.27732800E-01, 2.05428290E-01/ SVDQ0279  
 C DATA (ETA(I, 6), I=1, 8)/ 7.69230760E-02, 1.53846150E-01, SVDQ0280  
 1 2.09790210E-01, 2.23776220E-01, 1.86480190E-01, 1.11888110E-01, SVDQ0281  
 2 1.91295550E-01, 1.91733070E-01/ SVDQ0282  
 C DATA (ETA(I, 7), I=1, 8)/ 6.66666660E-02, 1.33333330E-01, SVDQ0283  
 1 1.84615380E-01, 2.05128200E-01, 1.86480190E-01, 1.34265730E-01, SVDQ0284  
 2 6.96192690E-02, 1.39442230E-01/ SVDQ0285  
 C DATA (ETA(I, 8), I=1, 8)/ 5.88235290E-02, 1.17647060E-01, SVDQ0286  
 1 1.64705880E-01, 1.88235290E-01, 1.80995470E-01, 1.44796380E-01, SVDQ0287  
 2 9.21431500E-02, 4.21225830E-02/ SVDQ0288  
 C ETA(I,J) I=1,2,...,J IS USED IN THE FIRST MODIFICATION OF THE SVDQ0289  
 C J-TH DIFFERENCE OF A J-TH ORDER METHOD AFTER THE STEPSIZE IS SVDQ0290

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C HALVED.
C ETA(I,J) J=1,2,...,I-1 IS USED IN THE SECOND MODIFICATION OF      SVDQ0296
C THE (J+1)-ST DIFFERENCE OF AN I-TH ORDER METHOD.                  SVDQ0297
C THE TWO MODIFICATIONS OF THE DIFFERENCE TABLE AFTER HALVING THE      SVDQ0298
C STEPSIZE REMOVES MOST OF THE INSTABILITY INHERENT IN THE METHOD      SVDQ0299
C USED HERE FOR HALVING THE STEPSIZE.                                SVDQ0300
C
C
C IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE FOLLOWING CARD.      SVDQ0301
C DATA LGSS,LGSD,LGSE/0,0,0/                                         SVDQ0302
C
C *****
C THE STATEMENTS BETWEEN THE LINE ABOVE AND A SIMILAR LINE BELOW      SVDQ0303
C ARE INSERTED IN THE JPL VERSION OF THIS SUBROUTINE TO INSURE        SVDQ0304
C THAT THE CODE IS COMPILED CORRECTLY. THESE STATEMENTS THEMSELVES     SVDQ0305
C ARE NOT ACTUALLY COMPILED.                                         SVDQ0306

C
C NEQ=NEQ
C HMINA=HMINA
C HMAXA=HMAXA
C DELT=DELT
C TFINAL=TFINAL
C MXSTEP=MXSTEP

C *****
C
C INITIALIZE
C KSTEP=-1
C NE=NEQ
C IF (NE.LE.0) GO TO 1190
C HH=H
C NV=0
C KDMAX=0
C KDD=KD(1)
C KDS=KDD
C DO 10 I=1,NE
C KQ(I)=1
C DT(1,I)=0.
C IF (KDS.LE.0) KDD=IABS(KD(I))
C IF ((KDD.EQ.0).OR.(KDD.GT.KMAX)) HH=0.E0
C IF (KDD.GT.KDMAX) KDMAX=KDD
C 10 NV=NV+KDD

C
C IF ((DELT*HH).LE.0.E0) GO TO 1190
C ERRMX=P1
C EMAX=ERND
C RNDc=RND*P25
C LDOUB=0
C E2HFAC=P25
C LSC=8
C LSTC=4

C LSC AND LSTC ARE USED IN COMBINATION AS FOLLOWS
C LSTC=4, LSC=4 FIRST TIME THROUGH THE FIRST STEP      SVDQ0334
C LSTC=3, LSC=4 SECOND TIME THROUGH THE FIRST STEP      SVDQ0335
C (NECESSARY TO CHECK STABILITY)                         SVDQ0336
C LSTC=2, LSC=4 THIRD TIME THROUGH THE FIRST STEP      SVDQ0337
C (ONLY OCCURS IF INSTABILITY POSSIBLE)                 SVDQ0338
C LSTC=2, LSC=2 SECOND STEP (IF KQ(I)=2, I=1,...,NEQ)   SVDQ0339
C LSTC=1, LSC=0 STARTING, ONE DERIVATIVE EVAL. PER STEP. SVDQ0340
C LSTC=1, LSC.GT.0 SET WHEN STARTING TWO DERIV. EVAL. PER STEP SVDQ0341

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C      LSTC=-1 LSC.LT.0 SET WHEN HALVING THE STEPSIZE          SVDQ0342
C      IN THE LAST TWO CASES LSC IS SET EQUAL TO LSTC*(MAXIMUM KQ(I))    SVDQ0343
C      +1). AT THE END OF EACH STEP IF LSC.NE.0 IT IS REPLACED BY    SVDQ0344
C      LSC-LSTC UNTIL LSC=0, AT WHICH TIME LSTC IS SET EQUAL TO 0.    SVDQ0345
C      WHEN DOUBLING H, LSTC IS SET EQUAL TO -1 AND LSC TO -3.    SVDQ0346
C      UNDER CERTAIN CONDITIONS WHEN KQ(I)=1, LSTC IS SET =-1 AND LSC=-5SVDQ0347
C
C      KSOUT=MXSTEP
C      TOUT=T
C      IFL=13
20  IFLAG=1
      GO TO 315
C      END OF INITIALIZATION
C
C      ENTRY SVDQ1
C
C      TO OUTPUT VARIABLES IN THE CALLING SEQUENCE REMOVE THE C-S          SVDQ0357
C      IN COLUMN ONE OF THE FOLLOWING CARDS UNTIL REACHING THE COMMENT      SVDQ0358
C      END OF CODE FOR PRINTING VARIABLES IN CALLING SEQUENCE.          SVDQ0359
C      IF (NEQ.NE.0) GO TO 28
C      NEQ=1
C 22 WRITE(6,5000) T,DELT,HMINA,HMAXA,KEMAX,EMAX,IFLAG,TFINAL,MXSTEP      SVDQ0360
C5000 FORMAT(3H0T=1PE15.8,7H DELT=E12.5,8H HMINA=,E10.3,8H HMAXA=,
C      1 E10.3,8H KEMAX=,I2,7H EMAX=E10.3,8H IFLAG=,I2/
C      2 9H I KQ KD,7X,4HF(I),9X,1HJ,8X,4HY(J),13X,5HYN(J),
C      3 10X,7HTFINAL=1E15.8,9H MXSTEP=I4)
C      J=1
C      DO 24 I=1,NE
C      IF (KDS.LT.0) KDD=IABS(KD(I))
C      K=KDD
C      WRITE(6,5001) I,KQ(I),KDD,F(I),J,Y(J),YN(J)
C5001 FORMAT(1H ,I2,2I3,1PE17.8,I4,2E17.8)
C 23 J=J+1
C      K=K-1
C      IF (K.EQ.0) GO TO 24
C      WRITE(6,5002) J,Y(J),YN(J)
C5002 FORMAT(26X,I4,1P2E17.8)
C      GO TO 23
C 24 CONTINUE
C      WRITE(6,5003)
C5003 FORMAT(3H0 I,15X,16HDIFFERENCE TABLE)
C      DO 27 I=1,NE
C      KQQ=KQ(I)+1
C      K=MIN0(KQQ,7)
C      WRITE(6,5004) I,(DT(IO,I),IO=1,K)
C5004 FORMAT(1H ,I2,1PE19.8,6E16.7)
C
C      IF (K.EQ.KQQ) GO TO 27
C      K=K+1
C      WRITE(6,5005) (DT(IO,I),IO=K,KQQ)
C5005 FORMAT(1H ,1PE21.5,7E14.5)
C 27 CONTINUE
C      IF (NEQ.EQ.0) RETURN
C      NEG=0
C 28 CONTINUE
C      END OF CODE FOR PRINTING VARIABLES IN CALLING SEQUENCE.

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      IF (Z-IFL) 30,60,320
      30 IF (IFL.GT.5) GO TO 1180
C
C      SET STEP STOP
      K$OUT=KSTEP+MXSTEP
      IF (IFL-4) 40,1210,210
C
C      SET PRINT STOP
      40 TOUT=T+DELT
C
      50 PTS1=ABS(AMOD((TOUT-TL)/HH,PTS2)-PTS1)
      LFD=-1
      IF (PTS1.GE.P5) LFD=1
C
C      LFD IS USED TO INDICATE WHETHER DOUBLING H IS PERMITTED.
C      IF LFD.LT.0 AT THE END OF A STEP THEN DOUBLING H IS
C      NOT PERMITTED. THE SIGN OF LFD IS CHANGED JUST BEFORE THE
C      END OF EACH STEP. IF DELT=H*(POWER OF 2) THEN
C      OUTPUT VALUES WILL BE OBTAINED WITHOUT INTERPOLATION.
C
      GO TO 200
C
C      ENTRY WITH IFLAG=2
C
C      UPDATE DIFFERENCE TABLE
C      AND COMPUTE KQM=MAXIMUM VALUE OF KQ(I), I=1,2,....,NEQ.
C
      60 KQM=0
      DO 80 I=1,NE
      KQQ=KQ(I)
      IF (KQQ.GT.KQM) KQM=KQQ
      D(1)=F(I)
      DO 70 K=1,KQQ
      D(K+1)=D(K)-DT(K,I)
      70 DT(K,I)=D(K)
      DT(KQQ+1,I)=D(KQQ+1)
      80 CONTINUE
C      END OF UPDATING DIFFERENCE TABLE
C
C      STORE Y(J) IN YN(J)
      DO 90 J=1,NV
      90 YN(J)=Y(J)
C
      LFD=-LFD
      TL=T
      KSTEP=KSTEP+1
C
C      IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE 2 FOLLOWING CARDS.
      IF (LGSS) 1430,1110,1510
      100 IFLAG=2
      110 IF (LSC.EQ.0) GO TO 140
      LSC=LSC-LSTC
      IF (LSC.EQ.0) GO TO 130
      IF (LSTC.NE.(-1)) GO TO 140
      IF (LDOUB.LT.0) RNDC=RND*P1
      120 E2HAVE=E2HMAX
      PTS1=PTS1

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GO TO 190                                     SVDQ0460
130 IF (ABS(HH).LT.HMINA) GO TO 1000          SVDQ0461
LSTC=0                                         SVDQ0462
140 IF (LDOUB.NE.1) GO TO 150                 SVDQ0463
IF ((LFD.GT.0).AND.(ABS(HH+HH).LE.HMAXA)) GO TO 1030   SVDQ0464
GO TO 200                                         SVDQ0465
150 RQMAX=PTS1/FLOAT(KQM+3)                   SVDQ0466
IF (LSTC.NE.0.OR.E2HAVE.EQ.0.E0)             GO TO 120   FK
TPS1=E2HMAX/E2HAVE                           SVDQ0468
IF (TPS1-PTS1) 160,190,170                  SVDQ0469
160 E2HFAC=AMAX1(.075E0,E2HFAC-RQMAX,E2HFAC*TPS1)   SVDQ0470
GO TO 180                                         SVDQ0471
170 TPS1=TPS1*TPS1                           SVDQ0472
E2HFAC=AMIN1(PTS1,E2HFAC*TPS1)               SVDQ0473
180 RNDC=(1.1-E2HFAC)*RND                   SVDQ0474
E2HAVE=P5*(E2HMAX+E2HAVE)                   SVDQ0475
190 ERRMX=AMAX1(P1,ERRMX-RQMAX*TPS1)         SVDQ0476
C     E2HFAC IS A FACTOR WHICH IS TAKEN TIMES AN INITIAL ESTIMATE OF
C     E2H TO GET A FINAL VALUE OF E2H. (E2H=ESTIMATE OF WHAT
C     (ESTIMATED ERROR)/(REQUESTED ERROR) WOULD BE IF H WERE
C     DOUBLED.)
C     E2HMAX IS THE MAXIMUM VALUE OF THE INITIAL ESTIMATE OF E2H OVER
C     ALL COMPONENTS WITH KQ(I).GT.1.                         SVDQ0481
C     E2HAVE IS A WEIGHTED AVERAGE OF PAST VALUES OF E2HMAX.
C     THE VALUE OF E2HFAC TENDS TO BE SMALLER WHEN E2HMAX IS
C     CONSISTANTLY SMALLER THAN E2HAVE.                         SVDQ0482
C
C     CHECK FOR PRINT STOP AND FOR T REACHING TFINAL           SVDQ0488
200 TPD=(TOUT-TL)/HH                                SVDQ0489
TPD1=(TFINAL-TL)/HH                               SVDQ0490
C
C     IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE FOLLOWING CARD.  SVDQ0491
IF (LGSE.LT.0) GO TO 1780                         SVDQ0492
IF (TPD1.LT.FAC(1)) GO TO 1220                   SVDQ0493
IF (TPD.LE.0.E0) GO TO 1280                         SVDQ0494
C
C     CHECK FOR STEP STOP                                SVDQ0496
IF (KSOUT.GT.KSTEP) GO TO 210                     SVDQ0497
C
IFL=5                                              SVDQ0498
GO TO 310                                         SVDQ0499
C
C     CHECK TO SEE IF ROUND-OFF ERROR IS PROMINENT          SVDQ0500
210 IF (EMAX.EQ.ERND) GO TO 220                   SVDQ0501
C     IT IS
IFL=6                                              SVDQ0502
IF (EMAX.GE.P1) GO TO 310                         SVDQ0503
IF ((LSTC.GE.0).OR.(LDOUB.EQ.1)) ERRMX=PTS1      SVDQ0504
C
220 IFL=1                                         SVDQ0505
230 T=TL+HH                                       SVDQ0506
C
C     START A NEW STEP                                 SVDQ0507
C
C     PREDICT                                         SVDQ0508
240 J=0                                           SVDQ0509
DO 290 I=1,NE
IF (KDS.LE.0) KDD=IABS(KD(I))                    SVDQ0510
IF (KDS.LE.0) KDD=IABS(KD(I))                    SVDQ0511
C
C     START A NEW STEP                                 SVDQ0512
C
C     PREDICT                                         SVDQ0513
240 J=0                                           SVDQ0514
DO 290 I=1,NE
IF (KDS.LE.0) KDD=IABS(KD(I))                    SVDQ0515
IF (KDS.LE.0) KDD=IABS(KD(I))                    SVDQ0516
IF (KDS.LE.0) KDD=IABS(KD(I))                    SVDQ0517
IF (KDS.LE.0) KDD=IABS(KD(I))                    SVDQ0518

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KDC=KDD	SVDQ0519
250 KQQ=KQ(I)	SVDQ0520
TPD=0.EU	SVDQ0521
K=KDC	SVDQ0522
260 TPD=TPD+DT(KQQ,I)*GAM(KQQ,KDC)	SVDQ0523
KQQ=KQQ-1	SVDQ0524
IF (KQQ.GT.0) GO TO 260	SVDQ0525
270 K=K-1	SVDQ0526
IF (K.LE.0) GO TO 280	SVDQ0527
L=J+K	SVDQ0528
TFD=YN(L+1)*FAC(K)+HH*TPD	SVDQ0529
GO TO 270	SVDQ0530
280 J=J+1	SVDQ0531
Y(J)=YN(J)+HH*TPD	SVDQ0532
KDC=KDC-1	SVDQ0533
IF (KDC.GT.0) GO TO 250	SVDQ0534
290 CONTINUE	SVDQ0535
C END OF PREDICT	SVDQ0536
C IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE C IN COLUMN ONE	SVDQ0537
C OF THE 2 FOLLOWING CARDS	SVDQ0538
C IF (IFL) 20,320,300	SVDQ0539
C 300 CONTINUE	SVDQ0540
C AND THEN REMOVE THE 2 FOLLOWING CARDS.	SVDQ0541
C IF (IFL) 1240,320,300	SVDQ0542
C 300 IF (LGSD.NE.0) GO TO 1520	SVDQ0543
C	SVDQ0544
310 IFLAG=IFL	SVDQ0545
315 CONTINUE	SVDQ0546
C TO OUTPUT VARIABLES IN THE CALLING SEQUENCE REMOVE THE C IN	SVDQ0547
C COLUMN ONE OF THE FOLLOWING CARD.	SVDQ0548
C IF (NEQ.EQ.0) GO TO 22	SVDQ0549
C	SVDQ0550
C RETURN	SVDQ0551
C	SVDQ0552
C ENTRY WITH IFLAG=1	SVDQ0553
320 EPS=EP(1)	SVDQ0554
ERND=0.	SVDQ0555
EMAX=0.	SVDQ0556
E2HMAX=0.	SVDQ0557
J=0	SVDQ0558
IF (LDOUB.GE.0) LDOUB=1	SVDQ0559
C	SVDQ0560
C LDOUB IS SET IN THE LOOP BELOW AS FOLLOWS	SVDQ0561
C LDOUB=0 HALVE	SVDQ0562
C LDOUB=1 DOUBLE	SVDQ0563
C LDOUB=2 DO NOT DOUBLE	SVDQ0564
C	SVDQ0565
C LDOUB,LT.0 AT THE BEGINNING OF THE LOOP INDICATES THE FOLLOWING	SVDQ0566
C --3 STEPSIZE HAS JUST BEEN HALVED. IF A DISCONTINUITY IS	SVDQ0567
C NOT INDICATED MODIFY THE DIFFERENCE TABLE AND REPEAT	SVDQ0568
C THE STEP.	SVDQ0569
C --2 STEP AFTER LDOUB=-3. PROCEED AS USUAL (ORDER IS NOT	SVDQ0570
C CHANGED)	SVDQ0571
C --1 STEP AFTER LDOUB=-2. MODIFY THE DIFFERENCE TABLE ONCE	SVDQ0572
C AGAIN AND REPEAT THE STEP.	SVDQ0573
C IF LDOUB IS SET EQUAL TO -4 THE ORDER IN AT LEAST ONE COMPONENT	SVDQ0574
	SVDQ0575
	SVDQ0576
	SVDQ0577

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C HAS BEEN GREATLY REDUCED AND THE STEP IS REPEATED.          SVDQ0578
C                                                               SVDQ0579
C                                                               SVDQ0580
C IF THE OUTPUT OPTION IS ELIMINATED, REMOVE THE 4 FOLLOWING CARDS. SVDQ0581
C IF (INEQ.LE.0) WRITE (6,5020) LSC,LFD,LSTC,KSTEP,E2HFAC,ERRMX,HH SVDQ0582
5020 FORMAT (19H0 I KQQ LRND LDOUB,5X,1HE,9X,3HE2H,               SVDQ0583
           1 8X,3HEPS,3X,4HLSC=,I3,6H LFD=,I2,7H LSTC=,I2,8H KSTEP=,I4, SVDQ0584
           2 9H E2HFAC=,F4.2,8H ERRMX=,F4.2,4H H=.1PE9.2)            SVDQ0585
C                                                               SVDQ0586
C                                                               SVDQ0587
C BEGINNING OF LOOP FOR CORRECTING, ESTIMATING THE ERROR,      SVDQ0588
C AND ADJUSTING THE NUMBER OF DIFFERENCES USED.                 SVDQ0589
C                                                               SVDQ0590
C DO 790 I=1,NE                                              SVDQ0591
C IF (KDS.LE.0) KDD=IABS(KD(I))                            SVDQ0592
C KQQ=KQ(I)                                              SVDQ0593
C KQQ GIVES THE ORDER OF THE PREDICTOR FORMULA AND KQQ+1 THE SVDQ0594
C ORDER OF THE CORRECTOR FORMULA.                           SVDQ0595
C                                                               SVDQ0596
C KQ1=KQQ+1                                              SVDQ0597
C D(1)=F(I)                                              SVDQ0598
C FORM THE DIFFERENCE TABLE FROM PREDICTED DERIVATIVE VALUES. SVDQ0599
C DO 330 K=1,KQ1                                         SVDQ0600
C D(K+1)=D(K)-DT(K,I)                                     SVDQ0601
330 CONTINUE                                              SVDQ0602
C D(K) GIVES THE (K-1)-ST DIFFERENCE FORMED FROM PREDICTED SVDQ0603
C DERIVATIVE VALUES                                         SVDQ0604
C TPS3=ABS(D(KQQ+1))                                      SVDQ0605
C IF (LDOUB.LT.0) GO TO 720                                SVDQ0606
C                                                               SVDQ0607
C 340 IF (KQQ.NE.1) GO TO 520                                SVDQ0608
C                                                               SVDQ0609
C KQ(I)=1 IS TREATED AS A SPECIAL CASE                      SVDQ0610
C E2H=TPS2                                              SVDQ0611
C TPS5=DT(3,I)                                           SVDQ0612
C IF (LSTC.LT.2) GO TO 370                                SVDQ0613
C FIRST STEP OF INTEGRATION                               SVDQ0614
C IF (LSTC.NE.4) GO TO 350                                SVDQ0615
C TPS4=0.                                                 SVDQ0616
C IF (KDD.GT.1) TPS3=AMAX1(TPS3,ABS(HH*D(1)))             SVDQ0617
C TPS3=TPS3*p1                                           SVDQ0618
C 350 DT(2,I)=D(2)                                         SVDQ0620
C D(2)=D(1)-DT(5,I)                                       SVDQ0621
C TPS2=-D(2)                                              SVDQ0622
C TPS3=TPS5*ABS(TPS2)                                     SVDQ0623
C FIRST STEP THAT KQ(I)=1                                 SVDQ0624
C 360 DT(7,I)=PT(4)                                         SVDQ0625
C IF (LSTC-2) 420,380,380                                  SVDQ0626
C 370 IF (TPS5.EQ.0.) GO TO 360                            SVDQ0627
C IF (DT(6,I).EQ.0.) GO TO 400                            SVDQ0628
C TPS2=DT(5,I)-DT(1,I)                                     SVDQ0629
C 380 TPS4=DT(4,I)                                         SVDQ0630
C TPS1=ABS(TPS4)                                         SVDQ0631
C TPS4=TPS2*SIGN(PT52,TPS4)-TPS5*TPS1                   SVDQ0632
C IF (TPS4.GT.(-TPS1)) GO TO 410                         SVDQ0633
C 390 TPS6=-PT51                                         SVDQ0634
C GO TO 450                                              SVDQ0635
C FIRST STEP AFTER THE STEPSIZE HAS BEEN CHANGED          SVDQ0636
400 DT(6,I)=PT(1)                                         SVDQ0637

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TPS6=0.
GO TO 450
410 IF (TPS4.LT.TPS1) GO TO 440
IF (TPS1.EQ.0.) GO TO 390
420 TPS6=PTS1
GO TO 450
430 KQ(I)=2
IF (2-LSTC) 510,510,520
440 TPS6=TPS4/TPS1
450 TPS4=TPS5+TPS6
IF (TPS4.LT.P25) GO TO 430
C INCREASE E2H IF (-S).GT..25
E2H=PTS4*TPS4
IF (2-LSTC) 460,470,480
460 LSC=0
GO TO 510
470 IF (TPS5-P25) 430,460,460
480 IF (TPS4.GT.PTS2) GO TO 490
IF (TPS4.GT.P5) D(2)=D(2)*GAM(2,1)
GO TO 510
490 IF (TPS4.LT.PTS4) GO TO 500
TPS4=PTS4
D(2)=D(2)/PT(3)
C THE ESTIMATE OF E (AND HENCE OF E2H) IS INCREASED IF (-S).GE.8.
TPS3=TPS3*DT(7,I)
GO TO 510
500 D(2)=D(2)*PTS2*(TPS4-PTS1)/(TPS4*TPS4)
IF (TPS4.GE.P3E1) E2H=E2H*DT(7,I)
C STORE D(1)=PREDICTED DERIVATIVE AND D(2)=2*(CORRECTED Y -
C PREDICTED Y)/H D(1) AND D(2) ARE USED TO COMPUTE (-S) ON
C THE NEXT STEP.
510 DT(5,I)=D(1)
DT(4,I)=D(2)
D(4)=TPS4
C STORE D(4)= CURRENT ESTIMATE OF (-S). (-S).CT.3 IS AN INDICATION SVDQ0672
C THAT THE STEPSIZE SHOULD BE LIMITED BECAUSE OF STABILITY PROBLEMS. SVDQ0673
C S=H*(ESTIMATE OF EIGENVALUE OF F)=H*(DIFFERENCE BETWEEN PREDICTED SVDQ0674
C AND CORRECTED DERIVATIVE VALUES)/(DIFFERENCE BETWEEN PREDICTED SVDQ0675
C AND CORRECTED INTEGRALS OF THE DERIVATIVE VALUES) SVDQ0676
C THE TREATMENT OF THE CASE KQ(I)=1 COULD BE IMPROVED BY USING A SVDQ0677
C SPECIAL METHOD FOR STIFF EQUATIONS WHEN (-S).GT.3 (MAYBE). SVDQ0678
C (THE ENTIRE TREATMENT OF THE CASE KQ(I)=1 IS FAR FROM IDEAL.) SVDQ0679
DT(3,I)=D(4)
C
C CORRECT
520 KDC=0
TPD=D(KQ1)
J=J+KDD
K=J
530 TPD=HH*TPD
KDC=KDC+1
Y(K)=Y(K)+GAM(KQQ+1,KDC)*TPD
K=K-1
IF (KDC.LT.KDD) GO TO 530
C END OF CORRECT
C
IF (EPS) 540,550,560
540 EPS=EP(I)
IF (EPS.NE.0.) GO TO 560

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550 IF (HMAXA) 1190,780,1190 SVDQ0697
560 TPS4=ABS(D(KQQ+2)) SVDQ0698
      TPS2=ABS(D(KQQ)) SVDQ0699
      TPS6=HH/EPS SVDQ0700
C           E=ABS(GAS(KQQ+1)*TPS3*TPS6) SVDQ0701
C   E GIVES ABS((ESTIMATED ERROR)/EPS) SVDQ0702
C           LRND=1 SVDQ0703
C           LRND= 1 MEANS NO ROUND-OFF ERROR SVDQ0704
C           = 0 MEANS SOME ROUND-OFF ERROR SVDQ0705
C           =-1 MEANS EXTREME ROUND-OFF ERROR SVDQ0706
C           FRND=PT(KQQ+2)*RNDC*ABS(D(1)) SVDQ0707
C   CHECK TO SEE IF ROUND OFF ERROR IS DOMINANT SVDQ0708
C   IF ((TPS3+TPS4).GT.FRND) GO TO 570 SVDQ0709
C   LRND=0 SVDQ0710
C   IF ((TPS4*TPS2).LT.FRND) LRND=-1 SVDQ0711
C
570 IF (E.LE.ERND) GO TO 590 SVDQ0712
      IF (E.LE.EMAX) GO TO 580 SVDQ0713
      EMAX=E SVDQ0714
      KEMAX=I SVDQ0715
580 IF (LRND.LE.0) GO TO 590 SVDQ0716
      ERND=E SVDQ0717
      IF (ERND.GT.ERRMX) LDOUB=0 SVDQ0718
590 IF (LDOUB.LE.0) GO TO 780 SVDQ0719
      TPS1=ABS(DD(KQQ)) SVDQ0720
      TPS5=TPS1 SVDQ0721
      IF (KQQ-2) 600,610,620 SVDQ0722
600 E2H=E*E2H SVDQ0723
      IF (E2H.LT.P01) GO TO 780 SVDQ0724
      IF (D(4).LT.P3E1) GO TO 770 SVDQ0725
      LSTC=-1 SVDQ0726
      LSC=-5 SVDQ0727
      GO TO 770 SVDQ0728
610 TPS1=TPS2 SVDQ0729
      IF (LSTC.NE.-2) GO TO 620 SVDQ0730
      KQ(1)=3 SVDQ0731
      TPS2=0. SVDQ0732
      TPS4=0. SVDQ0733
      LRND=0 SVDQ0734
620 E2H=TPS2+TPS3+TPS4 SVDQ0735
      E2H=ABS(GAS(KQQ-1)*PT(KQQ+1)*E2H*TPS6) SVDQ0736
C   E2H IS USED AS AN ESTIMATE OF WHAT THE VALUE OF E WOULD BE SVDQ0737
C   IF H WERE DOUBLED. THE ESTIMATE IS CONSERVATIVELY LARGE. SVDQ0738
      IF (E2H.GT.E2HMAX) E2HMAX=E2H SVDQ0739
C
      IF (LRND) 630,640,660 SVDQ0740
C   EXTREME ROUND-OFF ERROR--REDUCE E2H SVDQ0741
630 K=(KBIT2/KQQ)-4 SVDQ0742
      IF (K.LE.3) GO TO 640 SVDQ0743
      IF (K.GT.KQMAX) K=KQMAX SVDQ0744
      E2H=E2H/PT(K+1) SVDQ0745
      GO TO 650 SVDQ0746
640 E2H=AMINI(E2H,E2H*P3E1*E2HFAC) SVDQ0747
650 E2H=E2H*P1 SVDQ0748
      TPS6=PT54 SVDQ0749

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GO TO 670                                         SVDQ0756
C
660 E2H=E2H*E2HFAC                               SVDQ0757
      TPS6=FLOAT(KQQ+2)                           SVDQ0758
C     TEST TO SEE IF DIFFERENCES DECREASE MORE RAPIDLY THAN NECESSARY SVDQ0759
C
670 IF (TPS5.LT.(TPS3*TPS6)) GO TO 680          SVDQ0760
      IF (TPS2.LE.(TPS4*TPS6)) GO TO 760          SVDQ0761
C     THEY DO INCREASE KQ(I)                      SVDQ0762
      IF (KQQ.NE.KQMAX) KQ(I)=KQ1                 SVDQ0763
      GO TO 760                                    SVDQ0764
C
C     TEST TO SEE IF DIFFERENCES DECREASE TOO SLOWLY SVDQ0765
680 TPS6=TPS6*P25                                 SVDQ0766
      IF ((TPS1.GT.(TPS3*TPS6)).OR.(TPS2.GT.(TPS4*TPS6))) GO TO 760 SVDQ0767
C     THEY DO                                     SVDQ0768
      IF (LSTC.LE.0) GO TO 750                     SVDQ0769
      IF (E2H.LT.P01) GO TO 750                     SVDQ0770
      IF (LSC-LSTC) 690,750,770                   SVDQ0771
690 IF (KSTEP-4) 750,700,710                   SVDQ0772
700 KQ1=LSTC                                    SVDQ0773
710 LSC=KQ1                                     SVDQ0774
C     END OF ONE DERIVATIVE EVALUATION PER STEP SVDQ0775
      GO TO 770                                    SVDQ0776
C
C     AFTER HALVING H. REDUCE KQ(I) IF A DISCONTINUITY HAS OCCURRED. SVDQ0777
720 IF (LDOUR.EQ.(-2)) GO TO 340               SVDQ0778
      DT(KQQ+1,I)=D(KQQ+1)                         SVDQ0779
      IF (LDOUB.EQ.(-1)) DT(KQQ+1,I)=D(KQQ+2)       SVDQ0780
      K=KQQ
730 IF (K.EQ.1) GO TO 740                      SVDQ0781
      IF ((ABS(D(K-1)).GT.(PT(2)*ABS(D(K+1))))).OR. SVDQ0782
      I (ABS(D(K)).GT.(PT(2)*ABS(D(K+2)))) ) GO TO 740 SVDQ0783
      K=K-1
      GO TO 730                                    SVDQ0784
740 IF ((K+K).GE.KQQ) GO TO 780               SVDQ0785
      LDOUB=-4
      E2H=0.
      KQQ=K+1
C
C     DIFFERENCES DECREASE TOO SLOWLY REDUCE KQ(I). SVDQ0786
750 KQ(I)=KQQ-1                                SVDQ0787
      IF (KQQ.EQ.2) DT(3,I)=0.                      SVDQ0788
760 IF (E2H.LT.P01) GO TO 780                  SVDQ0789
770 LDOUB=2                                     SVDQ0790
780 CONTINUE                                    SVDQ0791
C
C     IF THE OUTPUT OPTION IS ELIMINATED, REMOVE THE 6 FOLLOWING CARDS. SVDQ0792
      IF (NEQ.GT.0) GO TO 790
      IO2=MAXU(1,(KQQ-1))
      IO3=IO2+3
      WRITE (6,5021) I,KQQ,LRND,LDOUB,E,E2H,EPS,
      1 (IO1,D(IO1),IO1=IO2,IO3)
5021 FORMAT (1H I2,I4,2I5,1PE13.3,2E11.3,4(3H (,I2,1H),E10.3)) SVDQ0793
C
    790 CONTINUE                                    SVDQ0794
C
C     END OF LOOP FOR CORRECTING, ESTIMATING THE ERROR, ETC. SVDQ0795

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C
C      IF THE INTERPOLATION CAPABILITY IS ELIMINATED REMOVE THE
C      FOLLOWING CARD.
C      IF (IFL.LT.0) GO TO 1250
C      TEST FOR HALVING H
C      IF (LDOUB) 800,950,870
800 LDOUB=LDOUB+1
C      IF (LDOUB+1) 810,870,820
810 IF (LDOUB.EQ.(-2)) GO TO 820
C      ORDER IN AT LEAST ONE COMPONENT HAS BEEN GREATLY REDUCED
C      LDOUB=0
C      GO TO 220
820 DO 860 I=1,NE
      KQQ=KG(1)
      TP=DT(KQQ+1,I)
      IF (KQQ.LE.3) GO TO 860
      IF (LDOUB.NE.0) GO TO 840
      DO 830 K=3,KQQ
C      SECOND MODIFICATION OF DIFFERENCE TABLE AFTER HALVING H
830 DT(K,I)=DT(K,I)+ETA(KQQ-1,K-2)*TP
      GO TO 860
840 DO 850 K=2,KQQ
C      FIRST MODIFICATION OF DIFFERENCE TABLE AFTER HALVING H
850 DT(K,I)=DT(K,I)+ETA(K-1,KQQ-1)*TP
860 CONTINUE
      IFL=0
      GO TO 240
C
870 IFL=2
      IF (LSTC.LE.0) GO TO 300
      IF (2-LSTC) 880,900,940
880 LSTC=LSTC-1
      IF (LSTC.EQ.3) GO TO 890
      IF (LSC) 920,960,920
890 IFL=1
      GO TO 300
900 IF (LSC-2) 910,930,920
910 LSTC=0
920 LDOUB=2
      GO TO 60
930 LSTC=1
      LSC=0
      GO TO 60
940 IF (LSC) 300,60,300

C      HALVE H
950 HH=FAC(2)*HH
      IF (LSTC.LT.2) GO TO 990
      ERND=P25*ERND
C      IN LOOP TO FIND A NEW INITIAL STEPSIZE
      IF (ERND.GE.P1) GO TO 950
      EMAX = ERND
      LSTC=4
960 LSC=4
      DO 970 I=1,NE
970 KQ(I)=I
      IF (LSTC-3) 890,890,1170
C

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C ENTRY AFTER IFLAG=7
980 IF (LDOUB.EQ.0) GO TO 990 SVDQ0873
    LSC=1 SVDQ0874
    LSTC=1 SVDQ0875
    GO TO 140 SVDQ0876
C TEST TO SEE IF H IS TOO SMALL FOR HALVING SVDQ0877
990 IF (ABS(HH).GE.HMINA) GO TO 1040 SVDQ0878
    IF (IFL.EQ.7) GO TO 1010 SVDQ0879
1000 IFL=7 SVDQ0880
    GO TO 1020 SVDQ0881
C SVDQ0882
1010 HH=HH+HH SVDQ0883
    IFL=2 SVDQ0884
1020 H=HH SVDQ0885
    GO TO 310 SVDQ0886
C SVDQ0887
C SVDQ0888
C ERROR CRITERIA PERMIT DOUBLING SVDQ0889
1030 HH=HH+HH SVDQ0890
    IF (LSTC.EQ.1) GO TO 1050 SVDQ0891
    LSC=-3 SVDQ0892
1040 LSTC=-1 SVDQ0893
C SVDQ0894
C CHANGE THE STEPSIZE SVDQ0895
1050 DO 1160 I=1,NE SVDQ0896
    KQQ=KQ(I)
    IF (KQQ.NE.1) GO TO 1070 SVDQ0897
    DT(6,I)=0. SVDQ0898
    D(3)=DT(3,I)*PT(2) SVDQ0899
    IF (D(3).GT.PT(3)) LSC=-6 SVDQ0900
    IF (LDOUB.NE.0) GO TO 1060 SVDQ0901
    KQM=8 SVDQ0902
    IF (D(3).GE.PT(5)) DT(7,I)=DT(7,I)*PT(2) SVDQ0903
    D(3)=D(3)/PT(3) SVDQ0904
1060 DT(3,I)=D(3) SVDQ0905
    GO TO 1160 SVDQ0906
C SVDQ0907
C BEGINNING OF LOOP FOR CHANGING DIFFERENCE TABLE TO SVDQ0908
C CORRESPOND TO NEW VALUE OF H SVDQ0909
1070 DO 1080 K=1,KQQ SVDQ0910
    D(K)=DT(K,I)/PT(K) SVDQ0911
1080 IF (LDOUB.EQ.0) D(K)=D(K)/PT(K) SVDQ0912
    KQQ2=KQQ-2 SVDQ0913
    IF (KQQ2) 1160,1140,1090 SVDQ0914
1090 DO 1130 J=1,KQQ2 SVDQ0915
    IF (LDOUB.NE.0) GO TO 1110 SVDQ0916
C SVDQ0917
C HALVE SVDQ0918
    K=KQQ SVDQ0919
1100 D(K-1)=D(K-1)+D(K) SVDQ0920
    K=K-1 SVDQ0921
    IF (K+J-KQQ) 1130,1130,1100 SVDQ0922
C SVDQ0923
C DOUBLE SVDQ0924
1110 DO 1120 K=J,KQQ2 SVDQ0925
1120 D(K+1)=D(K+1)-D(K+2) SVDQ0926
1130 CONTINUE SVDQ0927
C SVDQ0928
1140 DO 1150 K=2,KQQ SVDQ0929

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IF (LDOUB.NE.0) D(K)=D(K)*PT(K) SVDQ0932
DT(K,I)=D(K)*PT(K) SVDQ0933
1150 CONTINUE SVDQ0934
C DIFFERENCE TABLE NOW CORRESPONDS TO NEW VALUE OF H SVDQ0935
C SVDQ0936
1160 CONTINUE SVDQ0937
1170 H=HH SVDQ0938
IF (LDOUB.NE.0) GO TO 50 SVDQ0939
LFD=1 SVDQ0940
IF (LSTC.GE.0) GO TO 220 SVDQ0941
LDOUB=-3 SVDQ0942
LSC=LSTC-KQM SVDQ0943
GO TO 220 SVDQ0944
C END OF CHANGING STEPSIZE SVDQ0945
C SVDQ0946
C SVDQ0947
C IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE C IN COLUMN ONE SVDQ0948
C OF THE 2 FOLLOWING CARDS SVDQ0949
C1180 IF (7-IFL) 1181,980,220 SVDQ0950
C1181 IF (IFL-8) 60,1200,60 SVDQ0951
C AND THEN REMOVE THE 2 FOLLOWING CARDS. SVDQ0952
1180 K=IFL-5 SVDQ0953
GO TO (220,980,1200,1570,1570,1720,1720,60,1480,1450,1630+1570), K$VDQ0954
C SVDQ0955
C ILLEGAL VALUE OF PARAMETER INTEGRATION CAN NOT PROCEED SVDQ0956
1190 IFL=8 SVDQ0957
GO TO 310 SVDQ0958
1200 WRITE (6,4000) SVDQ0959
4000 FORMAT (26HOIFLAG=8 IN CALL TO DVDDQ1.)
STOP SVDQ0961
C SVDQ0962
C SVDQ0963
1210 IF (T-TFINAL) 200,1190,200 SVDQ0964
C SVDQ0965
C IF ONE DOES NOT WANT THE INTERPOLATION FEATURE, REMOVE ALL CARDS SVDQ0966
C BELOW THIS POINT (EXCEPT FOR THE END STATEMENT), AND ADD THE SVDQ0967
C FIVE FOLLOWING STATEMENTS. SVDQ0968
C1220 IFL=4 SVDQ0969
C IF (TPD1.GT.TPD) GO TO 1280 SVDQ0970
C GO TO 310 SVDQ0971
C1280 IFL=3 SVDQ0972
C GO TO 310 SVDQ0973
C SVDQ0974
1220 IFL=4 SVDQ0975
IF (KSTEP.NE.0) GO TO 1270 SVDQ0976
TPD2=TPD SVDQ0977
C ESTIMATE ERROR WHEN EXTRAPOLATION FROM INITIAL POINT IS REQUESTED SVDQ0978
1230 HH=HH*TPD1*.75E0 SVDQ0979
C SVDQ0980
C IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE FOLLOWING CARD. SVDQ0981
IFLS=IFL SVDQ0982
IFL=-1 SVDQ0983
GO TO 230 SVDQ0984
C SVDQ0985
C IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE 4 FOLLOWING CARDS. SVDQ0986
1240 IF ((LGSD.EQ.0).OR.(IFLS.NE.4)) GO TO 20 SVDQ0987
LGSE=-1 SVDQ0988
TPD=FAC(1) SVDQ0989
GO TO 1820 SVDQ0990

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1250 HH=H SVDQ0991
    IF (EMAX.LT.P01) GO TO 1260 SVDQ0992
C     ERROR IS TOO LARGE, REDUCE H AND REPEAT THE FIRST STEP SVDQ0993
    IF (TPD1.LT.0.E0) GO TO 1190 SVDQ0994
    LDOUB=1
    ERND=FAC(1)/TPD1
    ERND=ERND*ERND*P25
C     SET IFLAG SO INTERPOLATION IS DONE SVDQ0998
    IFLAG = 3 SVDQ0999
    GO TO 950
C
C     IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE C IN COLUMN ONE SVDQ1000
C     OF THE FOLLOWING CARD SVDQ1001
C1260 IFL=4 SVDQ1002
C     AND THEN REMOVE THE 2 FOLLOWING CARDS. SVDQ1003
1260 IFL=IFLS SVDQ1004
    IF (IFL.NE.4) GO TO 1790 SVDQ1005
    TPD=TPD2 SVDQ1006
    IFLAG=3 SVDQ1007
1270 IF (TPD1.GT.TPD1) GO TO 1280 SVDQ1008
    T=TFINAL SVDQ1009
    TPD=TPD1 SVDQ1010
    GO TO 1290 SVDQ1011
1280 T=TOUT SVDQ1012
    IFL=3 SVDQ1013
1290 IF ((TPD.EQ.C.E0).AND.(IFLAG.LE.2)) GO TO 310 SVDQ1014
C
C     INTERPOLATE FOR OUTPUT SVDQ1015
1300 TP=TPD SVDQ1016
    D(2)=TP SVDQ1017
    KQQ2=0 SVDQ1018
    KDC=0 SVDQ1019
    D(1)=PT(1) SVDQ1020
    DD(1)=PT(1) SVDQ1021
    DO 1310 K=2,KQM SVDQ1022
    DD(1)=DD(1)+PT(1) SVDQ1023
    TP=TP+PT(1) SVDQ1024
1310 D(K+1)=(D(K)*TP)/DD(1) SVDQ1025
    GO TO 1350 SVDQ1026
C
C     COMPUTE THE INTERPOLATING INTEGRATION COEFFICIENTS SVDQ1027
1320 KQQ2=1 SVDQ1028
    L=KQM-KDC SVDQ1029
    KDC=KDC+1 SVDQ1030
1330 IF (L.LE.0) GO TO 1350 SVDQ1031
    TP=0. SVDQ1032
    K=L SVDQ1033
    J=L+KDC SVDQ1034
1340 JS=J-K SVDQ1035
    TP=TP+GAS(K)*D(JS+1) SVDQ1036
    K=K-1 SVDQ1037
    IF (K.GT.0) GO TO 1340 SVDQ1038
    D(J)=TP SVDQ1039
C
C     D(J) IS THE INTEGRATION COEFFICIENT FOR THE INTERPOLATION WHICH SVDQ1040
C     CORRESPONDS TO GAM(J-KDC,KDC). SVDQ1041
C
    L=L-1 SVDQ1042
    GO TO 1330 SVDQ1043

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C END OF COMPUTING INTEGRATION COEFFICIENTS           SVDDQ1048
C PERFORM THE PARTIAL STEP INTEGRATION               SVDDQ1049
1350 J=0                                              SVDDQ1050
DO 1420 I=1,NE                                         SVDDQ1051
IF (KDS.LE.0) KDD=IABS(KD(I))                         SVDDQ1052
IF (KDC.GT.KDD) GO TO 1410                           SVDDQ1053
TP=0.                                                 SVDDQ1054
KQQ=KQ(I)+KQQ2                                       SVDDQ1055
1360 L=KQQ-KDC                                         SVDDQ1056
IF (L.LE.0) GO TO 1370                               SVDDQ1057
TP=TP+D(KQQ)*DT(L,I)                                SVDDQ1058
KQQ=KQQ-1                                            SVDDQ1059
IF (KQQ) 1390,1390,1360                            SVDDQ1060
1370 K=J+KDD                                         SVDDQ1061
L=KDC                                                SVDDQ1062
1380 L=L-1                                           SVDDQ1063
IF (L.EQ.0) GO TO 1400                               SVDDQ1064
TP=TP*HH+YN(K)*FAC(L)*TPD**L                         SVDDQ1065
K=K-1                                                 SVDDQ1066
GO TO 1380                                         SVDDQ1067
1390 F(I)=TP                                         SVDDQ1068
GO TO 1420                                         SVDDQ1069
1400 Y(K)=YN(K)+HH*TP                               SVDDQ1070
1410 J=J+KDD                                         SVDDQ1071
1420 CONTINUE                                         SVDDQ1072
IF (KDC.NE.KDMAX) GO TO 1320                         SVDDQ1073
C END OF PARTIAL STEP INTEGRATION                   SVDDQ1074
C IF THE GSTOP FEATURE IS ELIMINATED, REMOVE THE C IN COLUMN ONE
C OF THE FOLLOWING CARD                             SVDDQ1075
C GO TO 310                                         SVDDQ1076
C ALL STATEMENTS BELOW THIS POINT SHOULD THEN BE REMOVED (EXCEPT
C FOR THE END STATEMENT)                          SVDDQ1077
C IF (LGSE) 1800,310,1810                         SVDDQ1078
C
C SECTION FOR COMPUTING GSTOPS                     SVDDQ1079
C
C ENTRY SVDQG(NG,NSTOP,G,GT)                      SVDDQ1080
C
C VARIABLES IN THE CALLING SEQUENCE HAVE THE FOLLOWING TYPES.   SVDDQ1081
C INTEGER NG,NSTOP                                     SVDDQ1082
C REAL G(1),GT(1)                                    SVDDQ1083
C
C A GSTOP IS DEFINED AS A RETURN WHICH IS MADE TO THE USER WHEN A   SVDDQ1084
C USER SPECIFIED FUNCTION G PASSES THROUGH ZERO. THE USER MAY      SVDDQ1085
C SPECIFY ANY NUMBER OF FUNCTIONS G OF TWO TYPES. ZEROS OF THE FIRST  SVDDQ1086
C TYPE ARE LOCATED WITHOUT REQUIRING A DERIVATIVE EVALUATION       SVDDQ1087
C BEYOND THE ZERO. THIS TYPE OF GSTOP REQUIRES THAT G BE EVALUATED  SVDDQ1088
C BEFORE EACH DERIVATIVE EVALUATION. ZEROS OF THE SECOND TYPE ARE  SVDDQ1089
C LOCATED USING INTERPOLATION, WHICH IS MORE ACCURATE THAN THE     SVDDQ1090
C EXTRAPOLATION USED IN THE PRECEDING CASE AND ONLY REQUIRES ONE  SVDDQ1091
C EVALUATION OF G PER STEP. THUS ONE SHOULD USE THE SECOND TYPE OF  SVDDQ1092
C GSTOP IF POSSIBLE. USERS NOT USING THE GSTOP FEATURE NEED READ    SVDDQ1093
C NO FURTHER.                                         SVDDQ1094
C
C SVDQG IS USED AS A SET UP CALL TO INDICATE A CHANGE IN THE NUMBER  SVDDQ1095
C OR TYPES OF GSTOPS. SVDQG SHOULD BE CALLED JUST BEFORE OR JUST    SVDDQ1096

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C AFTER CALLING SVDQ IF SVDQ1107  
 C 1. ONE WANTS TO TEST FOR GSTOPS BEGINNING WITH THE FIRST STEP. SVDQ1108  
 C 2. A JOB IS BEING RUN AFTER ANOTHER JOB THAT USES THE GSTOP SVDQ1109  
 C FEATURE. SVDQG MUST BE CALLED EVEN IF ALL THE VARIABLES IN SVDQ1110  
 C THE NEW JOB ARE THE SAME. SVDQ1111  
 C IN ADDITION SVDQG MAY BE CALLED AT ANY TIME IN THE INTEGRATION SVDQ1112  
 C TO CHANGE THE NUMBER OR TYPE OF GSTOPS. SVDQ1113  
 C SVDQ1114  
 C THE USAGE OF THE VARIABLES IS GIVEN BELOW. SVDQ1115  
 C NG= THE NUMBER OF COMPONENTS IN G TO BE EXAMINED FOR A ZERO. SVDQ1116  
 C IF SVDQG IS CALLED AFTER THE FIRST STEP OF THE INTEGRATION, SVDQ1117  
 C THEN G IS EVALUATED FOR THE FIRST TIME AT THE END OF THE SVDQ1118  
 C NEXT STEP AND THUS A GSTOP IS NOT DETECTED IF G CHANGES SVDQ1119  
 C SIGN ON THE CURRENT STEP. IF IT IS IMPORTANT THAT G BE SVDQ1120  
 C EVALUATED IMMEDIATELY SET NG EQUAL TO THE NEGATIVE OF THE SVDQ1121  
 C NUMBER OF COMPONENTS TO BE TESTED FOR A ZERO. SETTING NG SVDQ1122  
 C LESS THAN ZERO WHEN CALLING SVDQG BEFORE THE FIRST STEP IS SVDQ1123  
 C NOT NECESSARY AND IS LIABLE TO BE DISASTEROUS. IF SVDQG IS SVDQ1124  
 C CALLED DURING THE INTEGRATION THE FOLLOWING STATEMENT SHOULD SVDQ1125  
 C BE A GO TO (THE COMPUTED GO TO FOLLOWING THE CALL TO SVDQ1). SVDQ1126  
 C SVDQ1127  
 C NSTOP=THE NUMBER OF COMPONENTS OF G THAT MUST BE EXAMINED FOR SVDQ1128  
 C A ZERO BEFORE COMPUTING THE DERIVATIVES (FIRST TYPE OF SVDQ1129  
 C GSTOP). IF NSTOP.LT.0 OR NSTOP.GT.ABS(NG) IFLAG IS SET SVDQ1130  
 C EQUAL 8 AND AN IMMEDIATE RETURN IS MADE. IF NSTOP.GT.0, SVDQ1131  
 C G(1),G(2),...,G(NSTOP) ARE EXAMINED FOR A ZERO BEFORE EACH SVDQ1132  
 C DERIVATIVE EVALUATION, THE REMAINING COMPONENTS (IF ANY) SVDQ1133  
 C ARE EXAMINED AT THE END OF EACH STEP. WHEN A GSTOP IS FOUND SVDQ1134  
 C THE SUBROUTINE SETS NSTOP EQUAL TO THE INDEX OF THE SVDQ1135  
 C COMPONENT OF G RESPONSIBLE FOR THE STOP. SVDQ1136  
 C SVDQ1137  
 C G= A VECTOR CONTAINING THE CURRENT VALUES OF THE FUNCTIONS SVDQ1138  
 C WHOSE ZEROS ARE TO BE DETERMINED. SVDQ1139  
 C SVDQ1140  
 C GT= A VECTOR WITH THE SAME DIMENSION AS G USED BY THE SVDQ1141  
 C SUBROUTINE FOR TEMPORARY STORAGE. SVDQ1142  
 C SVDQ1143  
 C RETURNS FROM CALLING SVDQ1 WITH IFLAG.GT.8 SHOULD BE INTERPETED SVDQ1144  
 C AS FOLLOWS. (WE USE NSTOPI TO DENOTE THE INITIAL VALUE OF NSTOP.) SVDQ1145  
 C IFLAG SVDQ1146  
 C = 9 COMPUTE G(NSTOPI+1),...,G(ABS(NG)) (THE COMPONENTS OF G WITH SVDQ1147  
 C ZEROS TO BE LOCATED USING INTERPOLATION). THEN CALL SVDQ1. SVDQ1148  
 C NO RETURN IS MADE WITH IFLAG=9 IF NSTOPI=ABS(NG). SVDQ1149  
 C =10 COMPUTE G(1),G(2),...,G(NSTOPI) (THE COMPONENTS OF G WITH SVDQ1150  
 C ZEROS TO BE LOCATED USING EXTRAPOLATION). THEN CALL SVDQ1. SVDQ1151  
 C NO RETURN IS MADE WITH IFLAG=10 IF NSTOPI=0. SVDQ1152  
 C -11 G(NSTOP) IS APPROXIMATELY ZERO. IF THERE ARE NO SVDQ1153  
 C DISCONTINUITIES SIMPLY CALL SVDQ1 TO CONTINUE THE INTEGRATION. SVDQ1154  
 C =12 G(NSTOP) CHANGES SIGN, BUT THERE IS DIFFICULTY IN CONVERGING SVDQ1155  
 C TO A ZERO. THE USER MAY WISH TO MAKE A SPECIAL CHECK TO BE SVDQ1156  
 C CERTAIN THAT EVERYTHING IS ALL RIGHT. TO CONTINUE THE SVDQ1157  
 C INTEGRATION CALL SVDQ1. SVDQ1158  
 C SVDQ1159  
 C REAL RG  
 C DIMENSION GI(2),RG(3) SVDQ1160  
 C SVDQ1161  
 C C INITIALIZE FOR GSTOPS SVDQ1162  
 C NGA=IABS(NG) SVDQ1163  
 C LGSS=-NGA SVDQ1164  
 C SVDQ1165

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LGSD=0          SVDQ1166
LGSE=0          SVDQ1167
IFLG=-20        SVDQ1168
IF (NG.GE.0) RETURN SVDQ1169
IFLG=-IFL      SVDQ1170
1430 LGSD=NSTOP SVDQ1171
IF (LGSD) 1190,1450,1440 SVDQ1172
1440 IFL=15     SVDQ1173
GO TO 1470     SVDQ1174
C   ENTRY WITH IFL=15 SVDQ1175
1450 LGSS=0     SVDQ1176
IF (LGSD-NGA) 1460,1480,1190 SVDQ1177
1460 LGSS=LGSD+1 SVDQ1178
IFL=14         SVDQ1179
1470 IFLAG=IFL-5 SVDQ1180
GO TO 315      SVDQ1181
C   ENTRY WITH IFL=14 SVDQ1182
1480 DO 1490 I=1,NGA SVDQ1183
1490 GT(I)=G(I) SVDQ1184
GO TO 1730     SVDQ1185
C   END OF INITIALIZATION FOR GSTOPS SVDQ1186
C
C   ENTRY TO EVALUATE G AT THE END OF THE STEP SVDQ1187
1500 LGSE=1     SVDQ1188
1510 IGK=LGSS   SVDQ1189
IFLG=0          SVDQ1190
IFL=9           SVDQ1191
GO TO 310      SVDQ1192
C   ENTRY TO EVALUATE G BEFORE EVALUATING THE DERIVATIVES SVDQ1193
1520 IFLG=IFL   SVDQ1194
IFL=10          SVDQ1195
1530 IFLAG=10   SVDQ1196
IGKM=LGSD      SVDQ1197
1540 IGK=1       SVDQ1198
1550 GO TO 315  SVDQ1199
1560 IGK=IGK+1  SVDQ1200
IF (IGK.GT.IGKM) GO TO 1650 SVDQ1201
C   ENTRY WITH IFL=9,10, AND 17 SVDQ1202
C   TEST FOR G CHANGING SIGN SVDQ1203
1570 IF (G(IGK)*GT(IGK)) 1600,1580,1590 SVDQ1204
1580 IF (GT(IGK).NE.0.) GO TO 1600 SVDQ1205
IF (TL.EQ.TG) GO TO 1560 SVDQ1206
1590 IF (LGSE.GT.0) GT(IGK)=G(IGK) SVDQ1207
GO TO 1560     SVDQ1208
C   G CHANGES SIGN -- PREPARE FOR ITERATION TO FIND ZERO SVDQ1209
1600 NSTOP=IGK SVDQ1210
NSTOPI=IGK    SVDQ1211
IFLGS=IFL     SVDQ1212
C   COMPUTE INITIAL VALUE FOR RG (=RATIO OF PARTIAL STEPSIZE WHERE SVDQ1213
C   G IS KNOWN/THE INTEGRATION STEPSIZE) SVDQ1214
C   IF (IFLG.EQ.0) GO TO 1610 SVDQ1215
RG(3)=FAC(1)  SVDQ1216
RG(2)=0.E0     SVDQ1217
IF ((IFLG.EQ.2).AND.(IGK.LT.LGSS)) RG(2)=FAC(1) SVDQ1218
GO TO 1620     SVDQ1219
1610 RG(3)=0.E0 SVDQ1220
RC(2)=-FAC(1) SVDQ1221
1620 IF (LGSE.LT.0) RG(3)=TPD SVDQ1222
LGSE=-3        SVDQ1223

```

```

GI(2)=GT(IGK)
EPSGS=RND
IFL=16
K=1
GO TO 1640
C END OF PREPARATION TO BEGIN THE ITERATION
C
C ENTRY WITH IFL=16
C ITERATE TO FIND GSTOP
1630 K=1
IF ((GI(2)*G(IGK)).GT.0.) K=2
IF (ABS(GI(K)).GT.ABS(G(IGK))) GO TO 1640
C CONVERGENCE PROBLEMS
LGSE=LGSE-1
IF (LGSE.EQ.(-5)) EPSGS=PTS1
EPSGS=EPSGS*PTS4
1640 GI(K)=G(IGK)
RG(K)=RG(3)
C SECANT ITERATION (GIVES NEW PARTIAL STEPSIZE/H)
TPD=RG(1)-(GI(1)*(RG(2)-RG(1)))/(GI(2)-GI(1))
T=TL+TPD*HH
C TEST FOR CONVERGENCE OF ITERATION
IF (ABS(TPD-RG(3)).LE.EPSGS) GO TO 1560
RG(3)=TPD
GO TO 1300
1650 IF (10-IFL) 1660,1700,100
1660 IF (IGKM.NE.NGA) GO TO 1710
IF (LGSE.GT.(-3)) GO TO 1690
IF (LSTC.NE.4) GO TO 1670
C ESTIMATE ERROR -- GSTOP IS THE RESULT OF EXTRAPOLATING FROM
C THE INITIAL POINT
TPD1=TPD
RG(3)=TPD
GO TO 1230
1670 IFL=11
IF (LGSE.LT.(-4)) IFL=12
1680 IFLAG=IFL
C TEST TO SEE IF GSTOP IS PRECEDED BY ANOTHER STOP
IF (((T-TOUT)*HH.LE.0.E0).AND.((T-TFINAL)*HH.LE.0.E0)) GO TO 1300
C IT IS
RG(3)=TPD
IFLS=IFL
GO TO 200
1690 LOSE=1
IFL=IFLG
IF (IFL.LT.0) GO TO 20
1700 IGKM=NGA
IFL=IFLG
GO TO 310
1710 IFL=17
IFLAG=9
IGKM=NGA
GO TO 315
C ENTRY WITH IFL=11 AND 12
C SET PARAMETERS TO INDICATE A GSTOP HAS BEEN FOUND
1720 GT(INSTOP1)=0.
1730 LOSE=1
IGKM=NGA
TG=TL

```

1740	IF (IFLG) 1740,1760,1770	SVDQ1284
1740	IF (IFL.LT.131) GO TO 1750	SVDQ1285
	IF (IFLG.EQ.(-20)) GO TO 100	SVDQ1286
	IFL=-IFLG	SVDQ1287
	GO TO 310	SVDQ1288
1750	HH=H	SVDQ1289
	GO TO 200	SVDQ1290
1760	TPD=U.E0	SVDQ1291
	T=TL	SVDQ1292
	LGSE=-2	SVDQ1293
	GO TO 1300	SVDQ1294
1770	IF (IFLG-3) 220,200,200	SVDQ1295
1780	IF (LGSE.EQ.(-1)) GO TO 1790	SVDQ1296
	LGSE=-1	SVDQ1297
	GO TO 1220	SVDG1298
1790	TPD=R6(3)	SVDG1299
	T=TL+TPD*HH	SVDQ1300
	IF (LGSE.NE.(-1)) GO TO 1670	SVDQ1301
	IFL=IFLS	SVDG1302
	LGSE=-3	SVDQ1303
	GO TO 1680	SVDQ1304
1800	IF (LGSE+2) 1550,1500,310	SVDQ1305
1810	IF (TPD.LE.0.E0) GO TO 310	SVDQ1306
	LGSE=-2	SVDQ1307
1820	IFLG=IFL	SVDQ1308
	IFL=17	SVDQ1309
	IFLAG=9	SVDQ1310
	IF (LGSD) 1540,1540,1530	SVDQ1311
	END OF SECTION FOR COMPUTING GSTOPS	SVDQ1312
		SVDQ1313
		SVDQ1314

IN SOME APPLICATIONS, FOR EXAMPLE MULTIPLE QUADRATURE, MORE THAN ONE INTEGRATION SUBROUTINE IS REQUIRED. THIS IS NOT NECESSARY IF ALL OF THE VARIABLES ASSOCIATED WITH ONE INTEGRATION ARE SAVED OUTSIDE OF THE INTEGRATOR WHILE DOING OTHER INTEGRATIONS, AND THEN RESTORING THEM WHEN NEEDED. THESE VARIABLES CAN BE RESTORED BY CALLING AN ENTRY WHICH CONTAINS ALL OF THE VARIABLES IN THE CALLING SEQUENCE AND ALL OF THE VARIABLES THAT MUST BE SAVED WHENEVER CHANGING TO A DIFFERENT INTEGRATION. (THIS ENTRY MUST BE ADDED BY THE USER AND SHOULD BE FOLLOWED BY A RETURN STATEMENT.) AFTER CALLING THIS ENTRY EITHER SVDQ OR SVDQ1 SHOULD BE CALLED DEPENDING ON WHETHER THE INTEGRATION IS BEING STARTED OR NOT.) THE VARIABLES WHICH MUST BE SAVED ARE-

NE,NV,KDS,KDMAX,KSOUT,LDOUB,LFD,LSC,LSTC,IFL,IFLS,KQM	(INTEGERS)	SVDQ1327
ERND,QDEC,ERRMX,E2HAVE,E2HFAC,E2HMAX,RNDC	(REAL)	SVDQ1328
HH,TOUT,TL	(REAL)	SVDQ1329

IF THE GSTOP FEATURE IS USED, THE EVALUATION OF G REQUIRES AN INTEGRATION, AND THIS INTEGRATION MAY RESULT IN ANOTHER GSTOP. THEN SOME ADDITIONAL VARIABLES MUST BE SAVED.

IN MANY APPLICATIONS NE(=NEQ), NV(=SUM OF ORDERS OF THE DIFFERENTIAL EQUATIONS), KDS(=KD), AND KDMAX(=MAXIMUM ORDER OF ANY DIFFERENTIAL EQUATION) WILL BE THE SAME FOR EVERY INTEGRATION, AND HENCE NEED NOT BE SAVED.

INSTRUCTIONS FOR MAKING CERTAIN CHANGES IN THIS SUBROUTINE ARE GIVEN THROUGHOUT THE LISTING. TO FIND THESE INSTRUCTIONS, SEE BELOW.

TO ELIMINATE THE GSTOP CAPABILITY, SEE JUST BELOW CARDS SEQUENCED

SVDQ1330
SVDQ1331
SVDQ1332
SVDQ1333
SVDQ1334
SVDQ1335
SVDQ1336
SVDQ1337
SVDQ1338
SVDQ1339
SVDQ1340
SVDQ1341
SVDQ1342

C 303,449,491,537,947,980,985,999, AND 1076.  
C THIS MAKES THE SUBROUTINE SHORTER AND REDUCES OVERHEAD A LITTLE.  
C  
C TO REMOVE THE INTERPOLATION CAPABILITY, SEE JUST BELOW CARDS  
C SEQUENCED 816 AND 965.  
C THE GSTOP FEATURE MUST ALSO BE ELIMINATED SINCE IT REQUIRES THE  
C INTERPOLATION CAPABILITY. IF OUTPUT POINTS ARE NOT HIT EXACTLY  
C (THEY ARE HIT EXACTLY IF HMAXA.LE.ABS(DELT), AND INITIAL H=  
C DELT\*(2\*\*(-K)), K=0,1,2...), THEN IFLAG=3 ON THE FIRST STEP THAT  
C (T-TOUT)\*H.GT.0 (SEE THE USAGE OF DELT). IFLAG IS SET EQUAL TO 4  
C ON THE LAST STEP THAT (T-TFINAL)\*H.LE.0.  
C  
C THE OUTPUT OPTION GIVES OUTPUT OF VARIABLES USED IN THE  
C INTEGRATION ON EVERY STEP THAT NEQ.LE.0. (WHICH OF COURSE MUST  
C BE SET AFTER THE INITIAL CALL TO THE INTEGRATOR) TO ELIMINATE  
C THIS OPTION, SEE JUST BELOW CARDS SEQUENCED 580 AND 803.  
C  
C THE CHECK OPTION WHEN ADDED TO THE OUTPUT OPTION OUTPUTS EVERY  
C VARIABLE IN THE CALLING SEQUENCE JUST AFTER ENTERING AND JUST  
C BEFORE LEAVING THE INTEGRATOR WHEN NEQ=0. THIS OUTPUT IS  
C SOMETIMES USEFUL IN DEBUGGING A PROGRAM. TO INCLUDE THIS OPTION  
C SEE JUST BELOW CARDS SEQUENCED 359 AND 548.  
C  
C END

SVDQ1343  
SVDQ1344  
SVDQ1345  
SVDQ1346  
SVDQ1347  
SVDQ1348  
SVDQ1349  
SVDQ1350  
SVDQ1351  
SVDQ1352  
SVDQ1353  
SVDQ1354  
SVDQ1355  
SVDQ1356  
SVDQ1357  
SVDQ1358  
SVDQ1359  
SVDQ1360  
SVDQ1361  
SVDQ1362  
SVDQ1363  
SVDQ1364  
SVDQ1365  
SVDQ1366

#### A-5. DESCRIPTIONS OF PROGRAM LOGIC, SUBROUTINES AND USE OF TEXT EQUATIONS

A FORFL0 chart of the overall program is shown in Figure A-1. The purpose of each subroutine was indicated by comment cards in the listing presented in Appendix A-4. A brief summary indicating the usage of the text equations is presented as follows.

DATAIN loads input and calculates various constants (in the nature of input) which are used throughout the program. For example, DATAIN calculates thermal diffusivity and dimensionless frequency from constituent inputs. DATAIN also equalizes all thermal properties to represent a homogeneous solid if IHOMO=1.

Function TAU defines the dimensionless temperature.

SLDFAZ solves Eq. (12) for wall temperature. If burn rate is specified, ITERA = 0, only one pass is made to calculate the wall temperature associated with that rate. If ITERA = 1, burn rate and wall temperature are solved by iteration in association with subroutine GASFAZ. SLDFAZ also calculates certain constants that are associated with Eqs. (4), (5) and (22) and are needed to calculate the thermal profiles.

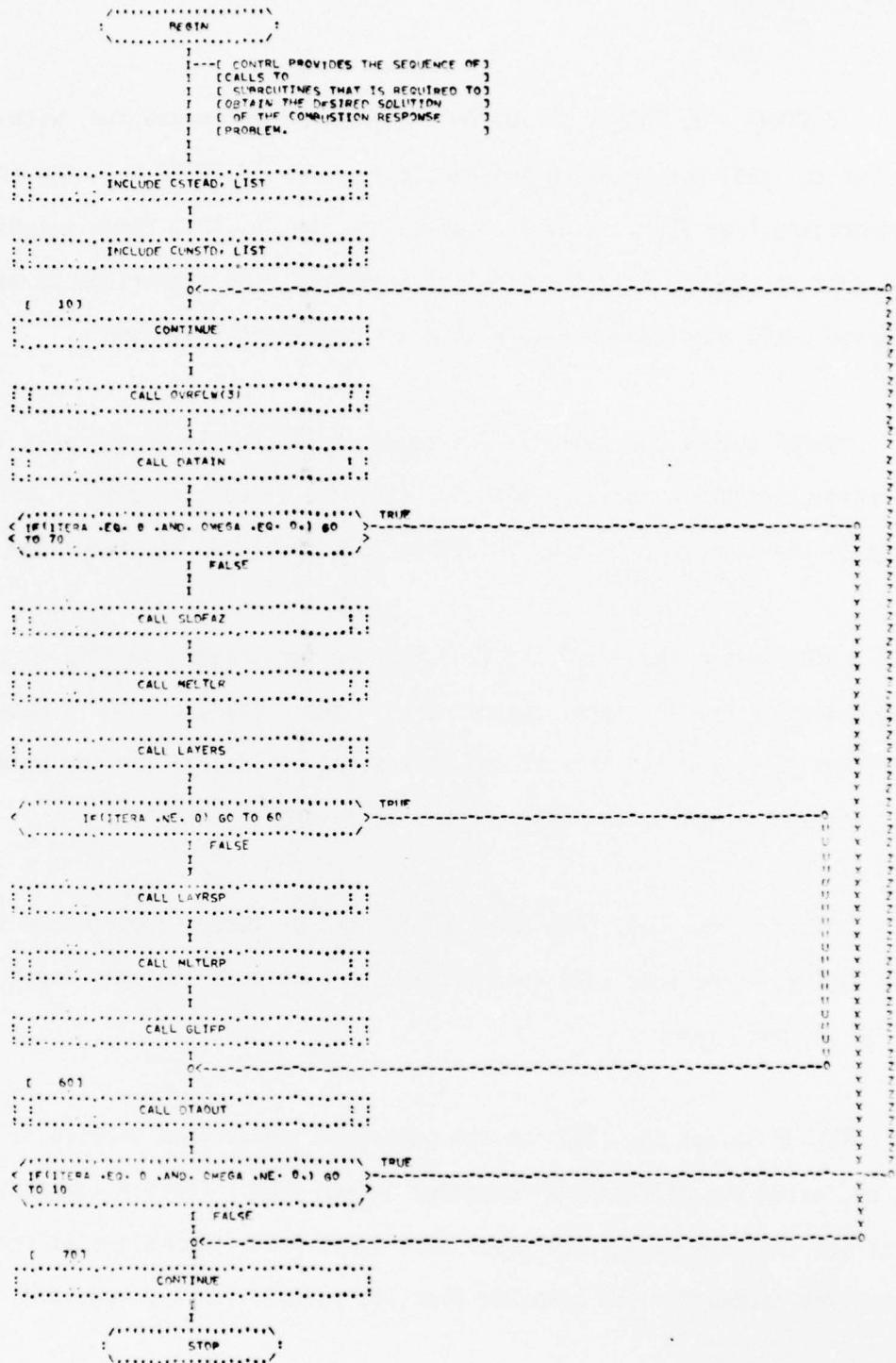


FIGURE A-1. FORFLO Chart of Overall Program

If ITERA = 0, GASFAZ solves Eq. (23) for flame height and, with AMULTI, solves Eq. (24) for an effective particle size. If ITERA = 1, the trial wall temperature from SLDFZ is used to calculate the Eq. (23) flame height. This is compared to the Eq. (24) flame height in AMULTI, and iterations on wall temperature proceed until the two agree to within a preassigned tolerance.

MELTLR solves Eq. (16) for the temperature profile in the melt layer. Certain constants associated with Eq. (16) are calculated also. Surface temperature is known, and melt layer thickness is determined from the known melting point.

LAYRS solves Eqs. (17) and (18) for the temperature profile in the succeeding layers in depth, beginning with the melting point. A satisfactory solution is tested in terms of the dimensionless temperature and gradient tending to zero at some adequate depth (number of layers traversed).

LAYRSP solves Eqs. (35) and (36) for the perturbed temperature profile in the layers, using Eqs. (34) and (38) to start at some adequate depth and working up to the melt layer.

MLTLRP solves Eq. (28) for the perturbed temperature profile in the melt layer, using the differential equation solver SVDQ. Certain constants associated with Eq. (28) are calculated also. The solid phase parameters at the mean surface which are needed for the response function calculation are provided.

GLIFP calculates the response function, Eq. (50), and the zero frequency limit, Eq. (53). Using Eqs. (29) - (31), the solid phase parameters at the mean surface are converted to values at the oscillating surface. Necessary gas phase parameters derived from Eq. (47) are calculated also.

DTAOUT prints the input and output.

Auxiliary JPL library routines which are used to solve the equations in the melt layer are subroutine PFIT, function SCPVAL and subroutine SVDQ. These were included in the listing to provide a self-contained program. PFIT and SCPVAL are called by MELTLR (steady-state solution); SVDQ and SCPVAL are called by MLTLRP (perturbed, complex solution). PFIT is a polynominal least squares curve fitting routine and SCPVAL evaluates the polynominal at a specified argument. Subroutines BHSLR, AHLR and SL2NRM are orthogonal transformation subroutines which are called by PFIT to solve the least squares problem. SVDQ computes the numerical solution of the ordinary differential equation describing the perturbed melt layer.

A-6. SOLUTIONS TO SAMPLE PROBLEM

COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

NDEG= 6 SIGFAC= .0000  
P(1),...,P(NDEG+3)= .19436020 .19436020 .84546567  
- .17224529 -.01451589 .00289440  
-.00031804 -.00000467 .00000915

TOLERANCE TESTS FOR A SATISFACTORY STEADY-STATE SOLUTION HAVE BEEN MET.

A SATISFACTORY STEADY-STATE SOLUTION HAS BEEN OBTAINED.

## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

YABRV	TAPR	DTAPR	D2TAPR
IFLAG= 3 H= -388720-02			
*388720+00	-479468-16	.446635-16	.699864-16
IFLAG= 3 H= -388720-02			
*399848+00	-496136-16	.408895-16	.119785-15
IFLAG= 3 H= -388720-02			
*310976+00	-510967-16	.349742-16	.188050-15
IFLAG= 3 H= -388720-02			
*272104+00	-522927-16	.259677-16	.279606-15
IFLAG= 3 H= -388720-02			
*233232+00	-530627-16	.128803-16	.398577-15
IFLAG= 3 H= -388720-02			
*194360+00	-532257-16	-539890-17	.546672-15
IFLAG= 3 H= -388720-02			
*155488+00	-525615-16	-299537-16	.720195-15
IFLAG= 3 H= -388720-02			
*116616+00	-508064-16	-615565-16	.906141-15
IFLAG= 3 H= -388720-02			
*777441-01	-476837-16	-100234-15	.107872-14
IFLAG= 3 H= -388720-02			
*388721-01	-429374-16	-144748-15	.119919-14
IFLAG= 3 H= -388720-02			
*144355-07	-363915-16	-192204-15	.122273-14
IFLAG= 4 H= -388720-02			
*000000	-363915-16	-192204-15	.122273-14

YABRV	TAPI	DTAPI	D2TAPI
-------	------	-------	--------

## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

IFLAG= 3 H= -.388720-02  
 .388720+00 -.291908-16 .723704-16 -.256974-17  
 IFLAG= 3 H= -.388720-02  
 .349843+00 -.319983-16 .718517-16 .317756-16  
 IFLAG= 3 H= -.388720-02  
 .310975+00 -.347558-16 .696997-16 .820005-16  
 IFLAG= 3 H= -.388720-02  
 .272104+00 -.373863-16 .652042-16 .153267-15  
 IFLAG= 3 H= -.388720-02  
 .233232+00 -.397828-16 .574403-16 .251042-15  
 IFLAG= 3 H= -.388720-02  
 .194360+00 -.417956-16 .452850-16 .379742-15  
 IFLAG= 3 H= -.388720-02  
 .155483+00 -.432305-16 .275029-16 .540203-15  
 IFLAG= 3 H= -.388720-02  
 .116616+00 -.438459-16 .295507-17 .725921-15  
 IFLAG= 3 H= -.388720-02  
 .777441-01 -.433634-16 -.290331-16 .918866-15  
 IFLAG= 3 H= -.388720-02  
 .388721-01 -.414955-16 -.681674-16 .108720-14  
 IFLAG= 3 H= -.388720-02  
 .144355-07 -.379932-16 -.112688-15 .118857-14  
 IFLAG= 4 H= -.388720-02  
 .000000-00 -.379932-16 -.112688-15 .118857-14  
 \$TPOUT3  
 K2 = (.40739436E+01, -.11566977E+01)  
 V3 = .43017409E+00  
 V5 = .38842347E+01  
 V6A = .15725228E+01  
 V6B = .19052972E+01  
 V7 = .24288042E+00  
 RF0 = .42595531E+00

COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

```

K2NM    =   .00000000E+00
V5NM    =   .00000000E+00
BEND
*INPUT
CA      =   .32800000E+00
CB      =   .30000000E+00
CG      =   .30000000E+00
KA      =   .90000000E-03
KB      =   .44000000E-03
R0A     =   .19500000E+01
R0B     =   .90000000E+00
WAC     =   .33000000E+00,   .54000000E+00,   .00000000E+00,   .00000000E+00
SMLA    =   .45000000E-02,   .20000000E-01,   .00000000E+00,   .00000000E+00
E       =   .22000000E+05
R       =   .19862000E+01
PRXFAC  =   .13500000E+09
QS      =   -.20957000E+03
QB      =   .56900000E+03
WLM     =   .59570000E+02
KFLHHT  =   .24600000E+02
TFLM    =   .21000000E+04
TH      =   .83315000E+03
TZRO    =   .30000000E+03
PBAR    =   .34030000E+02
RBR     =   .12300000E+01
TOL     =   .10000000E-04
ITERA   =           +0
NSMAX   =           +50
NPP     =   ( .50000000E-02,   .00000000E+00)
TAPIN   =   ( .10000000E-29,   .00000000E+00)
YTD     =   .10000000E+02
OMEGA   =   .12566000E+04
NEQ     =           +1
KD      =           +2
MXSTEP  =           +100
EP      =   .10000000E-04
IHOMO   =           +0
BEND
SOUTPT1
JMAX   =           +2
WA     =   .37000000E+00
DNM    =   .10033333E+03
WB     =   .13000001E+00
VFA    =   .75542691E+00
SMLATP =   .16329932E-01
DLTYTP =   .14274320E+02
DLTYAB =   .39335400E+01
SMLB   =   .65503794E-02
DLTYBB =   .49440478E+01
KS     =   .90000000E-03
ROS    =   .16931982E+01
CS     =   .32436000E+00
KAPA   =   .14071294E-02
KAPB   =   .16296296E-02
KAPS   =   .16387300E-02
Z      =   .85867067E+00
ZPR    =   .20340954E+01

```

## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

## **COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL**

```

      .25325174E-03,   .25725760E-03,   .26124719E-03,   .26522113E-03,
      .26917995E-03,   .27312420E-03,   .27705438E-03,   .28097099E-03,
      .28487448E-03,   .28876531E-03,   .29264389E-03,   .29651067E-03,
      .30036598E-03,   .30421025E-03,   .30804382E-03,   .31186704E-03,
      .31568024E-03,   .31948374E-03,   .32327785E-03,   .32706287E-03,
      .33083907E-03,   .33460675E-03,   .33836614E-03,   .34211753E-03,
      .34586112E-03,   .34959721E-03,   .35332597E-03,   .35704764E-03,
      .36076244E-03,   .36447057E-03,   .36817221E-03,   .37186758E-03,
      .37555683E-03,   .37924018E-03,   .38291777E-03,   .38658978E-03,
      .39025635E-03,   .39391768E-03,   .39757387E-03,   .40122510E-03,
      .40487149E-03,   .40851320E-03,   .41215033E-03,   .41578304E-03,
      .41941143E-03,   .42303563E-03,   .42665576E-03,   .43027192E-03,
      .43388423E-03,   .43749280E-03,   .44109772E-03,   .44469911E-03,
      .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
      .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
      .00000000E+00,   .00000000E+00

M      =          +101
N      =          +99
RBR    =   .12300000E+01
ITERA  =          +0
NS     =          +1
NSMAX  =          +50
LFLAG   =          +1
GWBRS  =   -.43017409E+00
DGWBRS =   -.34504740E+01
QLDMLS =   -.68946471E+00

BEND
BOUTPT4
TAULR  =   .66128246E+00,   .93458967E-01,   .-95290865E-01,   .-15069028E-01,
          .15364397E-01,   .24296824E-02,   .-24773068E-02,   .-39175429E-03,
          .39943310E-03,   .63165220E-04,   .-64403327E-04,   .-10184560E-04,
          .10384188E-04,   .16421262E-05,   .-16743137E-05,   .-26477123E-06,
          .26996103E-06,   .42690874E-07,   .-43527661E-07,   .-68833413E-08,
          .70182622E-08,   .11098481E-08,   .-11316024E-08,   .-17394840E-09,
          .18245598E-09,   .28853073E-10,   .-29418624E-10,   .-46521781E-11,
          .47433658E-11,   .75010245E-12,   .-76480528E-12,   .-12094414E-12,
          .12331478E-12,   .19500651E-13,   .-19882885E-13,   .-31442231E-14,
          .32058533E-14,   .50696458E-15,   .-51690164E-15,   .-81741363E-16,
          .83343583E-16,   .13179719E-16,   .-13438055E-16,   .-21250560E-17,
          .21667095E-17,   .34263731E-18,   .-34935337E-18,   .-55245753E-19,
          .56328630E-19,   .89076502E-20,   .-90822499E-20,   .-14362413E-20,
          .14643932E-20,   .23157500E-21,   .-23611412E-21,   .-37338420E-22,
          .38070294E-22,   .60203286E-23,   .-61383336E-23,   .-97069871E-24,
          .98972545E-24,   .15651238E-24,   .-15958020E-24,   .-25235561E-25,
          .25730206E-25,   .40689019E-26,   .-41486568E-26,   .-65605685E-27,
          .66891628E-27,   .10578053E-27,   .-10785394E-27,   .-17055717E-28,
          .17390028E-28,   .27500098E-29,   .-28039130E-29,   .-44340287E-30,
          .45209405E-30,   .71492874E-31,   .-72894211E-31,   .-11527284E-31,
          .11753232E-31,   .18586228E-32,   .-18950538E-32,   .-29967845E-33,
          .30555248E-33,   .48319205E-34,   .-49266314E-34,   .-77908356E-35,
          .79435445E-35,   .12561697E-35,   .-12807920E-35,   .-20254082E-36,
          .20651084E-36,   .32657040E-37,   .-33770496E-37,   .-47727617E-38,
          .49354910E-38,   .00000000E+00,   .00000000E+00,   .00000000E+00,
          .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
          .00000000E+00,   .00000000E+00

DTAULR =   .73799413E+00,   .-35855919E-06,   .-13546264E-02,   .16016336E-02,
```

## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

	-21841563E-03,	-25824233E-03,	-35216653E-04,	.41638174E-04,
	.56782192E-05,	.67136070E-05,	.91553829E-06,	.10824808E-05,
	.14761649E-06,	.17453577E-06,	.23801533E-07,	.28141596E-07,
	.38376839E-08,	.45374615E-08,	.61877614E-09,	.73160594E-09,
	.99769526E-10,	.11796182E-09,	.16066521E-10,	.19019791E-10,
	.25937395E-11,	.30666908E-11,	.41820627E-12,	.49446352E-12,
	.67430274E-13,	.79725729E-13,	.10872244E-13,	.12854724E-13,
	.17530058E-14,	.20726551E-14,	.28264918E-15,	.33418833E-15,
	.45573443E-16,	.53883465E-16,	.73481167E-17,	.86879996E-17,
	.11847873E-17,	.14008256E-17,	.19103137E-18,	.22586466E-18,
	.30801285E-19,	.36417706E-19,	.49663019E-20,	.58718749E-20,
	.80075041E-21,	.94676254E-21,	.12911055E-21,	.15265300E-21,
	.20817370E-22,	.24613287E-22,	.33565274E-23,	.39685683E-23,
	.54119566E-24,	.63987940E-24,	.87260687E-25,	.10317212E-24,
	.14069642E-25,	.16635146E-25,	.22685436E-26,	.26821983E-26,
	.36577262E-27,	.43246916E-27,	.58976067E-28,	.69729955E-28,
	.95091106E-29,	.11243037E-28,	.15332193E-29,	.18127917E-29,
	.24721135E-30,	.29228879E-30,	.39859579E-31,	.47127720E-31,
	.64268332E-32,	.75987239E-32,	.10362424E-32,	.12251942E-32,
	.16708045E-33,	.19754642E-33,	.26939507E-34,	.31851761E-34,
	.43436410E-35,	.51356770E-35,	.70035471E-36,	.82606031E-36,
	.11292304E-36,	.13351382E-36,	.18207351E-37,	.21527347E-37,
	.29356951E-38,	.34710009E-38,	.00000000E+00,	.00000000E+00,
	.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
	.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
	.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
XLR =	.44469911E-03,	.16774631E-01,	.23325010E-01,	.27625010E-01,
	.34375389E-01,	.38875389E-01,	.45425768E-01,	.49925768E-01,
	.56476147E-01,	.60976147E-01,	.67526526E-01,	.72026526E-01,
	.78576905E-01,	.83076905E-01,	.89627284E-01,	.94127283E-01,
	.10067766E+00,	.10517766E+00,	.11172804E+00,	.11622804E+00,
	.12277842E+00,	.12727842E+00,	.13382880E+00,	.13832880E+00,
	.14487918E+00,	.14937918E+00,	.15592956E+00,	.16042956E+00,
	.16697994E+00,	.17147993E+00,	.17803031E+00,	.18253031E+00,
	.18908069E+00,	.19358069E+00,	.20013107E+00,	.20463107E+00,
	.21118145E+00,	.21568145E+00,	.22223183E+00,	.22673183E+00,
	.23328221E+00,	.23778221E+00,	.24433259E+00,	.24883259E+00,
	.25538297E+00,	.25988296E+00,	.26643344E+00,	.27093334E+00,
	.27748372E+00,	.28198372E+00,	.28853410E+00,	.29303410E+00,
	.29958447E+00,	.30408447E+00,	.31063485E+00,	.31513485E+00,
	.32168523E+00,	.32618523E+00,	.33273561E+00,	.33723561E+00,
	.34378598E+00,	.34828598E+00,	.35483636E+00,	.35933636E+00,
	.36588674E+00,	.37038673E+00,	.37693711E+00,	.38143711E+00,
	.38798749E+00,	.39248749E+00,	.39903787E+00,	.40353787E+00,
	.41008624E+00,	.41458824E+00,	.42113862E+00,	.42563862E+00,
	.43218900E+00,	.43668900E+00,	.44323938E+00,	.44773937E+00,
	.45428975E+00,	.45878975E+00,	.46534013E+00,	.46984013E+00,
	.47639051E+00,	.48089051E+00,	.48744088E+00,	.49194088E+00,
	.49849126E+00,	.50299126E+00,	.50954164E+00,	.51404163E+00,
	.52059201E+00,	.52509201E+00,	.53164238E+00,	.53614238E+00,
	.54269276E+00,	.54719275E+00,	.55374313E+00,	.56000000E+00,
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	.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
	.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
DSCRIM =	.76711670E-01,	.93458609E-01,	.96645491E-01,	.13467394E-01,
	.15582813E-01,	.21714400E-02,	.25125234E-02,	.35011611E-03,

## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

.40511132E-03,	.56451613E-04,	-.65318865E-04,	-.91020792E-05,
.10531807E-04,	.14675904E-05,	-.16981152E-05,	-.23662963E-06,
.27379872E-06,	.38153412E-07,	-.44146438E-07,	-.61517353E-08,
.71180318E-08,	.99188632E-09,	-.11476889E-08,	-.15992861E-09,
.18504972E-09,	.25786382E-10,	-.29836830E-10,	-.41577145E-11,
.48107961E-11,	.67037672E-12,	-.77567752E-12,	-.10808942E-12,
.12506779E-12,	.17427996E-13,	-.20165534E-13,	-.28100348E-14,
.32514268E-14,	.45308111E-15,	-.52424975E-15,	-.73053363E-16,
.84528370E-16,	.11778893E-16,	-.13629087E-16,	-.18991914E-17,
.21975107E-17,	.30621960E-18,	-.35431967E-18,	-.49373878E-19,
.57129381E-19,	.79608877E-20,	-.92113604E-20,	-.12835883E-20,
.14852106E-20,	.20696171E-21,	-.23947065E-21,	-.33369851E-22,
.38611489E-22,	.53804492E-23,	-.62255943E-23,	-.86752658E-24,
.10037951E-23,	.13987724E-24,	-.16184874E-24,	-.22553363E-25,
.26095978E-25,	.36364328E-26,	-.42076329E-26,	-.58632690E-27,
.47842539E-27,	.94537491E-28,	-.10938716E-27,	-.15242925E-28,
.17637237E-28,	.24577210E-29,	-.28437726E-29,	-.39627515E-30,
.45852088E-30,	.63894150E-31,	-.73930454E-31,	-.10302090E-31,
.11920312E-31,	.16610764E-32,	-.19219933E-32,	-.26782669E-33,
.30989612E-33,	.43183528E-34,	-.49966669E-34,	-.69627753E-35,
.80564675E-35,	.11226558E-35,	-.12989993E-35,	-.18101347E-36,
.20944654E-36,	.29186039E-37,	-.33770496E-37,	-.47727617E-38,
.49354910E-38,	.00000000E+00,	.00000000E+00,	.00000000E+00,
.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,
.00000000E+00,	.00000000E+00,	.00000000E+00,	.00000000E+00,

N	=	+99
XTD	=	.11419713E-01
CAP0A	=	.11687480E+01
CAP0B	=	.13535545E+01
CAP0S	=	.13611132E+01

SEND

SOUTPTS

N2	=	+0
N2MXP1	=	+4
TAPIN	=	( .10000000E-29, .00000000E+00)
DTAPIN	=	( -.13500550E-29, -.68745435E-30)
XLR	=	.44469711E-03, .16774631E-01, .23325010E-01, .27825010E-01,
		.34375389E-01, .38875389E-01, .45425768E-01, .49925768E-01,
		.56476147E-01, .60976147E-01, .67526526E-01, .72026526E-01,
		.78576905E-01, .83076905E-01, .89627284E-01, .94127283E-01,
		.10067766E+00, .10517766E+00, .11172804E+00, .11622804E+00,
		.12277842E+00, .12727842E+00, .13382880E+00, .13832880E+00,
		.14487918E+00, .14937918E+00, .15592956E+00, .16042956E+00,
		.16697794E+00, .17147793E+00, .17803031E+00, .18253031E+00,
		.18908069E+00, .19358069E+00, .20013107E+00, .20463107E+00,
		.21118145E+00, .21568145E+00, .22223183E+00, .22673183E+00,
		.23328221E+00, .23778221E+00, .24433259E+00, .24883259E+00,
		.25538297E+00, .25988296E+00, .26643334E+00, .27093334E+00,
		.27748372E+00, .28198372E+00, .28853410E+00, .29303410E+00,
		.29958447E+00, .30408447E+00, .31063485E+00, .31513485E+00,
		.32168523E+00, .32618523E+00, .33273561E+00, .33723560E+00,
		.34378598E+00, .34828598E+00, .35483636E+00, .35933636E+00,
		.36588674E+00, .37038673E+00, .37693711E+00, .38143711E+00,
		.38798747E+00, .39248749E+00, .39903787E+00, .40353787E+00,
		.41008824E+00, .41458824E+00, .42113862E+00, .42563862E+00,
		.43218900E+00, .43668900E+00, .44323938E+00, .44773937E+00,

## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

## **COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL**

## COMPOSITE SOLID PROPELLANT COMBUSTION RESPONSE MODEL

```

( .00000000E+00, .00000000E+00), ( .00000000E+00, .00000000E+00),
( .00000000E+00, .00000000E+00), ( .00000000E+00, .00000000E+00),
( .00000000E+00, .00000000E+00), ( .00000000E+00, .00000000E+00),
( .00000000E+00, .00000000E+00), ( .00000000E+00, .00000000E+00)

TAUDPS = ( -36391481E-16, -37993231E-16)
GDPSS = ( -19220352E-15, -11268834E-15)
DGOPPS = ( -12227293E-14, -11885721E-14)
RF = ( -47143511E+00, -27978254E+00)
NRP = ( -23571755E-02, -13989127E-02)
YSWP = ( -10277711E-02, -17317998E-02)
XWP = ( -13693002E-05, -23072783E-05)
NXSTP = ( -37305429E-02, -32317242E-02)
XSTP = ( -46962826E-05, -40683328E-05)
NYSSTP = ( -37305429E-02, -32317242E-02)
YSSTP = ( -35249417E-02, -30536143E-02)
RFNMLT = ( .00000000E+00, .00000000E+00)
NRPNM = ( .00000000E+00, .00000000E+00)
YSWPNM = ( .00000000E+00, .00000000E+00)
XWPNM = ( .00000000E+00, .00000000E+00)
NXSTPN = ( .00000000E+00, .00000000E+00)
XSTPNM = ( .00000000E+00, .00000000E+00)
YSSTPN = ( .00000000E+00, .00000000E+00)
$END
$TPOUT1
TWBAR = .11062365E+04
QSDMLS = -68946471E+00
QMDMLS = .19597945E+00
QBDMLS = .30582425E+00
THETAA = .10012712E+02
CHI = .72881025E+00
D = .72973667E+01
B = -86570440E+05
KMLTLR = -53178746E+00
QLDMLS = -68946471E+00
FDMLS = -21616689E+00
GWBRSS = -43017409E+00
DGWBRSS = -34504740E+01
$END

```